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Biodegradation-inspired bioproduction
of methylacetoin and 2-methyl-2,
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Methylacetoin (3-hydroxy-3-methylbutan-2-one) and 2-methyl-2,3-butanediol are currently obtained exclusively via chemical synthesis. Here, we report, to the best of our knowledge, the first alternative route, using engineered *Escherichia coli*. The biological synthesis of methylacetoin was first accomplished by reversing its biodegradation, which involved modifying the enzyme complex involved, switching the reaction substrate, and coupling the process to an exothermic reaction. 2-Methyl-2,3-butanediol was then obtained by reducing methylacetoin by exploiting the substrate promiscuity of acetoin reductase. A complete biosynthetic pathway from renewable glucose and acetone was then established and optimized via *in vivo* enzyme screening and host metabolic engineering, which led to titers of 3.4 and 3.2 g l⁻¹ for methylacetoin and 2-methyl-2,3-butanediol, respectively. This work presents a biodegradation-inspired approach to creating new biosynthetic pathways for small molecules with no available natural biosynthetic pathway.

For a sustainable future, researchers are attempting to increase the number of small molecules that can be produced from renewable biomass, for use as chemical building blocks or liquid fuels¹. C5-branched compounds, which have unique carbon structures, are interesting targets because of their varied potential applications. For example, methylacetoin and 2-methyl-2,3-butanediol can be used to produce solvents, polymers², and pharmaceutical products^{3,4}. Via standard chemical dehydration, methylacetoin can be converted into methyl isopropenyl ketone, which is used to produce optical plastics, photodegradable plastics, and fire-resistant rubbers. Using established technology, 2-methyl-2,3-butanediol can be dehydrated over a pyrophosphate catalyst to form a mixture of isoprene and methyl isopropyl ketone (MIPK)⁵. Isoprene is a monomer used in synthetic rubbers. MIPK is a better gasoline additive than methyl *tert*-butyl ether and can also be used as a food additive, solvent, tantalum and niobium extractant, and reagent in indoline synthesis⁶. However, the current chemical production of these compounds suffers from limited feedstocks, the use of toxic catalysts, and high costs, which limits their widespread use^{7,8}.

Bioconversions using engineered microorganisms occur under mild conditions, have high selectivity, and have low potential costs and are thus highly valued as an alternative source of chemicals and fuels. The first challenge we faced in establishing a microbial production route to methylacetoin and 2-methyl-2,3-butanediol was the lack of natural biosynthetic pathways to these compounds. Methylacetoin was detected in the secretions of *Rhyssa persuasoria*, *Xyloterus domesticus*, and *X. lineatus*; however, the metabolic origin has not been studied^{9,10}. 2-Methyl-2,3-butanediol was found in blood and urine samples from animals that had inhaled or ingested *tert*-amyl methyl ether, a common gasoline additive, likely from a monooxygenase reaction¹¹. However, this biochemical reaction cannot be used for the microbial production of methyl-2,3-butanediol because *tert*-amyl methyl ether is not biologically available either. Thus, the *de novo* design and construction of non-natural synthetic pathways is required, and to be economically competitive, an ideal biosynthetic pathway should be straightforward with high atom efficiency and a minimal number of steps that preferably involve the condensation of small molecules from the cell's central metabolism.

Here, we established two biosynthetic pathways that produce one molecule of C5 product from one acetone and one-half or one glucose molecule inspired by the idea of reversing the known methylacetoin biodegradation pathway. On the basis of thermodynamic principles and mechanistic insight, we accomplished this reversal by modifying the enzyme complex, switching the reaction substrate, and coupling to an exothermic reaction to

overcome thermodynamic limitations. After optimization, the strains exhibited promising productivities and yields.

Results

Biosynthesis of methylacetoin by reversing its biodegradation.

Methylacetoin is not a natural metabolite of microorganisms. However, as an artificial substance, it can be degraded by some bacteria to serve as a carbon source for their growth¹². As reported, one molecule of methylacetoin degrades to one acetone and one acetyl-CoA while generating one NADH molecule from NAD⁺, catalyzed by a methylacetoin/acetoin dehydrogenase complex (Fig. 1). This biodegradation has an estimated $\Delta rG'^{\circ}$ of $-1.7 \text{ kcal mol}^{-1}$ (calculated using GCM software¹³, which is based on group contribution theory), which favors the forward reaction. However, previous studies have concluded that bioreactions with free energies between $+3.5 \text{ kcal mol}^{-1}$ and $-3.5 \text{ kcal mol}^{-1}$ are potentially reversible¹⁴. Thus, we proposed redirecting the reaction to achieve methylacetoin

biosynthesis by elevating the acetyl-CoA and acetone concentrations. To test this hypothesis, we cloned the operon *acoABCL* (which encodes the methylacetoin/acetoin dehydrogenase complex) from *Bacillus subtilis* into *E. coli* and confirmed its functional expression by observing the acetoin and methylacetoin degradation activity *in vivo* (Supplementary Fig. S1). We expected that methylacetoin could be synthesized by the recombinant *E. coli* from endogenous acetyl-CoA and NAD⁺ and exogenous acetone, which was added to reach a 200 mM concentration. However, no methylacetoin was detected from this culture. Increasing the acetone concentration further caused cell death. Increasing the intracellular acetyl-CoA concentration 34-fold via metabolic engineering has been previously reported¹⁵ but is unlikely to increase the methylacetoin production to an acceptable level.

We then referred back to methylacetoin biodegradation, this time with respect to the detailed enzymatic reaction mechanism. The degradation complex consists of three component enzymes: acetoin:2,6-dichlorophenolindophenol oxidoreductase (AcoAB), dihydrolipoamide acetyltransferase (AcoC), and dihydrolipoamide dehydrogenase (AcoL). This AcoAB component is a thiamine pyrophosphate (ThDP)-dependent enzyme that cleaves the carbon-carbon bond in methylacetoin to release acetone and a ThDP-bound 'active acetaldehyde'; AcoC oxidizes the acetaldehyde into an acetyl group and transfers it to free CoA to form acetyl-CoA via its lipoamide cofactor; AcoL regenerates the oxidized lipoamide using NAD⁺ and generates NADH¹⁶ (Fig. 1). In conclusion, methylacetoin degrades through a four-step reaction sequence organized by a multienzyme complex. The key step that must be reversed is the carbon-carbon bond cleavage catalyzed by AcoAB, i.e., a ThDP-bound 'active acetaldehyde' must condense with an acetone for methylacetoin synthesis. Because providing the 'active acetaldehyde' via the reduction of acetyl-CoA through AcoC and AcoL proved difficult, as described above, we reasoned that exchanging the acetyl-CoA with a higher energy substrate may enable the reversion. Our first candidate was pyruvate, the direct precursor in the central metabolism of acetyl-CoA and the end product of glycolysis. Energy calculations predicted that this substrate could greatly improve the thermodynamic aspects of the methylacetoin biosynthesis by providing an estimated $\Delta rG'^{\circ}$ of $-15.05 \text{ kcal mol}^{-1}$, which would make the reaction irreversible. As found for other ThDP enzymes such as pyruvate decarboxylase and acetolactate synthase, the decarboxylation of pyruvate can generate an 'active aldehyde' that is equivalent to that found in AcoAB. Another necessary modification is to block the 'active aldehyde' from transferring to AcoC; otherwise, the degradative reaction will occur rather than condensation (Fig. 1). The remaining question is whether pyruvate is an acceptable substrate for AcoAB (or AcoABCL), as previous studies have obtained inconsistent results¹⁶. To test this strategy, we omitted both *acoC* and *acoL* to clone *acoAB* alone in *E. coli* BL21(DE3). In the *in vitro* tests, the AcoAB enzyme prepared from this strain catalyzed the generation of methylacetoin from pyruvate and acetone, which was confirmed in GC-MS by comparison to the known compound (Supplementary Fig. S2). The recombinant *E. coli* was then used to produce methylacetoin via shake-flask experiments. After cultivating in an M9 glucose minimal medium supplied with 200 mM acetone under air-limited conditions for 24 h, 7.1 mg l⁻¹ of methylacetoin accumulated in the culture broth [Fig. 2, strain BL21(DE3)/pJXL32]. No methylacetoin was produced without the addition of acetone. We also examined the recombinant strains for any degradation activity. Unlike those strain expressing AcoABCL, the AcoAB strain did not degrade either methylacetoin or acetoin (Supplementary Fig. S1), which indicates that the ThDP-bound 'active acetaldehyde' tends to condense rather than release as free acetaldehyde, as occurred with pyruvate decarboxylase¹⁷.

To increase the productivity, we screened AcoAB enzymes from three acetoin-degrading bacteria arbitrarily selected from a pool of 22, namely, *B. subtilis*, *Pelobacter carbinolicus* (codon optimized),

Figure 1 | Biodegradation-inspired construction of the biosynthetic pathways. Methylacetoin biodegradation is presented with a dashed line, and the constructed biosynthetic pathways are presented using a solid line. The enzymes (gene names in parentheses) for each numbered step are as follows: (1) glycolysis; (2,3) acetolactate synthase and acetolactate decarboxylase (*alsS* and *alsD*); (4) acetaldehyde dehydrogenase (*acoD*); (5) acetoin:2,6-dichlorophenolindophenol oxidoreductase (*acoAB*); (6) dihydrolipoamide acetyltransferase (*acoC*); (7) dihydrolipoamide dehydrogenase (*acoL*); (8) acetoin/methylacetoin reductase (*bdhA*). Enzymes (5), (6), and (7) form the degradation complex. (6) and (7) need to be deleted to block biodegradation during the biosynthesis. The presence of (4) enhanced the biosynthesis of methylacetoin from acetoin and acetone by improving the reaction thermodynamics.

Figure 2 | Biosynthesis of methylacetoin and 2-methyl-2,3-butanediol. (a) Plasmids carrying the pathway genes. (b) Methylacetoin and 2-methyl-2,3-butanediol production via pathway 1 or 2 hosted by BL21(DE3) or YYC202(DE3)ΔldhA. The BL21(DE3) strains and YYC202(DE3)ΔldhA strains were cultured in an M9 medium and enhanced M9 medium, respectively, under shake-flask and air-limited conditions (see **Method** for details). After gene expression was induced, 200 mM acetone was added. The product concentrations were determined after cultivating for 24 h by GC or GC-MS. The error bars represent the standard error associated with triplicate experiments.

and *Pseudomonas putida*¹⁸. The highest productivities were achieved using AcoAB from *B. subtilis* and were 3.1- and 1.1-fold those of the *P. carbinolicus* and *P. putida* isozymes, respectively (Supplementary Fig. S3). We further screened other ThDP-dependent enzymes, including YerE from *Yersinia pseudotuberculosis* (codon optimized)¹⁹, PDC from *Zymomonas mobilis* and its Glu473Gln mutation¹⁷, PdhAB from *B. subtilis*, and PdhAB from *Sus scrofa* (optimized for codon with the transit peptides removed). No detectable methylacetoin was produced using recombinant *E. coli* strains expressing these enzymes. Similarly, no or only faint activities were detected for these enzyme samples *in vitro* (Supplementary Fig. S4).

Therefore, AcoAB from *B. subtilis* was used in the following studies. This biosynthetic route based on the condensation of pyruvate and acetone catalyzed by AcoAB was denoted as pathway 1. Its overall stoichiometry is as follows: $1/2 \text{ Glucose} + 1 \text{ Acetone} \rightarrow 1 \text{ Methylacetoin} + 1 \text{ CO}_2 + 1 \text{ ATP} + 1 \text{ NADH}$.

Pathway 1 successfully produced methylacetoin in the recombinant *E. coli* culture. However, the achieved methylacetoin titer was much lower than the acetone and pyruvate concentrations, which implies that the reaction is kinetically limited because it is highly thermodynamically favorable, as discussed above. This observation is not surprising because pyruvate is not the native substrate for

AcoABCL and thus has a low substrate-enzyme affinity. To address this issue, we started using acetoin instead of pyruvate as the ‘active acetaldehyde’ donor for methylacetoin synthesis and an acetaldehyde would be concomitantly generated instead of a CO_2 (Fig. 1). Acetoin was reported to be degraded by AcoABCL with an activity 81% that of methylacetoin¹⁶; therefore, it should be a good substrate for AcoAB. The feasibility of synthesizing methylacetoin from acetone and acetoin was demonstrated *in vitro* (Fig. 3). However, the reaction equilibrium strongly favored the reactants. A free energy of $5.37 \pm 0.20 \text{ kcal mol}^{-1}$ was determined, which is close to the predicted $\Delta\text{rG}'^\circ$ of $3.51 \text{ kcal mol}^{-1}$. During the shake-flask experiments, *E. coli* BL21(DE3) expressing AcoAB produced 0.72 mM methylacetoin from 5 mM acetoin and 200 mM acetone in an M9 medium (Supplementary Fig. S5).

To overcome this thermodynamic limitation and drive the equilibrium to completion, we coupled the reaction to an acetaldehyde dehydrogenation, which has an estimated $\Delta\text{rG}'^\circ$ of $-8.91 \text{ kcal mol}^{-1}$, to obtain a negative overall $\Delta\text{rG}'^\circ$. Acetaldehyde dehydrogenase (AcoD) from *Alcaligenes eutrophus* was chosen because it had the greatest reported preference for NADH over NADPH²⁰. *In vitro*, the combination of AcoD with AcoAB quantitatively converted acetoin

into methylacetoin, with no detectable acetoin remaining (Fig. 3). Similarly, the coexpression of AcoD and AcoAB in *E. coli* promoted methylacetoin formation from exogenous acetoin. Acetaldehyde dehydrogenase from *Saccharomyces cerevisiae* (ALD3) was also tested but did not work as well (Supplementary Fig. S5).

E. coli is not a natural acetoin producer; thus, introducing a biosynthetic pathway to acetoin in *E. coli* is required to complete the pathway from glucose to methylacetoin. This pathway consists of acetolactate synthase (AlsS) and acetolactate decarboxylase (AlsD), which convert two pyruvate molecules into one acetoin and release two CO_2 molecules. Previously, we cloned the *alsSD* operon from *B. subtilis* into *E. coli* and achieved an acetoin titer of over 7.8 g l^{-1} with greater than 80.2% yield (mole acetoin/mole glucose) in the M9 medium²¹. By coexpressing *alsSD*, *acoAB*, and *acoD* [strain BL21(DE3)/pJXL32,pJXL62B], we produced methylacetoin at a titer of 1.7 g l^{-1} , which is 240-fold that of pathway 1 using the same host and medium [Fig. 2]. In this strain, pyruvate and acetoin can both condense with acetone to produce methylacetoin via AcoAB. However, based on the improved productivity, most of the methylacetoin production can be attributed to acetoin. The new pathway based on the condensation of acetoin and acetone was denoted as

Figure 3 | Improving the methylacetoin biosynthesis from acetoin by coupling the conversion to acetaldehyde dehydrogenation. Acetoin and acetone were incubated with the AcoAB enzyme sample (left) or with the AcoAB and AcoD enzymes with the NAD^+ cofactor (right). The reaction mixture was composed of 400 mM Tris-HCl buffer (pH 8.0), 2 mM MgSO_4 , 100 mM KCl, 0.2 mM ThDP, 1 mM thioglycol, 2.5 mM NAD^+ , 50 mM acetone, and 1 mM acetoin. The reactions were initiated by adding the enzymes (time = 0) and were conducted at 30°C for 12 h to reach equilibrium. The reaction mixtures were analyzed by GC. I.S., internal standard (1-butanol).

pathway 2. Its overall stoichiometry is as follows: 1 Glucose + 1 Acetone $\rightarrow$ 1 Methylacetoin + 1 Acetate + 2 CO₂ + 2 ATP + 3 NADH.

Biosynthesis of 2-methyl-2,3-butanediol. Next, we sought to reduce methylacetoin into another important chemical, 2-methyl-2,3-butanediol. The non-enzymatic hydrogenation of ketones into alcohols involves high H₂ pressure and elevated temperatures; therefore, we sought to implement this conversion biologically using a reductase. As such a reductase had not yet been reported, we chose acetoin reductase (also known as 2,3-butanediol dehydrogenase, encoded by *bdhA*) from *B. subtilis* as the first candidate based on the similarities between methylacetoin and acetoin²². This selection was also supported by a preliminary experiment indicating that 2-methyl-2,3-butanediol was generated via the addition of methylacetoin to *B. subtilis* cultures. This preliminary experiment also indicated that *E. coli* did not reduce methylacetoin into 2-methyl-2,3-butanediol at a detectable rate despite previous studies finding that it possessed a broad-range of alcohol dehydrogenases and could reduce many heterologous substrates, such as 4-hydroxybutyraldehyde²³ and isobutyraldehyde²⁴. BdhA enzyme samples were prepared by overexpressing *bdhA* in an *E. coli* host BL21(DE3). The *in vitro* activity was determined from the consumption of NADH, as measured by the change in absorbance at 340 nm. The generation of 2-methyl-2,3-butanediol was confirmed via GC-MS by comparing to the authentic compound (Supplementary Fig. S6). BdhA was found to reduce methylacetoin at a rate of 55% of its natural activity (acetoin reduction) (Supplementary Fig. S7). By introducing BdhA into our methylacetoin producing strains, we produced 8.6 mg l⁻¹ and 1.5 g l⁻¹ of 2-methyl-2,3-butanediol via pathways 1 and 2, respectively [Fig. 2, strains BL21(DE3)/pJXL37 and BL21(DE3)/pJXL37,pJXL62B]. For the pathway 2 strain culture, 9.6 mg l⁻¹ of 2,3-butanediol was also detected as a byproduct, which is likely a reduction product of the intermediate, acetoin, by BdhA (Supplementary Fig. S8).

Metabolic engineering of the host strain. With the functional pathways to methylacetoin and 2-methyl-2,3-butanediol validated, we next aimed to improve their production levels by metabolic engineering of the host strain to channel carbon flux into the end products. First, we investigated whether any native pathways existed in the host background that might compete with these heterogeneous pathways by dissipating a flux of the intermediates. Acetone, acetoin, and methylacetoin were added to the *E. coli* culture at concentrations close to those required by the biosynthesis. No substantial change in their concentrations was observed after 12 h (Supplementary Fig. S9). We then focused on the upstream reactants, increasing the flux toward pyruvate by modifying the native metabolism. Fortunately, because pyruvate is a common precursor for many fermentation products, a series of *E. coli* strains with enhanced pyruvate biosynthesis have been developed. YYC202Δ*ldhA* is one such strain, with the pathways converting pyruvate into ethanol, acetate, lactate, and TCA blocked (resulting in acetate auxotrophy) and with the highest reported pyruvate production (yields of 0.87 g/g of glucose, titer of 110 g l⁻¹)²⁵. Its derivative, YYC202(DE3)Δ*ldhA*, was constructed for harboring T7 expression plasmids and was successfully applied in an acetoin biosynthesis study²⁶. In this study, using YYC202(DE3)Δ*ldhA* as the host to express the biosynthetic pathways improved the production (Fig. 2) in an M9 medium supplemented with 1 g l⁻¹ ammonium acetate, 0.1 g l⁻¹ tryptone, 10 mg l⁻¹ vitamin B1, and 200 mM acetone. Here, the ammonium acetate and tryptone were added to rescue the acetate auxotrophy of the host. Using this metabolic engineered host, pathway 1 produced 9.2 mg l⁻¹ of methylacetoin [Fig. 2, strain YYC202(DE3)Δ*ldhA*/pJXL32] or 8.3 mg l⁻¹ 2-methyl-2,3-butanediol when BdhA was included [Fig. 2, strain YYC202(DE3)Δ*ldhA*/pJXL37]. Significantly higher titers were again achieved through pathway 2, which

produced 3.4 g l⁻¹ methylacetoin with a yield of 1 g methylacetoin per 2.63 g of glucose and 0.67 g of acetone consumed [Fig. 2, strain YYC202(DE3)Δ*ldhA*/pJXL32,pJXL62B] or 3.2 g l⁻¹ of 2-methyl-2,3-butanediol with a yield of 1 g of 2-methyl-2,3-butanediol per 2.81 g of glucose and 0.75 g of acetone consumed when BdhA was included [Fig. 2, strain YYC202(DE3)Δ*ldhA*/pJXL32,pJXL62B]. The byproduct, 2,3-butanediol, was detected at 21.6 mg l⁻¹ for the YYC202(DE3)Δ*ldhA*/pJXL32,pJXL62B strain (Supplementary Fig. S8).

Discussion

In this study, we report the first microbial routes for the production of methylacetoin and 2-methyl-2,3-butanediol. No natural biosynthetic pathway has been identified for these compounds, which presents a major challenge to this endeavor. However, as with many artificial substances, methylacetoin can be microbiologically degraded, which provides a metabolic relationship between methylacetoin and common cellular metabolites. Based on the functional reversal of methylacetoin biodegradation, we constructed two artificial biosynthetic pathways to methylacetoin formation. The equilibrium, which originally favored degradation, was redirected toward biosynthesis by using alternative substrates with higher free energy, modifying the enzyme complex to block the degradation branch, and coupling the synthesis to an exothermic reaction. These pathways were then extended to 2-methyl-2,3-butanediol using a methylacetoin reductase. Notably, similar to the classic ethanol-acetate fermentation, producing 2-methyl-2,3-butanediol via pathway 1 produces one net ATP and is redox balanced, whereas pathway 2 produces two ATP and two NADH (per product). Thus, it is theoretically possible to make these reactions the primary energy-producing pathways and couple them to the growth and maintenance of the host. In that case, a high yield and low process cost can be obtained²⁷. In this study, enzyme screening and metabolic engineering were used to improve the productivity, which resulted in the strains producing methylacetoin at concentrations of 3.4 g l⁻¹ or 2-methyl-2,3-butanediol at 3.2 g l⁻¹. However, the yields were still much lower than the theoretical maxima calculated from the stoichiometry, and no contribution of the pathway expression to the cell growth has been observed. Another problem is that pathway 1 has a higher atom efficiency than pathway 2 without the byproducts acetate and 2,3-butanediol but is limited by the low activity of AcoAB toward pyruvate. Future studies require the enzyme engineering of AcoAB to increase its activity and finely tune the enzyme expression levels to reach the potential of these two biosynthetic pathways.

In this study, we used glucose and acetone as the starting feedstocks. Acetone can be produced from acetone-butanol fermentation in large amounts. The expected commercialization of bio-butanol in the near future means that an increased amount of acetone will be available as a renewable byproduct²⁸. Acetone biosynthesis has also been reconstructed using *E. coli* in high yield from glucose²⁹. Incorporating this acetone pathway into the methylacetoin biosynthesis eliminates the need of exogenous acetone.

To our knowledge, this study presents the first intuitive biosynthetic pathway inspired by the biodegradation of the product compounds; however, some other examples have also demonstrated the reversible nature of biodegradation and thus support the general applicability of our strategy. Recently, a non-natural product, 1,4-butanediol, was biosynthesized via a computationally designed pathway²³ that nearly mirrors its biodegradation pathway³⁰. In another study, the engineered reversal of the β -oxidation cycle was used to synthesize fatty acids and derivatives that surpassed natural fatty-acid biosynthesis pathway in product titer and yield³¹. In addition, many strategies have been proposed to change the direction of reaction equilibria and can be applied to biodegradation reversal, such as switching cofactors [FAD to NAD(P)H or ferredoxin], the physical sequestration of products, enzyme-substrate compartmentalization^{31,32}, and changing the NAD(P)H/NAD(P)⁺ ratio²³. The synthetic potential of biological

catalysts is masked when the product are not required by living organisms. The biodegradation of artificial substances by natural or laboratory-evolved microbes unmasked this potential in a roundabout manner. As a large number of commodity chemicals can be biodegraded, the exploration of their biodegradation for use in our biodegradation-reversal strategy will help realize the bioproduction of more such useful chemicals.

Methods

Strains and plasmids. *E. coli* DH5 α was used for the plasmid construction. *E. coli* BL21(DE3) was used for the enzyme sample preparation and product biosynthesis. The *E. coli* YYC202(DE3) Δ ldhA with enhanced pyruvate biosynthesis was generously provided by Prof. Kristala L. J. Prather (Department of Chemical Engineering, Massachusetts Institute of Technology) and used in this study for biosynthesis.

Plasmid isolation, genomic DNA isolation, and PCR product purification were conducted using an E.Z.N.A.TM Plasmid Mini Kit, Bacterial DNA Kit, and Cycle-Pure kit (OMEGA, Doraville, CA), respectively. The gene chemical syntheses, PCR primer syntheses and DNA sequencing were conducted by the Shanghai Genaray Biotech Co. The genes and operons used in this study were chemically synthesized or amplified from the appropriate genomic DNA templates using PyrobestTM DNA polymerase. Codon optimization was performed using an online tool, OPTIMIZER (<http://genomes.urv.es/OPTIMIZER/>), based on *E. coli* codon usage. Expression vectors from pET and pACY systems (Novagen, Madison, WI) were used to harbor the genes or operons in their multicloning sites (Details are provided in **Supplementary Methods**). The following antibiotics were used to maintain the plasmids when necessary: kanamycin (Kan, 50 μ g ml⁻¹), and chloramphenicol (Cm, 30 μ g ml⁻¹).

Preparation of crude enzyme and *in vitro* enzyme assays. Colonies of strains were picked to LB liquid medium (10 g l⁻¹ Oxoid tryptone, 5 g l⁻¹ Oxoid yeast extract, and 10 g l⁻¹ NaCl) containing the appropriate antibiotics and grown overnight at 37°C. The enzymes were expressed by inoculating 0.5 ml of the overnight cultures in 50 ml of fresh LB and incubating at 37°C to an OD600 between 0.6 and 0.9 before inducing with 0.5 mM IPTG for 2 h at 30°C. The cells were collected by centrifuging at 5,000 G and 4°C. The harvested cells were washed twice and resuspended in PBS (containing 137 mM NaCl, 2.7 mM KCl, 8.1 mM Na₂HPO₄, and 1.76 mM KH₂PO₄, pH 7.4). The resuspended cells were then lysed via ultrasonication while cooling in an ice bath. After centrifuging at 20,000 G, the cell-free supernatant was used as the crude enzyme. The total protein concentrations were measured through Bradford assays. Strains containing empty plasmids were used as the control.

Enzyme assays of the methylacetoin synthesis and degradation were performed at 30°C in 50 mM potassium phosphate at a pH of 7.0 with 2 mM MgCl₂ and 0.2 mM ThDP. The substrates were added at the indicated concentrations. A reaction mixture composed of 400 mM Tris-HCl buffer (pH 8.0), 2 mM MgSO₄, 100 mM KCl, 0.2 mM ThDP, 1 mM thioglycol, 2.5 mM NAD⁺, 50 mM acetone, and 1 mM acetoin was used to couple methylacetoin synthesis with acetaldehyde dehydrogenation. For methylacetoin (and acetoin) reduction, the reaction mixture was composed of 100 mM Tris-HCl buffer (pH 8.0), 0.2 mM NADH, and 20 mM methylacetoin or acetoin. The NADH oxidation was monitored at 340 nm and 30°C using a Cary 50 bio UV-visible spectrophotometer.

Analysis of methylacetoin and 2-methyl-2,3-butanediol by gas chromatography and mass chromatography-mass spectroscopy. Pure methylacetoin and 2-methyl-2,3-butanediol were purchased from Alfa Aesar (Ward Hill, MA) and Sigma-Aldrich (St. Louis, MO), respectively. For the methylacetoin analysis, 0.8 ml aqueous samples (culture supernatants or enzyme reactions) were mixed with 50 μ l of 100 mM butanol in ethyl acetate (internal standard) and 0.8 ml of ethyl acetate. The mixture was shaken vigorously for 3 min. After centrifuging, the upper organic layer was filtered (0.22 μ m) and subjected to GC or GC-MS analysis. For the 2-methyl-2,3-butanediol analysis, 1 ml of the filtered samples were dried in an Eppendorf concentrator for approximately 3 h at 30°C. The residents were resolved in 1 ml of ethyl acetate and centrifuged for 5 min before filtering (0.22 μ m) and subjecting to GC or GC-MS analysis.

The GC analyses were performed using an SP-6890 gas chromatography system equipped with a CP-Wax58 column (25 m length, 0.25 mm ID, and 0.2 μ m film thickness from Varian). The experimental chromatographic conditions were an injector temperature of 200°C, flame ionization detector set to 270°C, and N₂ carrier gas at 0.05 Mpa, and the oven temperature program was as follows: held for 1 min held at 50°C followed by a linear temperature increase of 3°C min⁻¹ to 90°C and then 40°C min⁻¹ to 200°C, which was held for 5 min.

The GC-MS analysis was performed using an Agilent 5975C GC-MS System equipped with a DB-5 ms column (50 m length, 0.25 mm ID, and 0.25 μ m film thickness from Agilent, Palo Alto, CA, USA). The experimental chromatographic conditions were as follows. The injector was set to 250°C, helium was used as the carrier gas and flowed at 1 ml min⁻¹, and the oven temperature was programmed as follows: held for 1 min at 40°C, followed by a linear temperature increase of 5°C min⁻¹ to 80°C and then 25°C min⁻¹ to 300°C, which was held for 5 min. The MS scan used a source temperature of 230°C, an interface temperature of 300°C, an E energy of 70 eV, and a mass scan range from 2 to 150 amu.

Microbial synthesis of methylacetoin and 2-methyl-2,3-butanediol. *E. coli* BL21(DE3) strain precultures were diluted 100-fold in an M9 minimal salt medium (per liter: 17 g Na₂HPO₄·12H₂O, 3 g KH₂PO₄, 1 g NH₄Cl, 0.5 g NaCl, and 0.5 g MgSO₄·7H₂O) supplemented with 20 g l⁻¹ of D-glucose and the appropriate antibiotics. For the acetate auxotrophic YYC202(DE3) Δ ldhA strains, 1 g l⁻¹ of ammonium acetate, 0.1 g l⁻¹ of tryptone, and 10 mg l⁻¹ of vitamin B1 were also supplemented. The strains were incubated at 37°C to an OD600 between 0.6 and 0.9. Then, enzyme expression was induced by adding 0.5 mM IPTG and at 30°C. At the time of induction, 200 mM of acetone was added and the flasks were sealed to subject the cultures inside to air-limited conditions. A shaking rate of 180 rpm was maintained throughout. Methylacetoin and 2-methyl-2,3-butanediol production were determined by GC as described above.

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Author contributions

X.J., Haibo Zhang., J.Y., Y.Z. and M.X. designed the experiments. X.J., Haibo Zhang., M.X., Y.Z., J.Y., R.Z., T.C. and D.F. performed the experiments. X.J., Haibo Zhang., M.X., W.L., X.X., Y.C., F.J. and Huibin Zou wrote the manuscript.

Additional information

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Affiliation 1 was incorrect in the original version of this Article. The affiliation was incorrectly listed as “Qingdao Institute of Bioenergy and Bioprocess Technology, Chinese Academy of Sciences, Qingdao, 266101, China”. The correct affiliation is listed above, and has been corrected in the HTML and PDF versions of this Article.

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