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[4-(3-Amino-4-methoxy-5-methylphenyl)-1-oxo-1*H*-phthalaz-2-yl] acetic acid hydrazide and its synergetic effect with KI as a novel inhibitor for low carbon steel corrosion in 0.5 M H₂SO₄

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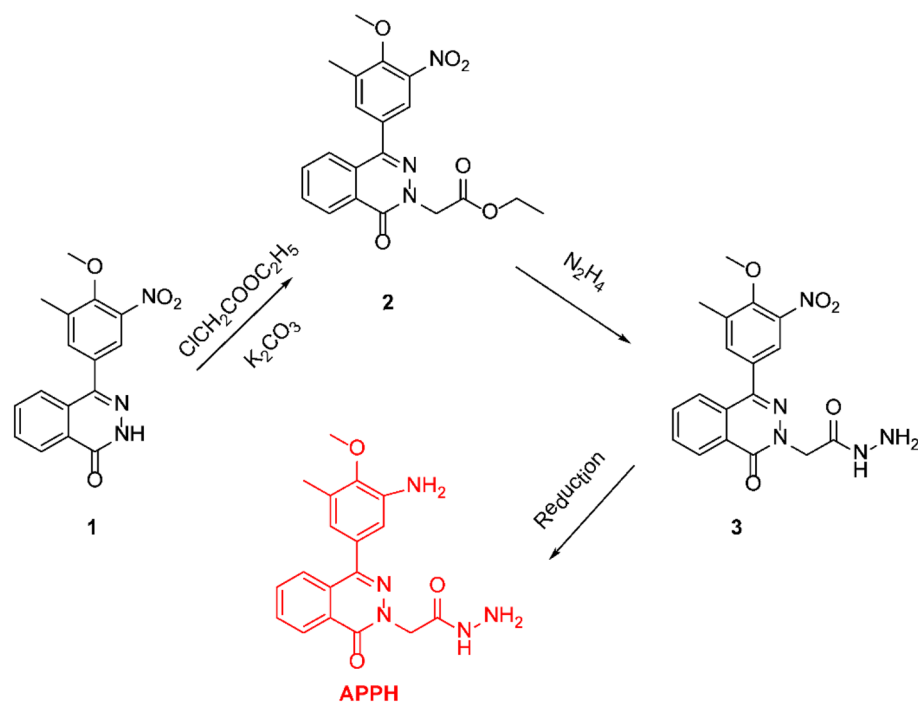
We report the synthesis of novel [4-(3-amino-4-methoxy-5-methyl phenyl)-1-oxo-1*H*-phthalaz-2-yl] acetic acid hydrazide (APPH), followed by its characterization using X-ray diffraction (XRD), Fourier transforms infrared (FT-IR) spectroscopy, ¹H-NMR spectroscopy, and LC/MS. Further, the inhibition effect of the varying concentration of APPH on the corrosion of low steel (LCS) in 0.5 M H₂SO₄ was investigated by weight loss and electrochemical measurements at 30 °C. The percentage inhibition efficacy of APPH increased with concentration and reached about 84% at 0.5 mM at 30 °C, also rising to 88% after 6 h of exposure. According to the polarization measurements, the investigated APPH works as a mixed-type inhibitor. Furthermore, the synergistic corrosion inhibition mechanism APPH showed that the inhibition efficiency maximizes with increasing inhibitor concentration, and the maximum value was 83% at 0.5 mM APPH. The adsorption of APPH on the LCS surface is more fitting to the Langmuir isotherm model. The free energy value (−Δ*G*^o ads) was 33.3 kJ mol^{−1}. Quantum chemical calculation was applied to APPH and acted as excellent support for the experimental data.

Metal corrosion has caused severe ecological impacts and economic loss to various productions, such as chemical engineering, oilfield category, desalination plants, etc. The destructive influence of strong acids such as Sulfuric acid (H₂SO₄) in the pickling and descaling process of metals seriously affected some infrastructure construction, especially carbon steel (CS) channels^{1–3} and accordingly, the addition of inhibitors is an important requirement^{4,5}. Corrosion inhibition of steel is expected because of the excellent probability of protective film formation through the different electronic systems; π-bonds systems, free lone pairs on functional groups and conjugated systems between heterocyclic rings and functional groups^{6–8}.

Corrosion inhibitors create a protective barrier on metal via chemical or physical adsorption^{9–12}. Charge sharing or transfer of free lone pairs of electrons from the conjugated site of the inhibitor molecule to the non-complete d orbital on the metal surface is the chemical process that produces the protective layer^{13–15}. Electrostatic forces between a steel surface charged in one direction and an inhibitor charged in the other direction are responsible for the physical formation of the protective layer. Like this, unoccupied d-orbitals of iron can share electrons with p-orbitals in aromatic systems to form feedback bonds, creating many chemisorption active sites^{16,17}.

Phthalazinones are an intriguing class of organic compounds with a 2*H*-pyridazin-3-one core that includes aromatic systems, nitrogen atoms, and various electronegative centers that may be adjacent or substituent groups on the pyridazine ring^{18–23}. In the past few years, derivatives of 2*H*-phthalazin-1-one were also applied

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Scheme 1. Synthetic route of APPH inhibitor.

as corrosion inhibitors of aluminum, steel and copper in an acidic environment^{24–29}. Recently we considered the inhibitory outcome of two derivatives of 4-aryl phthalazinone, which contain amino or hydrazide moiety³⁰.

Because not all individual compounds positively affect corrosion inhibition, many studies have been conducted to minimize the corrosion percentage by depending on the phenomenon of synergism through adding halide anions. It has been demonstrated that in acid solutions, halide ions form intermediates on a corroding steel surface, which may inhibit or accelerate iron anodic dissolution by substituting some of the adsorbed OH ions in the anodic process. Authors have proposed various mechanisms to explain the synergistic effect of organic inhibitors and halide ions. These include halide ion accumulation, which attracts the inhibitor molecule to the metal, halide ion and organic ion exchange, co-adsorption of inhibitor and halide ions, and a combination of various scenarios. According to the literature, inhibitor cation adsorption would be maximized on the directed dipoles formed by the halide ions as they first adsorb on the metal surface^{31,32}.

As an important section of Theoretical chemistry, Quantum chemical calculations have proven to be an excellent tool for interpreting corrosion inhibition mechanisms^{33–36}. The development of hardware and software of quantum chemical procedures, such as functional density theory (DFT), have recently been required as a quick and strong tool to interpret and explain corrosion inhibition performances of inhibitors problems. This is due to the strong associations found between the corrosion inhibitions effectiveness of maximum compounds and numerous semi-empirical criteria. The importance of the adsorption of inhibitor molecules on substrates in the context of corrosion research has lately increased^{37–45}.

Further, the goal of this study is to continue our previous study on 4-aryl phthalazinone derivatives, which contain amino or hydrazide moiety to synthesize novel inhibitor²⁴. APPH that contains both amino and hydrazide groups was investigated for its corrosion percentage on LCS in 0.5 M H₂SO₄ using electrochemical impedance spectroscopy (EIS), weight loss (WL), and potentiodynamic polarization (PDP) analyses. Iodide ions' synergistic impact on APPH's inhibitive performance was also discussed. Also measured, discussed, and interpreted were a number of thermodynamic parameters, kinetic parameters, and quantum chemical calculations of density functional theory (DFT) for LCS corrosion at varied concentrations of APPH.

Experimental procedure

APPH synthesis and equipment. Opti Melt equipment (a melting point automated system with digital image) was used to measure the melting points and are uncorrected. Thin layer chromatography (TLC) on silica gel plates 60-F254 (Merck, 0.25 thickness layer) was used to determine the products' purity and monitor the reactions. Infra-red spectra FTIR were recorded on Bruker Model Vertex 70 with Platinum ATR unit. ¹H-NMR spectroscopy were carried on Bruker 400 MHz in deuterated dimethylsulphoxide (DMSO-d₆) using tetramethylsilane (TMS) as an internal standard. Triple Quad LC/MS Agilent Technologies 6460 equipment with electrospray ionization (ESI-MS/MS) coupled to an Agilent Technologies 1260 using Agilent ZORBAX column (Eclipse plus C18; 4.6 × 100 nm × 3.5 μm), Mobile phase: 50% CH₃CN/50% H₂O + 0.1% HCOOH was used to detect Mass spectra. The APPH was synthesized according to the synthetic route in Scheme 1.

4-(4-methyl-3-nitro) phenyl-2H-phthalazin-1-one (1) was synthesized following the reported method⁴⁶.

Ethyl [4-(4-methoxy-5-methyl-3-nitro-phenyl)-1-oxo-1H-phthalaz-2-yl] acetate (2). Compound **1** (3.1 g, 0.01 mol) was reacted with ethyl acetoacetate (2.4 g, 0.002 mol) in acetone in the presence of anhydrous K_2CO_3 (2.6 g, 0.02 mol) at heating at reflux for 12 h (checked by TLC). The reaction mixture was put onto the water after the solvent was concentrated. Compound **2** was obtained with a 90% yield after the precipitate was filtered out, dried, and recrystallized from ethanol. m.p. 237–240 °C, FTIR (ν , cm^{-1}): 3316 (NH), 1672 (C=O, acetic acid hydrazide), 1650 (C=O, phthalazinyl), 1524, 1339 (NO_2). 1H -NMR (400 MHz, DMSO- d_6 , ppm) δ : 2.44 (s, 3H, CH_3), 3.92 (s, 3H, OCH_3), 4.36 (bs, 2H, NH_2), 4.78 (s, 2H, $NCH_2C=O$), hydrazide, 7.75–8.38 (m, 6H, Ar-H), 9.29 (bs, 1H, $NH-NH_2$). MS m/z : 384 ($M^+ + 1$).

[4-(4-Methoxy-5-methyl-3-nitro-phenyl)-1-oxo-1H-phthalaz-2-yl]acetic acid hydrazide (3). Compound **2** (4 g, 0.01 mol) was reacted with 2 mL hydrazine hydrate in 50 mL absolute ethanol at reflux for 4 h followed by cooling to room temperature. The obtained solid was filtered off followed by crystallization from ethanol to produce compound **3** in yield 90% as off-white crystals. m.p. 237–240 °C. FTIR (ν , cm^{-1}): 3316 (NH_2), 1672 (C=O, acetic acid hydrazide), 1650 (C=O, phthalazinyl), 1524, 1339 (NO_2). 1H -NMR (400 MHz, DMSO- d_6 , δ ppm): 2.44 (s, 3H, CH_3), 3.92 (s, 3H, OCH_3), 4.78 (s, 2H, $NCH_2C=O$), 5.14 (s, 2H, NH_2 hydrazide), 7.75–8.38 (m, 6H, ArH), 9.29 (bs, 1H, $NH-NH_2$). MS m/z : 384($M^+ + 1$).

[4-(3-Amino-4-methoxy-5-methyl phenyl)-1-oxo-1H-phthalaz-2-yl] acetic acid hydrazide (APPH). 0.01 mol of compound **3**, 30 mg $FeCl_3$ and 3.0 g active charcoal were mixed in 50 mL 1,4-dioxan in 3 neck 250 mL round flask fitted with condenser ending with a balloon on the top. The steering mixture received 16 mL of hydrazine hydrate, which was added in drops. After four hours of addition, the reaction had reached a temperature of 60 °C. The system needs to be periodically opened as the reaction takes place to allow the surplus gases to escape. The reaction mixture was filtered out after it had finished (confirmed by TLC), and the resulting solution was evaporated. The target product, APPH, was obtained from recrystallizing the acquired precipitate from ethanol in an 80–90% yield with off-white crystals. m.p. 260–265 °C. FTIR ATR (ν , cm^{-1}): 3377 and 3177 (NH_2), 1671 (C=O). 1H -NMR (400 MHz, DMSO- d_6 , ppm) δ : 2.24 (s, 3H, CH_3 Ar), 3.69 (s, 3H, OCH_3), 4.89 (s, 2H, $N-CH_2-C=O$), 5.08 (bs, 2H, NH_2-NH), 6.76 (bs, 2H, Ar NH_2), 7.76–8.37 (m, 6H, Ar-H), 10.36 (bs, 1H, $CH_2-C=ONHNH_2$). MS m/z : 354 ($M^+ + 1$).

Corrosion study. *Apparatus, materials and solution preparation for corrosion measurements.* The electrochemical studies (EIS and PDP) were examined at room temperature via a Gamry Potentiostat/Galvanostat (Model reference 3000). The electrochemical cell was a conventional three-electrode system used a saturated calomel electrode (SCE) as a reference electrode, graphite rod as a counter electrode and steel rod as the working electrode in wt % was as follows; 98.62 Fe, 0.68 C, 0.662 Mn, 0.015 P, 0.249 Si, 0.022 S, 0.027 Ni, and 0.031 Cu. The steel was mechanically cut in standard cylindrical coupons with a total surface area of 4.08 cm^2 and used for weight loss measurements; Teflon covered other cylindrical coupons, and only one exposed surface with an exposed area of 0.64 cm^2 for the electrochemical study. Then, samples were polished using SiC paper of various grades (#220 to #1200), washed with double-distilled water, degreased with acetone in an ultrasonic bath for 5 minutes, and air-dried before use. The pure H_2SO_4 of 98 percent analytical quality was used to create the corrosive medium containing 0.5 mol L^{-1} of H_2SO_4 .

Technical conditions for corrosion measurements. Electrochemical measurements conditions. EIS experiments were performed at measured EOCV using a sinusoidal voltage signal of 10 mV peak to peak. The analysis was carried out in the frequency range of 0.1 Hz to 100 kHz. The PDP test was performed using a potential range of –250 to +250 mV versus SCE at EOCV with a sweep rate of 0.1 $mV s^{-1}$. Each test was replicated at least three times to ensure reproducible results. The experimental data were analyzed using Echem Analyst 6.0 software.

Gravimetric study conditions. The calculated average values of low carbon steel (LCS) coupons were achieved by immersion of steel samples into 0.5 M H_2SO_4 using calculated concentrations of APPH for different periods at 303 ± 2 K. LCS coupons were removed after a specific amount of time, rinsed with distilled water and acetone, and then dried in a low oven before being reweighed. Using mathematical relationships, the corrosion rate, C_R ($mg cm^{-2} h^{-1}$), and inhibition efficiency (IE) were determined from the weight loss of the examined LCS coupons using equations (1, 2):

$$C_R = \frac{\Delta m}{At} \times 365 \quad (1)$$

$$E\% = \left(\frac{C_{R_0} - C_R}{C_{R_0}} \right) \times 100 \quad (2)$$

where C_{R_0} and C_R are the corrosion rates of LCS due to the dissolution in 0.5M H_2SO_4 mixed with calculated concentrations of APPH, respectively.

Surface study. LCS samples were exposed to 0.5 M H_2SO_4 containing calculated concentrations of APPH. After removing the samples from the corrosive solution and drying it, the surface morphology and structure were investigated using a scan electron microscope (SEM lined to energy dispersive X-ray (EDX) spectroscopy

[APPH] (mM)	Weight loss (g) 1 day	Weight loss (g) 3 days	Surface area (cm ²)	CR (g/cm ² .year) 1 day	CR (g/cm ² .year) 3 days	E (%) 1 day	E (%) 3 days
0.0	0.3746	1.4686	4.08	5.69704	22.33496	0	0
0.05	0.2461	0.5851	4.08	3.7427	8.89916	34	60
0.1	0.1365	0.2849	4.08	2.07594	4.33285	63	81
0.2	0.0765	0.2549	4.08	1.16344	3.8766	79	83
0.4	0.0718	0.1779	4.08	1.09196	2.70556	81	88
0.5	0.0542	0.1124	4.08	0.82429	1.70942	86	92

Table 1. Effect of APPH concentrations on the corrosion rate of carbon steel in 0.5 M H₂SO₄.

(JEOL-JSM-5300LV, Tokyo, Japan) and Bruker FTIR. The same techniques should be used in the case of a synergistic effect.

Adsorption isotherm and determination of adsorption thermodynamics parameters. The mechanism by which organic inhibitors attach to the LCS surface is discussed in the adsorption isotherm. Fitting the linear isotherm models (Freundlich, Langmuir, Frumkin, Temkin, and Flory Huggins isotherm models) expressed in linear equations with the corrosion rate (C_R) and the percentage of θ of the APPH using the following Eqs. (3–9)^{47–51}.

The Langmuir adsorption isotherm model (Eq. 3):

$$\frac{C_R}{\theta} = \left(\frac{1}{K_{ads}} \right) + C_R \quad (3)$$

Frumkin adsorption isotherm model (Eq. 4):

$$\log \left[C_R \left(\frac{\theta}{1-\theta} \right) \right] = 2 \alpha \theta + 2.303 \log K_{ads} \quad (4)$$

Temkin adsorption isotherm model (Eq. 5):

$$\theta = \ln C_R + K_{ads} \quad (5)$$

Freundlich adsorption isotherm (Eq. 6):

$$\log \theta = \log K_{ads} + n \log C_R \quad (6)$$

Flory–Huggins adsorption isotherm (Eq. 7):

$$\log \left(\frac{\theta}{C_R} \right) = b \log(1-\theta) + \log K_{ads} \quad (7)$$

$$K_{ads} = K^{\frac{1}{y}} \quad (8)$$

El-Awady's thermodynamic/kinetic adsorption isotherm model (Eq. 9):

$$\log \frac{\theta}{1-\theta} = y \log C_R + \log K \quad (9)$$

Change of adsorption Gibbs free energy (ΔG_{ads}) is expressed in Equation (10) and was used to clarify the ability and nature of the adsorption. K_{ads} is a constant of the adsorption equilibrium that was achieved from the isotherm models.

$$\Delta G^{\circ} = -RT \ln K \quad (10)$$

Results and discussions

Weight loss measurements. The effects of APPH concentration on steel LCS corrosion are shown in Table 1. According to the findings, adding APPH to 0.5 M H₂SO₄ dramatically reduces the corrosion rate (C_R) of LCS while increasing the IE%. In the presence of APPH, a maximum IE of 92% was obtained at 0.5 mM. Adding a higher concentration of APPH had no discernible effect on inhibition efficiencies above the used concentrations. As a result, 0.5 mM is chosen as the optimum concentration and used in subsequent immersion time studies. The enhanced performance of APPH at very low concentrations may be attributable to the hydrazide group's interaction with the steel surface through N or O atom and NH₂.

Electrochemical study. *Tafel extrapolation technique.* Figure 1 displays the polarization graphs of LCS in 0.5 M H₂SO₄ with different APPH concentrations. The electrochemical properties are summarized in Table 1. The findings indicated that the APPH molecule is an effective corrosion inhibitor since it demonstrated a steady

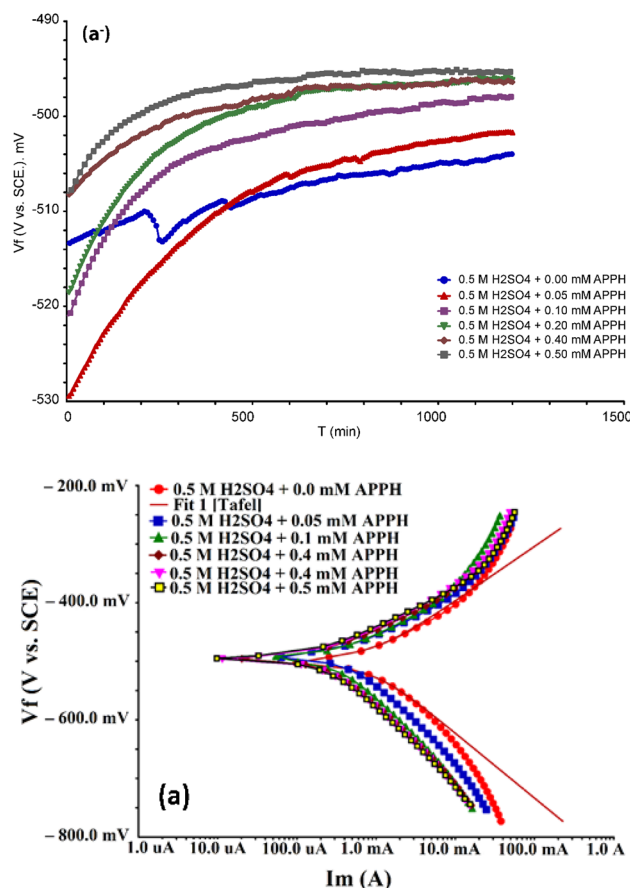


Figure 1. (a⁻) OCP and (a) Tafel polarization graph for LCS in 0.5 M H₂SO₄ with different concentrations of APPH at 303 K.

[APPH] (mM)	$-E_{\text{corr}}$	I_{corr} (μA)	β_a	β_c	E %
0.00	500	900	57.1	99.80	0
0.05	491	480	82	140	45
0.10	495	364	78	153	59
0.20	493	158	68	131	72
0.40	491	222	68	120	75
0.50	492	189	72	119	79

Table 2. Tafel polarization parameters were obtained at different concentrations of APPH for LCS in 0.5 M H₂SO₄ at 303 K.

decrease in corrosion current density relative to APPH concentration while increasing inhibition efficiency. The fact that all of the displacements are less than 85 mV and that E_{corr} is minimally shifted shows that the APPH molecule functions as a mixed-type inhibitor^{52,53}. Table 2 shows that the inhibitory efficiency of APPH varies from 45 to 79% as concentration increases, with 0.5 mM being the ideal concentration. Further evidence that the APPH compound works as a corrosion prevention agent by lowering the polarization potential came from the reduction in Tafel slopes data from the cathodic and anodic areas. While reducing hydrogen evolution at the cathodic site, the Tafel slopes, on the other hand, have validated metal oxidation at the anodic site^{54–56}. Additionally, because the values of i_{corr} and C_R decreased, the Tafel slopes without inhibitor values were larger than those cited in the absence of APPH.

$$C_R(\text{mpy}) = t \times M \times \frac{i_{\text{corr}}}{F} \quad (11)$$

where M is the equivalent molar weight of iron, i_{corr} is the corrosion current density (A cm^{-2}), t is the immersion time (s), and F is the Faraday constant⁵⁷.

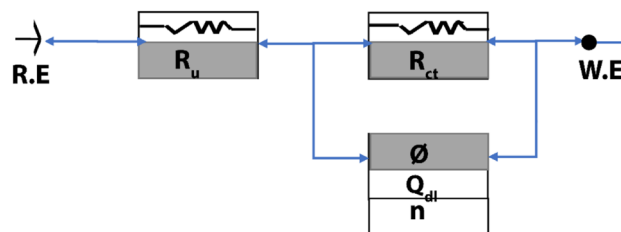


Figure 2. An inhibited system's equivalent electrical circuit (CPE) with an inhibited system.

[APPH] (mM)	R_s (ohm)	R_{ct} (ohm)	I_{cor}	n	Goodness of fit $\times 10^{-6}$	IE%
0.00	2.3	15	461	0.88	72.27	0
0.05	2.9	35	379	0.79	533	58
0.10	3.1	54	384	0.79	632	73
0.20	2.2	71	388	0.83	598	77
0.40	2.4	79	391	0.92	963	82
0.50	2.3	91	463	0.87	798	84
0.05 + 100 mM KI	6.0	107	355	0.80	221	86
0.10 + 100 mM KI	2.5	116	424	0.88	467	87
0.20 + 100 mM KI	4.8	143	519	0.71	313	90
0.40 + 100 mM KI	1.9	160	580	0.69	925	91
0.50 + 100 mM KI	2.4	194	772	0.77	1480	93
0.40 + 1 h	5.1	98	420	0.79	980	85
0.40 + 2 h	3.5	116	579	0.83	1020	87
0.40 + 6 h	4.8	123	613	0.91	1350	88

Table 3. The current comparable circuit simulation settings and associated inhibition efficiency (IE) of LCS in 0.5 M H_2SO_4 containing different APPH concentrations at 303 K.

Measurements made using EIS. EIS is a supplemental method for testing the affectivity of APPH, which is used to cover the surface of LCS in 0.5 M H_2SO_4 and to clarify the surface chemistry and kinetic properties of the LCS/electrolyte interface processes. Diverse corrosion systems, such as charge transfer regulation, diffusion control, or a mixed type, may exhibit different characteristics in their EIS analysis. EIS data is typically converted into equivalent electrical circuits in practice, which are then used to categorize the electrical properties of the electrochemical boundary. One of these circuits is the constant phase element model (CPE)⁵⁸, which is broken down into three components CPE, solution resistance (R_s), and charge transfer resistance (R_{ct}) (Fig. 2).

No nature effect of impedance diagrams with the presence of APPH with and without 100 mM KI compared with 0.5 M H_2SO_4 ; accordingly, the existence of APPH does not affect the corrosion mechanism (Table 3). The Nyquist grave and bode plot lines grave for LCS in 0.5 M H_2SO_4 electrolyte at calculated quantities of APPH are depicted in Fig. 3a,b. The observed single depressed capacity semicircles on the obtained plots for the LCS/electrolyte interface in the analyzed sulfuric acid environments with and without varied APPH amounts suggest that a charge transfer mechanism structures the corrosion behavior on the surface of LCS. The protective layer and adsorption formation at the LCS-electrolyte interface are connected to how the size of the Nyquist semicircle changes as APPH concentration increases⁵⁹.

Synergism consideration. When the combined effect of multiple compounds is greater than the sum of the activities of the individual compounds, this is known as the synergistic effect of APPH inhibitors. For the purpose of determining the synergism parameter (S), the formula that follows should be utilized as in equation (12).

$$S = \frac{1 - (\eta_1 + \eta_2)}{1 - \eta'_{1+2}} \quad (12)$$

where η^1 is the inhibitory action of iodide, η^2 is the IE of the APPH and η'_{1+2} is IE of iodide + APPH. The values of S are calculated as 1.81, 1.79, 1.83 and 1.81 with respect to 0.1, 0.2, 0.4 and 0.5 Mm APPH, respectively, which are more than unity, showing that the enhanced IE is also a function of KI⁶⁰. Addition KI into 0.5 M H_2SO_4 corrosive media, I^- anion quickly absorbs into the anodic area of the LCS; thus, the positive excess charge on the anodic area of the steel surface is reduced, and the surface will be negatively charged. Accordingly, the protonated APPH is attracted to the negative surface of the steel, forming a protective layer through physical adsorption.

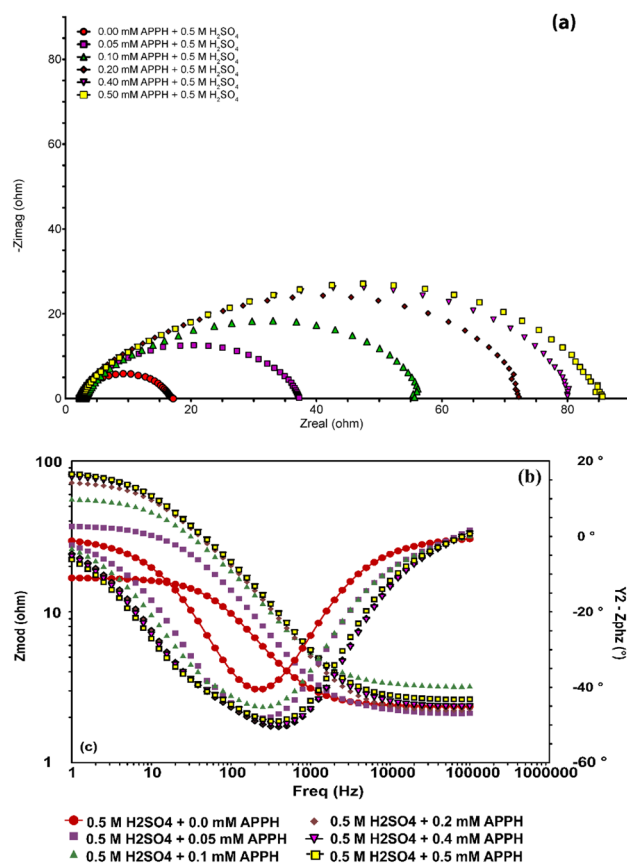


Figure 3. (a) Nyquist grave and (b) bode plots grave of LCS obtained at different APPH concentrations in 0.5 M H₂SO₄ at 303 K.

The previous investigation approves the shift in corrosion potential to a less negative value; thus, the inhibition in the case of adding KI is an anodic inhibitor (Tables 2, 3; Fig. 4).

The influence of exposure duration on the corrosion behavior of LCS in 0.5 M H₂SO₄. In the absence of APPH, an increase in the immersion time to 1, 2, and 6 h led to an increase in the corrosion of the LCS, as shown by an increase in the values of i_{corr} and a decrease in the values of R_p . This was confirmed by the fact that the values of i_{corr} increased while the R_p values decreased (Fig. 5). This is due to the fact that prolonging the duration of immersion results in a greater degree of LCS being dissolved by the caustic action of 0.5 M H₂SO₄ solution. According to some reports, the cathodic reaction for metals and alloys in H₂SO₄ solutions is the hydrogen evolution, which results in the consumption of electrons at the cathode. The increase in the anodic currents with potential and with the increase in immersion time indicates that increasing the applied voltage in a less negative direction makes it easier for steel to corrode⁶¹. The reduction in the corrosion parameters for the LCS was due to the inclusion of APPH. Whereas, the i_{corr} values go down while the R_p and $IE\%$ values go up when there is an increase in the amount of APPH present as well as when the exposure period of the LCS goes up from 0 to 6 h before the electrochemical measurements are taken. This was further corroborated by the electrochemical results shown in Table 3, which demonstrates that APPH is a good corrosion inhibitor for the LCS when immersed in a solution containing 0.5 M H₂SO₄ and its effectiveness rises with the increase of immersion time.

Surface study. FTIR spectra were analyzed so that researchers could better understand the interaction of APPH molecules with the steel surface. Figure 6 displays the infrared (FTIR) spectra of pure APPH as well as scrapped samples collected from LCS surfaces following corrosion experiments conducted in the presence of APPH. It was discovered that the peaks that appear in the spectrum of pure APPH do not appear in the scrapped samples' spectra in the same way. The N–H stretching frequencies for APPH were observed to be at 3377 cm⁻¹, the C=C stretching frequencies for individual APPH were recorded to be at 1612 cm⁻¹, and almost completely disappeared with a noticeable reduction in peak integration in the scrapped sample. The stretching frequencies of the C–H, C–O group, almost disappeared in the scrapped sample.

The surface morphology of the corroded coupon was characterized with the aid of SEM after immersion in 0.5 M H₂SO₄ solution and is a function of 0.5 mM APPH and in the case of adding 100 mM KI. The surface images presented in Fig. 7 are indicated that the surface of LCS before and after immersion in 0.5 M H₂SO₄ solution while LCS, which corroded in 0.5 M H₂SO₄, exhibit a more severe grain border attack than the presence of 0.5 M H₂SO₄ (Fig 7a,b). The attack is more extreme in the case of addition APPH (Fig. 7c) than in the addition of

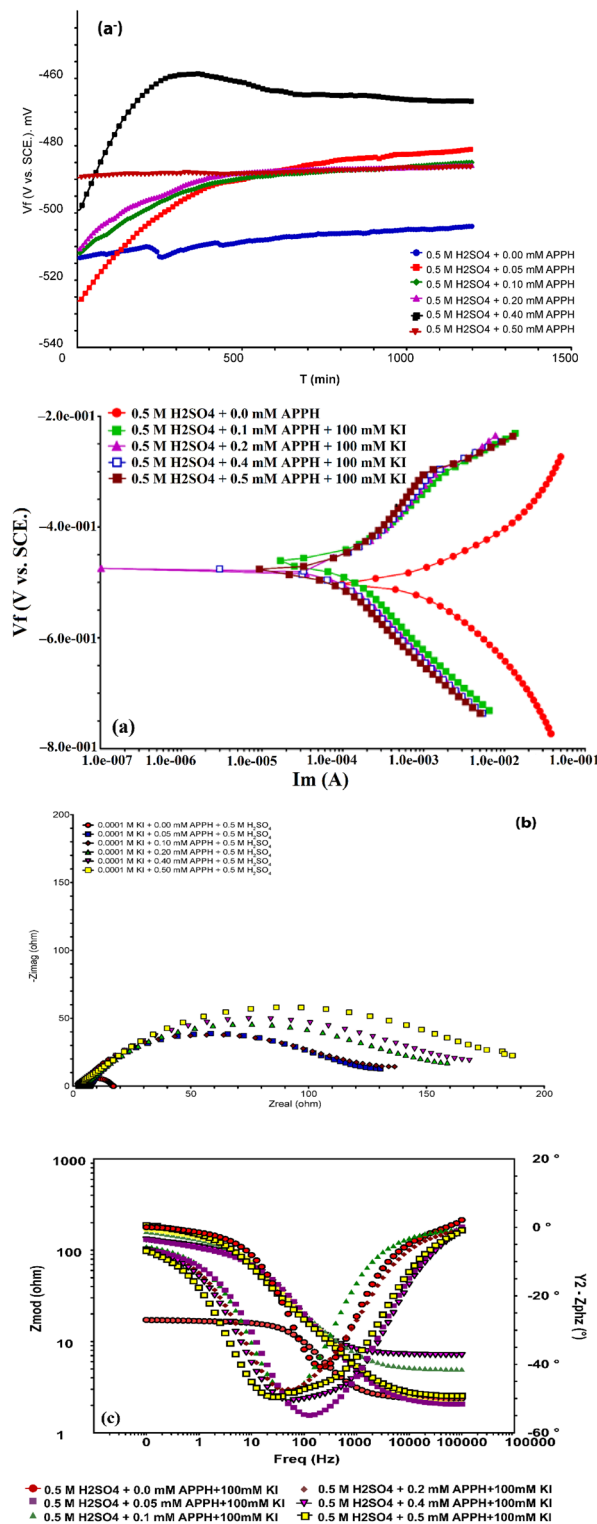


Figure 4. Synergistic effect of KI + APPH on LCS corrosion in 0.5 M H₂SO₄ using (a⁻) OCP (a) Tafel; (b) Nyquist grave; and (c) Bode plots grave.

APPH and 100 mM KI (Fig. 7d). Metals and alloys often have the lowest energy and are most susceptible to corrosion attack near grain boundaries and areas of discontinuity. They offer APPH microcell molecules to adsorb at grain boundaries and discontinuities, lowering the rate of corrosion and the amount of hydrogen evolution.

Computational calculations. Quantum chemical calculations have been employed extensively to provide a better understanding, on a molecular level, of the relationship that exists between the structure of inhibitors

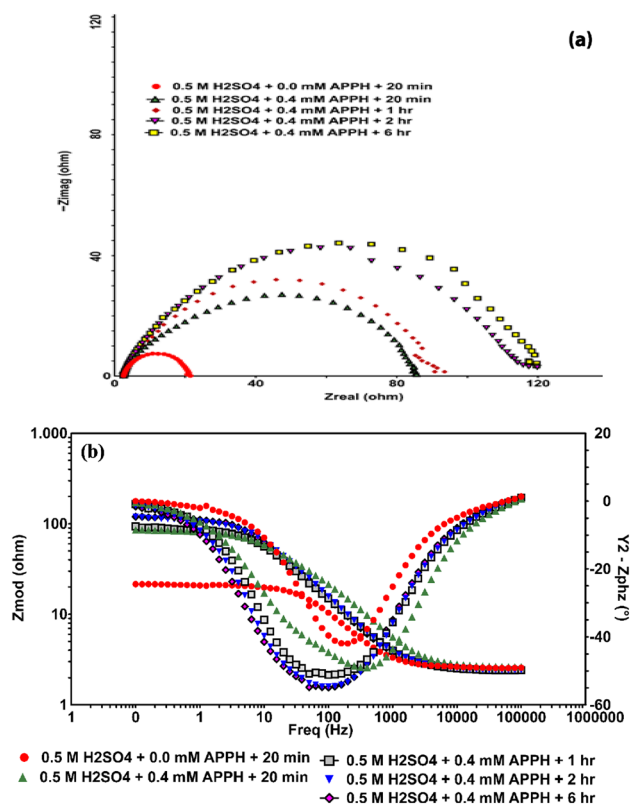


Figure 5. Impact of 6 h Immersion period of LCS corrosion in 0.5 M H₂SO₄ containing 0.4 mM APPH (a) grave of Nyquist; and (b) grave of bode plots.

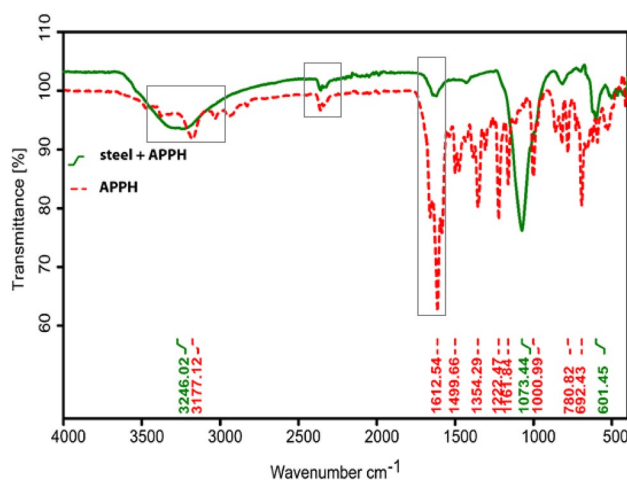


Figure 6. IR spectrum of APPH separately and on the LCS surface in 0.5 M H₂SO₄.

and the activities that they perform. The chemical reactivity of the APPH inhibitor can be anticipated by using this method, which involves conducting an analysis of the quantum chemical indices. According to the frontier orbital theory, the reaction that takes place between reactants typically takes place on the HOMO and LUMO, and the creation of a transition state is controlled by an interaction that takes place between the frontier orbitals of the reactants. As a consequence of this, analyzing the distribution of HOMO and LUMO was necessary to discover the inhibition mechanism. On the one hand, the unoccupied d orbitals of the Fe atom have the ability to accept electrons^{42,44,62,63}. Equations (13–19) provide a summary of the computed quantum descriptors, which include E_{HOMO} , E_{LUMO} , $E_{\text{HOMO}} - E_{\text{LUMO}}$ energy gap (ΔE), dipole moment (μ) and total energy (TE), electronegativity (χ), electron affinity (A), global hardness (η), softness (σ), ionization potential (I). The overall electrophilicity,

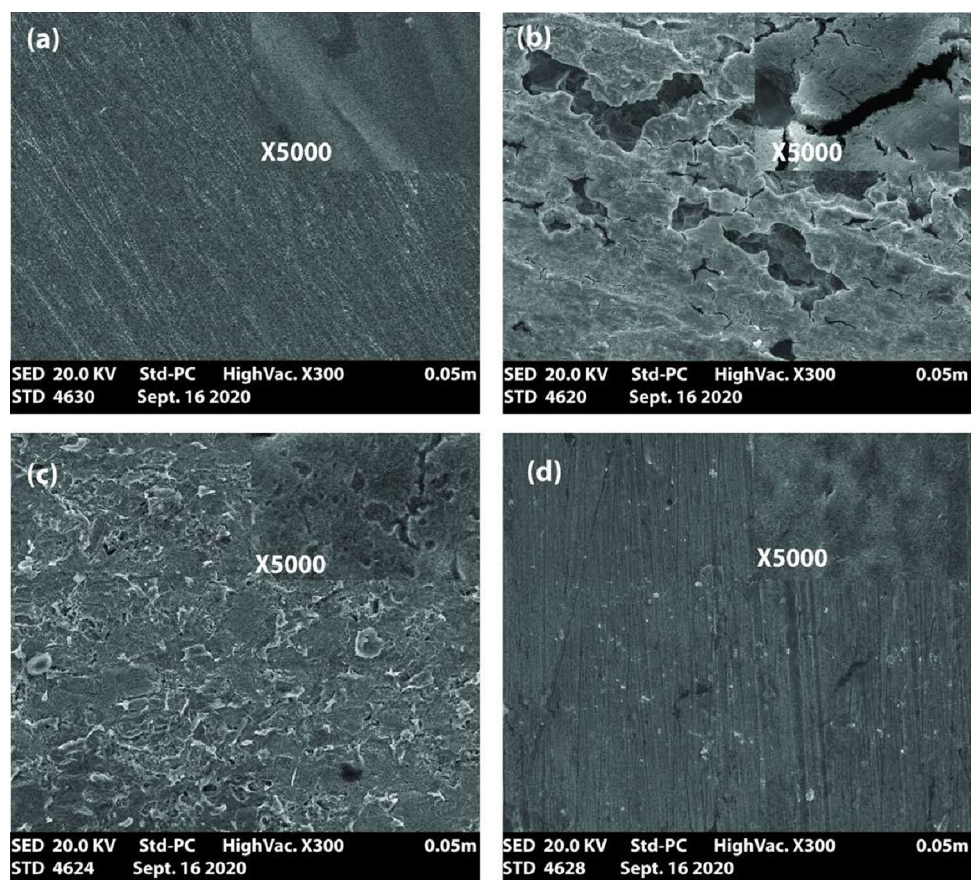


Figure 7. The SEM image of LCS specimens of (a) before treatment with 0.5 M H₂SO₄; (b) corroded; (c) inhibited by APPH; and (d) inhibited by APPH with 100 mM KI.

denoted by the symbol (ω), as well as the fraction of electrons that are transported from the inhibitor to the iron surface, is denoted by the symbol (ΔN).

$$\Delta E = ELUMO - EHOMO = I - A \quad (13)$$

$$-ELOMO = I \quad (14)$$

$$A = -ELUMO \quad (15)$$

$$\eta = \frac{I - A}{2} = \frac{ELUMO - EHOMO}{2} = \frac{\Delta E}{2} \quad (16)$$

$$X = \frac{I + A}{2} \quad (17)$$

$$\delta = I/\eta \quad (18)$$

$$\Delta N = \frac{X_{Fe} - X_{inh}}{2(\eta_{Fe} + \eta_{inh})} \quad (19)$$

Because APPH molecule contains hetero-atoms (N and O), a hydrazide group, and a benzene ring in addition to a benzene ring and is resonant on the whole APPH inhibitor molecule, the APPH corrosion inhibitor molecule has unique properties in terms of stability as well as the sensitivity of APPH molecule to the formation of coordination bonds with the LCS surface. These properties are due to the fact that APPH molecule is resonant on the whole inhibitor molecule. In the case of APPH molecule, HOMO and LUMO were investigated, and the results are presented in Fig. 8. Table 4 contains a listing of the E , μ and χ , and values that were calculated for the criterion energy of frontier molecular electrons. HOMO is the theory that describes how the contribution electrons of APPH molecule have an effect. It should come as no surprise that APPH molecule include more

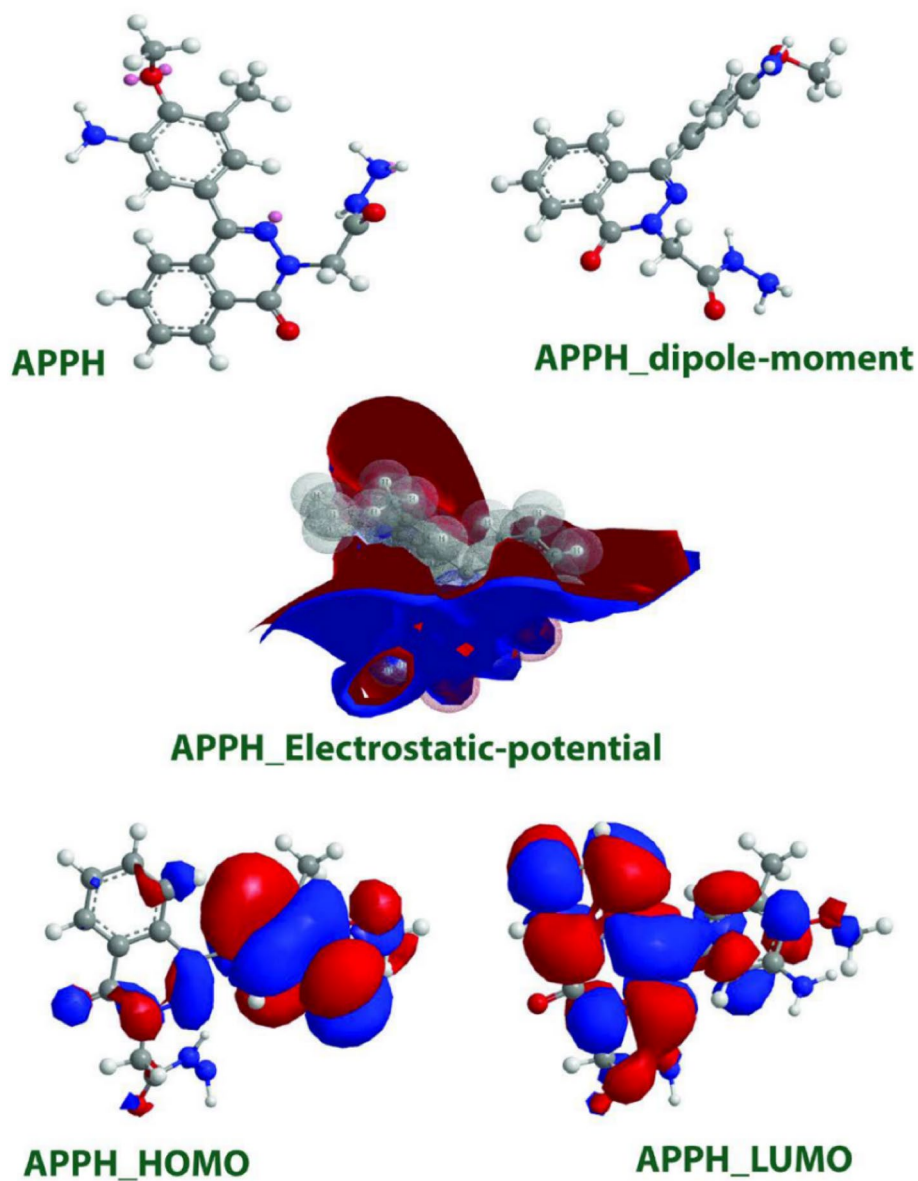


Figure 8. The frontier molecular orbital for protonated form of studied APPH.

Model	DFT31G	AM1	PM3
E_{HOMO} (eV)	-0.2033	-0.3105	-0.3161
E_{LUMO} (eV)	-0.0661	-0.3267	-0.0374
ΔE (eV)	0.1372	-0.0162	0.2786
I (eV)	0.2033	0.3105	0.3161
A (eV)	0.0661	0.3267	0.0374
η	0.0686	-0.0081	0.1393
δ	14.5751	-123.6094	7.1780
μ (Debye)	5.8158	-	-
X	0.1347	0.3186	0.1768
ΔN	50.0316	-412.9413	24.4886

Table 4. The quantum chemical parameters of the APPH inhibitors that were examined.

electrons. E_{HOMO} is a marker for inhibitive action and serves as a signal. Because **APPH** molecule also contains O and N in addition to the hydrazide group, the **APPH** particles used as a corrosion inhibitor have the ability to donate unshared pairs of electrons to the free orbitals of iron atoms, which are referred to as d-orbitals. A better explanation of LUMO could be found in the affinity calculations performed on **APPH** molecule. On the other hand, E is also an important quantity that specifies the bonding of **APPH** to the steel surface.

A smaller value for E was associated with a more significant degree of inhibition in most cases. According to Table 4, **APPH** has an E value equal to 0.1372 eV. **APPH** has a minimal value of χ , demonstrating that it is quite effective at inhibiting activity. In this investigation, the value of χ supported the methodological findings. The high value of μ indicated that the corrosion inhibitor was superior to the others. According to the findings of this research, the value of the dipole moment μ of **APPH** molecules was 5.8158, which indicates that the **APPH** molecules have effective inhibitory control. As seen above, **APPH** molecules can adsorb on the LCS surface by exchanging water for more **APPH** molecule^{5,64–67}.

The HOMO/LUMO for **APPH** showed that the HOMO orbital was localized on pyridine, but the LUMO orbital was switched to the benzene ring. DFT studies⁶⁵ were used to estimate hardness and softness values. The **APPH** has a value of 0.0686, indicating that **APPH** as a corrosion inhibitor is expected to be a perfect inhibitor. **APPH** molecules have a chemical softness of 14.57, indicating that they have a higher inhibition efficiency⁶⁶.

The calculations for HOMO and LUMO on **APPH** showed that the HOMO orbital was situated on the pyridine atom, whilst the LUMO orbital was moved to the benzene ring. This was discovered by comparing the two orbitals. To make estimations about the values of hardness and softness, DFT research was applied⁶⁵. In light of the fact that the **APPH** has a value of 0.0686, one can conclude that the **APPH**, when employed as a corrosion inhibitor, ought to perform at the level of an ideal inhibitor. The chemical softness of **APPH** molecules is 14.57, which implies that they are more effective in suppressing activity than other molecules⁶⁶.

Adsorption isotherms. Figures 9 illustrates the different adsorption models that were investigated in this study. To choose the most suitable model, we considered the R^2 values presented in Table 5 for each isotherm model. The data were compatible with the isotherms of Langmuir, Flory-Huggins, and Temkin, but the Langmuir isotherm offered the best fit for the data. The Langmuir isotherm, which has R^2 values of 0.99, provides the most accurate description of the adsorption mechanism of **APPH** on LCS in a medium of sulfuric acid. As a consequence of this finding, the Langmuir adsorption isotherm is an appropriate tool for determining the adsorption equilibrium constant (K_{ads}).

Table 6 reported the Gibb's free energy change of adsorption (ΔG_{ads}) at room temperature. The ΔG_{ads} of **APPH** as LCS corrosion inhibitor is negative and have value of 33.3 kJ/mol. This finding suggests that the **APPH** adsorption on the LCS surface occurred spontaneously, was possible, and instead followed the physical adsorption mechanism (Fig. 10).

When a metallic substrate is positively charged in H_2SO_4 , many published works have shown that chloride ions and negative species first adsorb onto the surface of the substrate. Because of this, the negatively charged surface that was produced as a result is what makes the adsorption of protonated **APPH** possible via electrostatic attraction. It is important to point out that the protonation of the amino-functional group found in **APPH** results in a favorable state in H_2SO_4 . Consequently, following the initial adsorption of I^{1-} and SO_4^{2-} species, the protonated **APPH** will adsorb via electrostatic contact on the first created layer of the negative species. This will occur after the initial adsorption of I^{1-} and SO_4^{2-} species. As mentioned earlier, **APPH** is considered a mixed adsorption inhibitor, which suggests that it inhibits both physisorption and chemisorption. Other un-protonated **APPH** induces coordination interactions with d empty molecular orbitals of metal, in addition to the apparent physical adsorption of the protonated molecule. Figure 10 shows a diagrammatic representation of the adsorption process in its basic form. Koumya et al.⁶⁷ made observations that were very similar to these ones.

Conclusion

[4-(3-Amino-4-methoxy-5-methyl phenyl)-1-oxo-1H-phthalaz-2-yl] acetic acid hydrazide (**APPH**) was prepared and tested as a low carbon steel (LCS) corrosion inhibitor in 0.5 M H_2SO_4 . The corrosion percentage of LCS in 0.5 M H_2SO_4 decreased with increases in the concentration of **APPH**, which is a mixed-type inhibition. **APPH** behaves as a mixed-type inhibitor and makes passivation. The adsorption of **APPH** has performed the inhibitory effect through the coordination bond of their heteroatoms with LCS surface. The adsorption of the **APPH** on the LCS follows the Langmuir adsorption isotherm model. The impact of exposure time using 0.4 mM of **APPH** shows that it maximized the inhibition efficiency to 88% after 6 hours of contact time. The value of free energy of adsorption ($-\Delta G^{\circ}_{\text{ads}}$) was 33.3 kJ mol⁻¹. The application of Quantum chemical calculations to **APPH** supported the experimental results.

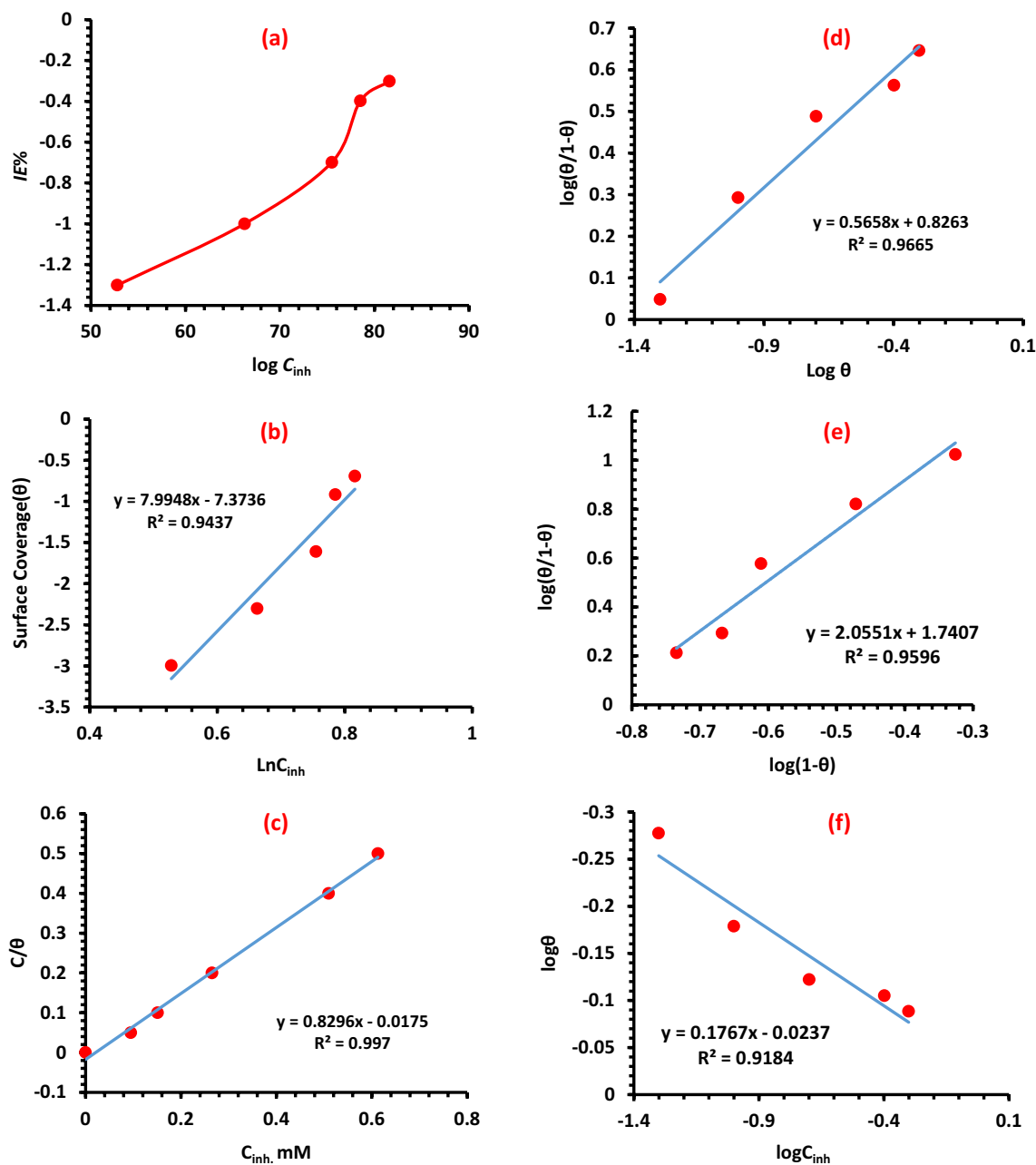


Figure 9. (a) Corrosion of carbon steel in 0.5 M H₂SO₄ solution and the relationship between the IE% and APPH concentration, (b) Temkin adsorption isotherm, (c) Langmuir adsorption isotherm plot, (d) Kinetic-thermodynamic model, (e) Flory–Huggins adsorption isotherm, and (f) Freundlich adsorption isotherm.

	Langmuir	Temkin	El– Awary’s	Flory–Huggins	Freundlich
R ²	0.9970	0.9437	0.0.9665	0.0.9596	0.9184
K	57.14	7.994	4.826	112.202	1.4996

Table 5. R² Values for the various adsorption isotherms considered for APPH at 303 K.

Kads (L/g)	R ²	− ΔG ^o _{ads} (KJ mol ^{−1})
57.14	0.9970	33.63

Table 6. Thermodynamic parameters of (APPH) adsorption on LCS in 0.5 M H₂SO₄.

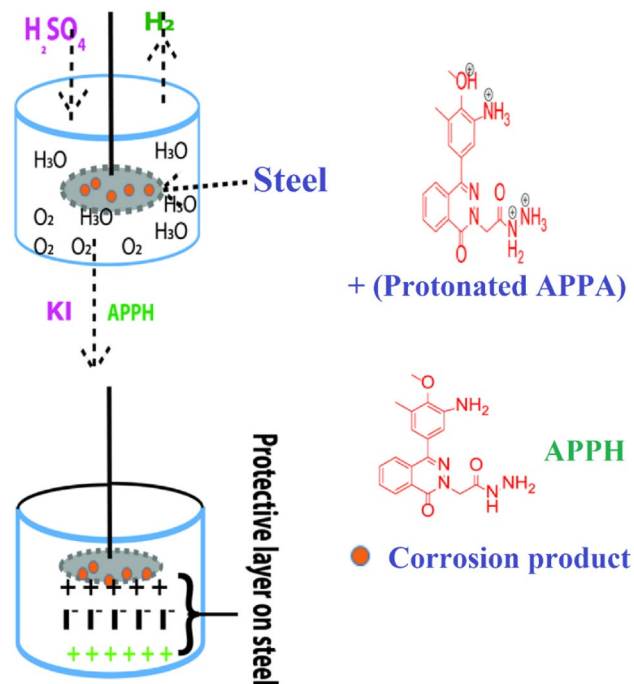


Figure 10. The mechanism of the APPH adsorption on the surface of LCS in 0.5 M H₂SO₄.

Data availability

This article contains all of the data that was generated or processed while this study was being conducted, and it was published. It is recommended that anyone who is interested in requesting data from this study get in touch with Professor Dr. A. El Nemr.

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Author contributions

R.S.A. did the APPH synthesis, structural elucidation, and original manuscript writing, while N.A.B. conducted the corrosion investigation and original manuscript writing. S.R. edited the original text and oversaw the laboratory work. The work was supervised by S.S.A.E.-S., the late M.A.E.-H., and M.H.S. A.E.N. oversaw the project, offered financial assistance, edited the final manuscript and submitted for the Journal.

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Competing interests

The authors declare no competing interests.

Additional information

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