



OPEN

A numerical study on the effect of CO₂ addition for methane explosion reaction kinetics in confined space

Jingyan Wang^{1,2,3}, Yuntao Liang^{2,3}✉, Fuchao Tian^{2,3} & Chengfeng Chen^{1,2,3}

To explore the influence of the CO₂ volume fraction on methane explosion in confined space over wide equivalent ratios, the explosion temperature, the explosion pressure, the concentration of the important free radicals, and the concentration of the catastrophic gas generated after the explosion in confined space were studied. Meanwhile, the elementary reaction steps dominating the gas explosion were identified through the sensitivity analysis. With the increase of the CO₂ volume fraction, the explosion time prolongs, and the explosion pressure and temperature decrease monotonously. Moreover, the concentrations of the investigated free radicals also decrease as the increase of the CO₂ volume fraction. For the catastrophic gas, the concentration of the gas product CO increases and the concentrations of CO₂, NO, and NO₂ decrease as the volume fraction of CO₂ increases. When 7% methane is added with 10% CO₂, the increase rate of CO is 76%, and the decrease rates of CO₂, NO, and NO₂ are 27%, 37%, and 39%, respectively. If the volume fraction of CO₂ is constant, the larger the volume fraction of methane in the blend gas, the greater the mole fraction of radical H and the lower the mole fraction of radical O. For radical OH, its mole fraction first increases, and then decreases with the location of peak value of 9.5%, while the CO concentration increases with the increase of the methane concentration. For all the investigated volume fraction of methane, the addition of CO₂ reduces the sensitivity coefficients of each key elementary reaction step, and the sensitivity coefficient of reaction promoting methane consumption decreases faster than that of the reaction inhibit methane consumption, which indicates that the addition of CO₂ effectively suppresses the methane explosion.

Mine gas explosion accidents are one of the biggest factors, which endangers the safe production in coal mines. These accidents cause serious economic losses and casualties¹. In recent years, with the continuous increase in coal production, the gas explosion accidents have occurred frequently^{2,3}.

To prevent the occurrence of gas explosions, many relevant researches had been conducted in the field of inert gas explosion suppression. In terms of the explosion suppression experiments, Lu et al. designed a device that can automatically eject nitrogen during the explosion process. The effects of injection pressure, injection timing, and nozzle arrangement on the explosion suppression function were studied. The results showed that successful explosion suppression can be achieved when the nitrogen pressure reaches or exceeds 0.3 MPa^{4,5}. Cao et al. studied the suppression effect of ultrafine mist on methane/air explosions. With the increase of ultrafine water/NaCl solution mist, the flame propagation speed, the maximum explosion overpressure, and the maximum pressure rising rate descended^{6–8}. Based on the eddy dissipation concept combustion model, Wang et al. studied the mechanism and effect of ultrasonic water mist on suppressing gas explosion through experiments and EDC (Eddy-Dissipation Concept) combustion model⁹. Liang et al. investigated the influence of the nitrogen fraction in the blend of on the unstretched laminar flame propagation velocity, unstretched laminar combustion velocity, Markstein length, flame stability, and maximum combustion pressure. It was found that above parameters decrease distinctly with the increase of nitrogen fraction in the gas mixture¹⁰. Qian et al. obtained a fitting formula through experiments under different conditions, which can predict the explosion limit of methane at

¹China Coal Research Institute, Beijing 100020, China. ²State Key Laboratory of Coal Mine Safety Technology, China Coal Technology and Engineering Group Shenyang Research Institute, Fushun 113122, China. ³College of Emergency Management and Safety Engineering, China University of Mining and Technology (Beijing), Beijing 100080, China. ✉email: liangyuntao@sycrci.com

any ratio of N_2 to CO_2 . They reported that the limit oxygen volume fraction decreases linearly with the increase in N_2 content in the mixture¹¹. Furthermore, some researches had been carried out to research the inhibition effect of N_2 , CO_2 and N_2/CO_2 mixture on gas explosion, it was found that both N_2 and CO_2 can inhibit the gas explosion, and the inhibition effect on high concentration gas is better. At the same time, the higher the volume fraction of CO_2 in the mixed gas, the better the inhibition effect^{12–14}. The above researches show that the inert gas can inhibit the explosion, to deeply understand the behavior, many simulation works are performed.

Luo et al. used the (DFT) B3LYP/6-31G methods of density functional theory and the GRI-Mech 3.0 to analyze the related elementary reactions. The results indicated that the NH_3 could achieve explosion suppression by competing the free radicals H and OH, and the reactant of O_2 with CH_4 ^{15,16}. Liang et al. and Wang et al. found that the increase of the water content in the mixed gas can promote the generation of CO_2 but reduce the intensity of the gas explosion, and inhibits the generation of harmful gases, such as CO, NO, and NO_2 ^{17,18}.

Lu et al. suggested that the H_2O acts as the third body in the explosion process, which directly participated in the ternary collision reaction existing in the form of inert molecules. It would collide with the free radicals and the free atoms to destroy the chain carrier, which reduces the concentration of active centers in the chain reaction, and achieve the explosion suppression¹⁹. Ren et al. modified the reaction mechanism of GRI-Mech 3.0 by assuming that the N_2 , CO_2 , and H_2O only participated in the inhibition process as the third body. The physical and chemical effects of the three inert gases on the laminar combustion velocity, adiabatic flame temperature, and net heat release rate under different methane equivalence ratios ($\Phi = 0.8, 1.0$ and 1.2) were analyzed²⁰. Jia et al. indicated that the N_2 , CO_2 , and H_2O reduced the sensitivity of the elementary reaction steps dominating the gas explosions and the inhibition effect of CO_2 and H_2O were better than that of the N_2 ^{1,2,21}. Li et al. pointed out that the addition of N_2 , CO_2 , and H_2O would strongly inhibit the generation of free radicals CH_3 and HCO . The inhibitory effect of CO_2 and H_2O is not only from their participation in the three-body collision reaction, but also from their participation in another chain reactions^{22,23}.

Though a number of experiments and simulation had been performed to investigate the suppression effect of inert gas on methane explosion, most of the previous studies focused only on the independent influences of different volume fractions of inert gas on methane explosion mechanism under stoichiometric ratio condition. Because the working condition of coal mine is complicated, and the inhibition effect may be different in different conditions. However, the influence of inert gases with different volume fractions on explosions over wide methane equivalence ratios has not been reported. In this study, the influence of CO_2 volume fraction on methane explosion in confined space under different methane equivalent ratios was investigated to provide a theoretical basis for the improvement of the inert gas explosion suppression mechanism under complex working conditions.

Mathematical model

Governing equation. The composition equation is as follows.

$$\frac{dY_i}{dt} = \nu \dot{w}_i M_i \quad (i = 1, 2, \dots, k_g) \quad (1)$$

$$\dot{w}_i = \sum_{k=1}^{N_g} \nu_{ik} K_{fk} \prod_{j=1}^{k_g} [X_j]^{V'_{jk}} \quad (j = 1, 2, \dots, k_g) \quad (2)$$

$$K_{fk} = A_k T^{b_k} \exp \left[\frac{-E_k}{RT} \right] \quad (k = 1, 2, \dots, N_g) \quad (3)$$

where Y_i , w_i , and M_i denote the mass fraction, chemical reaction rate, and molecular weight of the substance i , respectively, t is the time, ν , R , and T represent the specific heat capacity, gas constant, and temperature of the mixture, respectively, and N_g and k_g are the total number of reaction steps and groups, respectively. The total number of points is the reverse stoichiometric coefficient, forward stoichiometric coefficient, and the difference between the forward and reverse stoichiometric coefficients of substance i in elementary reaction k . Here, K_{fk} is the rate constant of the positive reaction in the elementary reaction j , $[X_j]$ is the molar concentration of component j , and A_k , b_k , and E_{ak} are the pre-exponential factors, temperature index, and reaction activation energy of the elementary reaction k , respectively.

The energy equation is

$$c_v \frac{dT}{dt} + V \sum_{i=1}^{k_g} e_i \dot{w}_i M_i = 0 \quad (4)$$

where c_v is the constant volume specific heat of the mixed gas, and e_i is the internal energy of component i .

Sensitivity analysis. Sensitivity analysis is a method to determine the sensitivity factors that have an important impact on the overall response from multiple uncertain factors²⁴.

Assuming a variable, it is expressed as

$$\frac{dZ}{dt} = F(Z, t, a) \quad (5)$$

Reaction step	Elementary reaction
R32	$O_2 + CH_2O \rightleftharpoons HO_2 + HCO$
R38	$H + O_2 \rightleftharpoons O + OH$
R52	$H + CH_3(+M) \rightleftharpoons CH_4(+M)$
R53	$H + CH_4 \rightleftharpoons CH_3 + H_2$
R57	$H + CH_2O(+M) \rightleftharpoons CH_3O(+M)$
R98	$OH + CH_4 \rightleftharpoons CH_3 + H_2O$
R118	$HO_2 + CH_3 \rightleftharpoons O_2 + CH_4$
R119	$HO_2 + CH_3 \rightleftharpoons OH + CH_3O$
R155	$CH_3 + O_2 \rightleftharpoons O + CH_3O$
R156	$CH_3 + O_2 \rightleftharpoons OH + CH_2O$
R157	$CH_3 + H_2O_2 \rightleftharpoons HO_2 + CH_4$
R158	$2CH_3(+M) \rightleftharpoons C_2H_6(+M)$
R161	$CH_3 + CH_2O \rightleftharpoons HCO + CH_4$
R170	$CH_3O + O_2 \rightleftharpoons HO_2 + CH_2O$

Table 1. Main reactions affecting the change of free radicals.

7 vol% CH ₄ ($\varphi=0.72$)			9.5 vol% CH ₄ ($\varphi=1$)			11 vol% CH ₄ ($\varphi=1.18$)		
CO ₂	O ₂	N ₂	CO ₂	O ₂	N ₂	CO ₂	O ₂	N ₂
0	19.53	73.47	0	19.005	71.495	0	18.69	70.31
2	19.11	71.89	2	18.585	69.915	2	18.27	68.73
4	18.69	70.31	4	18.165	68.335	4	17.85	67.15
6	18.27	68.73	6	17.745	66.755	6	17.43	65.57
8	17.85	67.15	8	17.325	65.175	8	17.01	63.99
10	17.43	65.57	10	16.905	63.595	10	16.59	62.41

Table 2. Initial working conditions of methane explosion.

where $Z = (Y_1, Y_2, \dots, Y_{k_g})^t$ is the mass fraction of each component, and $a = (A_1, A_2, \dots, A_{N_r})$ is the prefactor of each elementary reaction.

$$w_{l,i} = \frac{\partial Z_l}{\partial a_i} \quad (6)$$

where $w_{l,i}$ is the sensitivity coefficient, Z_l is the variable number l , and a_i is the preference factor of the reactions i .

As the derivation of Eq. (6), one obtains

$$\frac{dw_{l,i}}{dt} = \frac{\partial F_l}{\partial Z} w_{l,i} + \frac{\partial F_l}{\partial a_i} \quad (7)$$

Reaction mechanism. The total chemical reaction formula of gas explosion is $CH_4 + 2(O_2 + 3.76N_2) \rightarrow CO_2 + 2H_2O + 7.52 N_2 + 882.6 \text{ kJ/mol}$, GRI-Mech 3.0 is selected as the chemical reaction mechanism of methane combustion, the mechanism includes 53 species and 325 elementary reactions²⁵. The study is performed by using a closed homogeneous 0-D reactor in CHEMKIN-Pro. Table 1 shows some key elementary reaction steps in the detailed mechanism of gas explosion chain reaction.

Simulation condition. To reveal the effect of carbon dioxide on the kinetic characteristics of the methane explosion over wide methane equivalent ratios, the explosion of different methane concentrations within the explosion limit was simulated by using a higher initial temperature instead of the high-temperature heat source ($> 650^\circ\text{C}$)²⁶. In the present study, the methane explosion is simulated with the constant volume combustion bomb model, with the initial temperature of 1300 K, the initial pressure of 1 atm, and the reaction time of 0.02 s. The specific working conditions are presented in Table 2.

Calculation results and analysis

Pressure and temperature. The variations of the pressure and temperature during the explosion process of 7% CH₄-air with different CO₂ additions are plotted in Fig. 1. With the increase of the CO₂ volume fraction, the explosion time prolongs and the explosion pressure and temperature decrease monotonously. When the

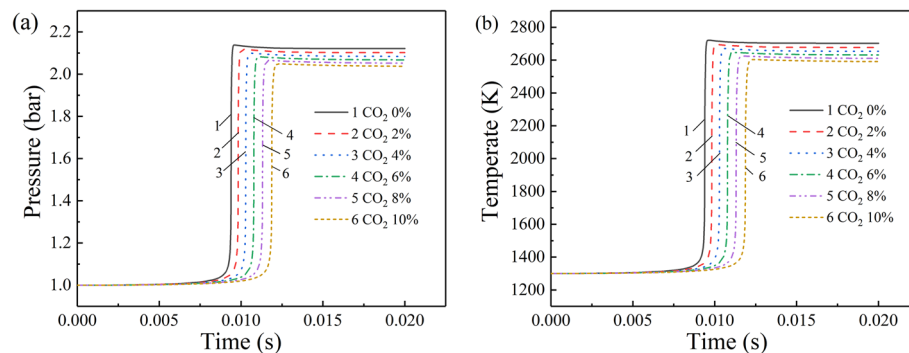


Figure 1. Variation of explosion pressure and temperature with time under different CO₂ volume fractions at 7% CH₄: (a) explosion pressure and (b) explosion temperature.

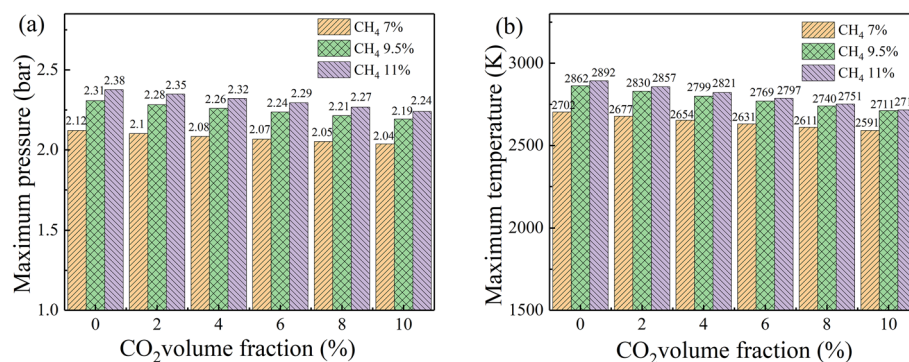


Figure 2. Variation of explosion pressure and temperature with CO₂ volume fraction under different methane volume fractions: (a) explosion pressure and (b) explosion temperature.

volume fraction of CO₂ increases from 0 to 10%, The maximum gas explosion pressure decreases from 2.12 to 2.04 MPa with the decrease rates of 3.77%. The maximum temperature decreases from 2702.882 K to 2591 K with the decline rates of 4.14%. These results indicate that the increase of the volume fraction of CO₂ would suppress the gas explosions. This conclusion agrees with the effect of water addition on methane explosion²⁷.

Figure 2 further displays the influence of the CO₂ volume fraction on the maximum explosion pressure and explosion temperature with different methane volume fraction. As seen, the maximum explosion pressure and explosion temperature decrease with the increase of the CO₂ volume fraction under all the methane volume fraction. The larger the methane volume fraction, the greater the maximum explosion pressure decrease, and the better the suppression effect on the methane explosion. When the volume fraction of methane is 7%, 9.5%, 11%, the maximum explosion pressure of adding 10% CO₂ is reduced by 3.9% compared with the case with no addition in Fig. 2a. As Fig. 2b shows, for methane with a volume fraction of 11%, the explosion temperature is more sensitive to changes in the CO₂ volume fraction than for 7% and 9.5% volume fractions. When the volume fraction of methane is 7%, 9.5%, 11%, the explosion temperature of the addition of 10% CO₂ decreases by 4.2%, 5.3%, 6.2% compared with the case with no addition. The results indicate that the inhibitory effect of CO₂ addition on the methane explosions increases as the increase of the methane concentration.

Free radicals. The essence of gas explosion is a complex thermal chain reaction. The chain-branching and chain-propagating reactions initiated by free radicals play an important role in the chemical reaction. $H + O_2 \rightleftharpoons O + OH$ and $H + CH_4 \rightleftharpoons CH_3 + H_2$, which are the most dominant chain branching reactions of methane explosion²⁸, contribute to the product amounts of free radicals O and OH²⁹. When the mixed gas absorbs enough energy, the molecular chain breaks. Then, the number of free radicals H, O and OH begin to soar to form a chemical reaction active center with a high concentration of free radicals, which eventually leads to the explosion. As shown in Fig. 3, when the volume fraction of methane is 7% with no CO₂ addition, the maximum mole fraction of the free radicals H, O, and OH are 0.013, 0.016, and 0.021, respectively. Because the addition of CO₂ increases the probability of free radicals collision with the third body to form low-activity stable molecules, as the increase of the CO₂ volume fraction, the location of peak concentration of free radicals prolongs and the peak concentrations of the free radicals H, O, and OH decrease.

Figure 4 shows the effect of CO₂ addition on the peak concentration of radical H, O, and OH over $\varphi = 0.72, 1, 1.18$. It can be found that the CO₂ addition reduces the peak concentration of all the investigated radicals. The greater the methane volume fraction, the greater the decrease rate of radicals H and OH, and the smaller the decrease rate of radical O. When the volume fraction of CO₂ is constant, the increase of the volume fraction

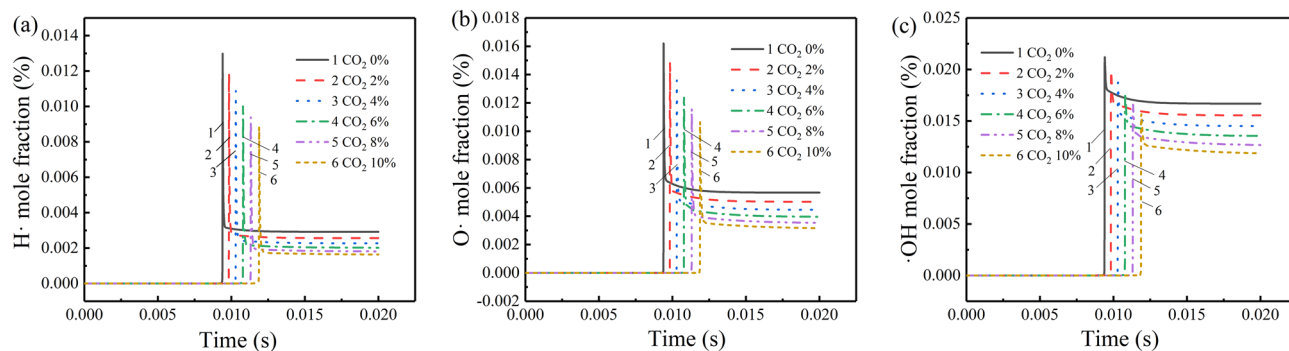


Figure 3. Variation of free radicals concentration with time under different CO₂ concentrations at 7% CH₄: (a) free radical H, (b) free radical O, and (c) free radical OH.

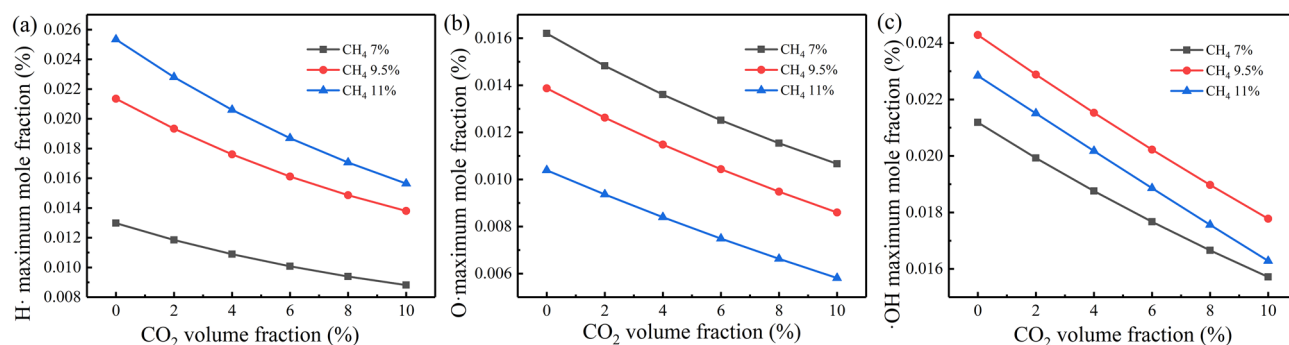


Figure 4. Variation of maximum mole fraction of free radicals with CO₂ volume fraction under different methane volume fractions: (a) free radical H, (b) free radical O, and (c) free radical OH.

of methane leads to the increase of the maximum mole fraction of radical H \cdot and the decrease of the maximum mole fraction of radical O. For radical OH, its maximum mole fraction first increases and then decreases with the location of peak value of 9.5%. The larger the equivalence ratio of CH₄, the less O₂ in the mixture, which increases the number of CH₄ molecules and decreases the number of O₂ molecules in the unit volume of the reactant. The concentration of radical H increases, and the concentration of radical O decreases. At the same time, with the increase of CH₄ concentration, the elementary reaction step R52: H + CH₃(+M) \rightleftharpoons CH₄(+M), R11: O + CH₄ \rightleftharpoons OH + CH₃ tend to promote the consumption of CH₄. It also explains the appearance of Fig. 2.

Gas products. The catastrophic gases, such as CO, CO₂, NO, NO₂, produced in the gas explosions process are the major cause of casualties³⁰. After adding CO₂, the change of the mole fraction of catastrophic gas with 7% CH₄-air is shown in Fig. 5.

As seen, with the increase of the CO₂ volume fraction, the mole fraction of CO is increased, whereas the mole fractions of CO₂, NO, and NO₂ are decreased. This is caused by elementary reaction R31: O₂ + CO \rightleftharpoons O + CO₂, R99: OH + CO \rightleftharpoons H + CO₂, R120: HO₂ + CO \rightleftharpoons OH + CO₂, R132: CH + CO₂ \rightleftharpoons HCO + CO, R153: CH₂(S) + CO₂ \rightleftharpoons CO + CH₂O. When CO₂ is added to the gas mixture, the initial concentration of CO₂ in the gas mixture increases, which causes the above reaction is easier to happen toward to the direction of CO₂ consumption, which results in a large amount of CO. Figure 5a reveals that the mole fraction of CO reaches its peak first, then it reacts with the excess oxygen to form CO₂, and eventually tends to a stable value. Under working condition 1, after gas explosion, the mole fractions of CO, CO₂, NO, and NO₂ are 0.0159, 0.0527, 0.0150, and 7.94 $\times 10^{-6}$, respectively. Under working condition 6, after gas explosion, the mole fractions of CO, CO₂, NO, and NO₂ are 0.0281, 0.0382, 0.0094, and 4.84 $\times 10^{-6}$. the increase rate of CO is 76%, and the decrease rates of CO₂, NO, and NO₂ are 27%, 37%, and 39%.

Table 3 lists the effect of CO₂ addition on the concentration of the catastrophic gas under different methane volume fractions. It shows that, $\phi = 0.72, 1, 1.18$, with the increase of the CO₂ volume fraction, the mole fraction of CO is increased, and the mole fractions of CO₂, NO, and NO₂ are decreased accordingly in all the investigated conditions. When the volume fraction of CO₂ is 10%, with the increase in methane volume fraction, the volume fraction of CO rises while those of CO₂, NO and NO₂ fall. The above results indicate that the addition of CO₂ plays a positive role in inhibiting the formation of NO and NO₂ but promoting the formation of CO.

Key reactions. The key elementary reaction steps during the methane explosion under different conditions are shown in Fig. 6. According to Fig. 6a, when 7% CH₄-Air explodes, the key reaction steps inhibiting CH₄ consumption are R53 and R158. Both reactions consume the free radicals H, O, and OH, which interrupt the chain

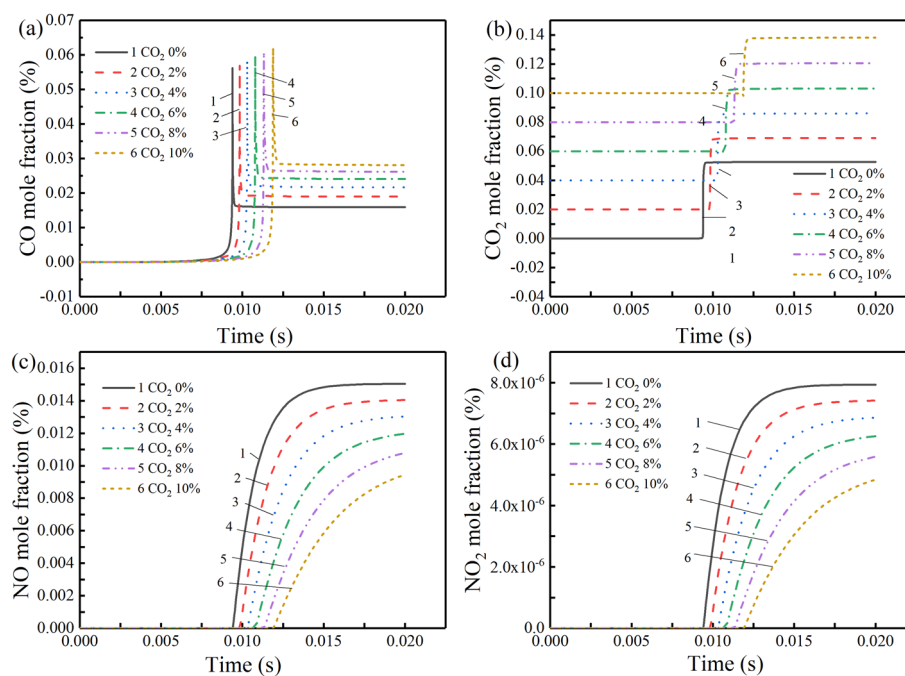


Figure 5. Variation of product concentration of some gases with time under different CO_2 volume fractions at 7% CH_4 : (a) CO, (b) CO_2 , (c) NO, and (d) NO_2 .

Working condition	CO	CO_2	NO	NO_2
7% CH_4	0.01590066	0.05270834	0.01503820	0.00000793779
7% CH_4 + 10% CO_2	0.02811000	0.03818010	0.00944985	0.00000484152
9.50% CH_4	0.04258436	0.04812039	0.01105626	0.00000329051
9.5% CH_4 + 10% CO_2	0.06740572	0.01813410	0.00693919	0.00000190858
11% CH_4	0.06146430	0.04155837	0.00759739	0.00000149968
11% CH_4 + 10% CO_2	0.09511225	0.00064950	0.00415820	0.00000070496

Table 3. Mole fractions of gas products under different working conditions.

reaction. The key reaction steps promoting CH_4 consumption are R118, R155, R157, R156, R38, R52, R119, and R85. These reactions promote the formation of free radicals, and enhance the chain reaction.

According to Fig. 6b, after the addition of 10% CO_2 , the key elementary reaction steps inhibiting CH_4 consumption change from R53 and R158 to R158, R53, and R98. The key reaction step promoting CH_4 consumption change from R118, R155, R157, R156, R38, R52, R119, and R85 to R155, R156, R38, R32, R119, R161, and R170. The sensitivity coefficients of each elementary reaction step are decreased, and the time of the maximum sensitivity coefficient of each elementary reaction step prolongs; at the same time, the reduction amplitude of the coefficient to promote methane consumption is greater than to promote methane formation. This indicates that the change in methane concentration is affected by these reaction steps, the influence becomes weaker, and the addition of CO_2 inhibits the combustion of methane.

Figure 6c, d show that, when 9.5% CH_4 -Air explodes, the key elementary reaction steps inhibiting CH_4 consumption are R158, R53, and R57, and the key elementary reaction steps promoting CH_4 consumption are R155, R156, R38, R32, R119, R161, and R170. When 10% CO_2 was added, the key elementary reaction steps promoting and inhibiting CH_4 consumption do not change. The effects of CO_2 addition on the sensitivity coefficients of CH_4 mole fraction under the methane volume fraction of 9.5% are given in Fig. 7. It can be seen that the sensitivity coefficients of these elementary reactions drop gradually with the increase of CO_2 concentration. Meanwhile, the time when the sensitivity coefficient of each elementary reaction step reaches the maximum value moves back. This means that for the methane explosion with a methane equivalence ratio of 1, the addition of CO_2 has little effect on the change in the methane concentration during the explosion, but inhibits the methane explosion.

As Fig. 6e, f show, when 11% CH_4 -Air explodes, the key elementary reaction steps inhibiting CH_4 consumption are R158 and R53, and the key elementary reaction steps promoting CH_4 combustion are R118, R155, R156, R38, R32, R119, R161, and R170. When 10% CO_2 was added, the key elementary reaction steps inhibiting CH_4 consumption are R158, R53, and R57, and the key elementary reaction steps promoting CH_4 combustion are R155, R156, R38, R32, R119, R161, and R170. The key elementary reaction steps promoting and inhibiting CH_4

The addition of CO₂ changed the key elementary reaction steps affecting CH₄ concentration, and the time of the maximum sensitivity coefficient of each reaction step prolonged. When CH₄ was in a fuel-lean, stoichiometric and fuel-rich conditions, the sensitivity coefficient of each key elementary reaction step was reduced, and the reduction amplitude of the coefficient promoting methane consumption was larger than inhibiting the consumption, indicated that the addition of CO₂ could inhibit CH₄ explosion.

In general, the methane explosion can be inhibited by adding CO₂, and the greater the volume fraction of CO₂, the better the inhibition effect. However, more CO will be produced under a higher methane concentration. In the application of CO₂ addition to gas explosion suppression, it is necessary to consider the possibility of CO poisoning under practical working conditions.

Received: 13 July 2021; Accepted: 28 September 2021

Published online: 20 October 2021

References

- Jia, B. S., Li, Y. H., Zeng, W., Liang, Y. T. & Wen, H. Y. Kinetic simulation for the effect of N₂ content on gas explosion in an constant volume system. *Chin. J. Process. Eng.* **11**, 812–817 (2011).
- Jia, B. S., Wen, H. Y. & Li, Z. X. Study on mechanism characteristic of N₂ & H₂O on inhibiting gas explosion in coal mine tunnel. *J. Nat. Disasters* **22**, 269–276. <https://doi.org/10.13577/j.jnd.2013.0535> (2013).
- Su, B., Luo, Z. M., Wang, T. & Liu, L. Experimental and numerical evaluations on characteristics of vented methane explosion. *J. Central South Univ.* **27**, 2382–2393. <https://doi.org/10.1007/s11771-020-4456-1> (2020).
- Lu, C., Wang, H. B., Pan, R. K., Zhang, Y. P. & Yu, M. G. Preventing the propagation of gas explosion in ducts using spurting nitrogen. *Process Saf. Environ. Prot.* **123**, 11–23. <https://doi.org/10.1016/j.psep.2018.12.028> (2019).
- Lu, C., Wang, H. B., Zhang, Y. P., Zhu, H. & Yu, M. G. Experimental on the prevention of gas explosion by nitrogen curtain. *Chem. Ind. Eng. Progress* **38**, 3056–3064. <https://doi.org/10.16085/j.issn.1000-6613.2018-2009> (2019).
- Cao, X. Y., Ren, J. J., Bi, M. S., Zhou, Y. H. & Li, Y. M. Experimental research on the characteristics of methane/air explosion affected by ultrafine water mist. *J. Hazard. Mater.* **324**, 489–497. <https://doi.org/10.1016/j.jhazmat.2016.11.017> (2016).
- Cao, X. Y., Ren, J. J., Bi, M. S., Zhou, Y. H. & Wang, Q. J. Experimental research on methane/air explosion inhibition using ultrafine water mist containing additive. *J. Loss Prev. Process Ind.* **43**, 352–360. <https://doi.org/10.1016/j.jlp.2016.06.012> (2016).
- Cao, X. Y. *et al.* Suppression of methane/air explosion by ultrafine water mist containing sodium chloride additive. *J. Hazard. Mater.* **285**, 311–318. <https://doi.org/10.1016/j.jhazmat.2014.11.016> (2015).
- Wang, F. H., Chen, W., Wen, X. P., Zhao, W. L. & Liu, Z. C. Numerical simulation and mechanism analysis of gas explosion suppression by ultrasonic water mist. *Energy Sources Part A: Recovery Util Environ Effects* **41**, 2821–2833. <https://doi.org/10.1080/15567036.2019.1576077> (2019).
- Liang, Y. T., Zeng, W. & Hu, E. J. Experimental study of the effect of nitrogen addition on gas explosion. *J. Loss Prev. Process Ind.* **26**, 1–9. <https://doi.org/10.1016/j.jlp.2012.08.002> (2013).
- Qian, H. L., Wang, Z. R. & Jiang, J. C. Influence of N₂/CO₂ mixture on methane explosion. *Explosion Shock Waves* **32**, 445–448. <https://doi.org/10.3969/j.issn.1001-1455.2012.04.016> (2012).
- Li, M. H., Xu, J. C., Wang, C. J. & Wang, R. Thermal and kinetics mechanism of explosion mitigation of methane-air mixture by N₂/CO₂ in a closed compartment. *Fuel* **255**, 115747.115741–115747.115749. doi:<https://doi.org/10.1016/j.fuel.2019.115747> (2019).
- Wang, Z. R., Ni, L., Liu, X., Jiang, J. C. & Wang, R. Effects of N₂/CO₂ on explosion characteristics of methane and air mixture. *J. Loss Prev. Process Ind.* **31**, 10–15. <https://doi.org/10.1016/j.jlp.2014.06.004> (2014).
- Zhang, Y. X., Wu, Q., Liu, C. H., Jiang, B. Y. & Zhang, B. Y. Experimental study on coal mine gas explosion suppression with inert gas N₂/CO₂. *Explosion Shock Waves* **37**, 906–912. [https://doi.org/10.11883/1001-1455\(2017\)05-0906-07](https://doi.org/10.11883/1001-1455(2017)05-0906-07) (2017).
- Luo, Z. M., Kang, K. & Ren, J. Y. Microscopic mechanism of NH₃ on chain of methane explosion. *J. China Coal Soc.* **41**, 876–883. <https://doi.org/10.13225/j.cnki.jccs.2015.0922> (2016).
- Luo, Z. M. *et al.* Study on influence of NH₃ on CH₄ explosion characteristics and reaction kinetics. *China Safety Sci. J.* **30**, 51–58. <https://doi.org/10.16265/j.cnki.issn1003-3033.2020.09.008> (2020).
- Liang, Y. T. & Wen, Z. Simulation of the inhibition mechanism of humidity ratio of air in gas explosion process. *J. Shenzhen Univ. (Science and Engineering)* **30**, 48–53. <https://doi.org/10.3724/SP.J.1249.2013.01048> (2013).
- Wang, L. C., Luo, H. Z. & Liang, Y. T. Effects of water on reaction kinetic for gas explosion in shock tube. *J. China Coal Soc.* **39**, 2037–2041. <https://doi.org/10.13225/j.cnki.jccs.2013.1383> (2014).
- Lu, S. X., He, J., Yu, C. H. & Qin, Y. H. Study on the mechanism of water inhibiting gas explosion. *J. China Coal Soc.* **23**, 83–87. <https://doi.org/10.13225/j.cnki.jccs.1998.04.017> (1998).
- Ren, F., Xiang, L. K., Chu, H. Q., Jiang, H. T. & Ya, Y. C. A modelling study of the impact of blending N₂, CO₂ and H₂O on characteristics of CH₄ laminar premixed combustion. *Energy Fuels* **34**, 1184–1192. <https://doi.org/10.1021/acs.energyfuels.9b02108> (2019).
- Jia, B. S., Wen, H. Y., Liang, Y. T. & Wang, X. Y. Mechanism characteristics of CO₂ and N₂ inhibiting methane explosions in coal mine roadways. *J. China Coal Soc.* **38**, 361–366. <https://doi.org/10.13225/j.cnki.jccs.2013.03.019> (2013).
- Li, C. B. Chemical kinetics mechanism analysis of N₂/CO₂/H₂O suppressing methane explosion. *China Safety Sci J* **20**, 88–92. <https://doi.org/10.16265/j.cnki.issn1003-3033.2010.08.011> (2010).
- Li, C. B., Wu, G. D., Zhou, N. & Luo, Y. Numerical analysis of methane combustion suppression by N₂/CO₂/H₂O. *J. Univ. Sci. Technol. China* **40**, 288–293. <https://doi.org/10.3969/j.issn.0253-2778.2010.03.014> (2010).
- Carrasco, N. *et al.* Sensitivity of a Titan Ionospheric model to the ion-molecule reaction parameters. *Planet. Space Sci.* **56**, 1644–1657. <https://doi.org/10.1016/j.pss.2008.04.007> (2008).
- Gregory, P. & Smith, D. G. *GRI-Mech 3.0*. Preprint at <http://combustion.berkeley.edu/gri-mech/version30/text30.html> (2007).
- Gao, N., Zhang, Y. S., Hu, Y. T. & Peng, J. H. Dynamics analysis of gas explosion chain reaction in restricted space. *China Safety Sci. J.* **24**, 60–65. <https://doi.org/10.16265/j.cnki.issn1003-3033.2014.01.013> (2014).
- Liang, Y. T. & Zeng, W. Numerical study of the effect of water addition on gas explosion. *J. Hazard. Mater.* **174**, 386–392. <https://doi.org/10.1016/j.jhazmat.2009.09.064> (2010).
- Wang, T. *et al.* Flammability limit behavior of methane with the addition of gaseous fuel at various relative humidities. *Process Saf. Environ. Prot.* **140**, doi:<https://doi.org/10.1016/j.psep.2020.05.005> (2020).
- Wang, T. *et al.* The explosion enhancement of methane-air mixtures by ethylene in a confined chamber. *Energy* **214**, doi:<https://doi.org/10.1016/j.energy.2020.119042> (2021).
- Li, X. C., Nie, B. S., Yang, C. L. & Chen, J. W. Effect of gas concentration on disastrous gases produced by gas explosion in confined space. *China Safety Sci. J.* **26**, 69–75. <https://doi.org/10.16265/j.cnki.issn1003-3033.2016.01.012> (2016).

Acknowledgements

This work was supported by National Natural Science Foundation of China (Grant No. 51774181); National Natural Science Foundation of China (Grant Nos. 52174229, 52174230); Liaoning Provincial Natural Science Foundation of China (Grant No. 2020-BS-285);

Author contributions

Jingyan Wang: Investigation, Methodology, Data curation, Writing—original draft, Visualization. Yuntao Liang: Conceptualization, Resources, Funding acquisition, Supervision, Writing—review & editing. Fuchao Tian: Investigation, Writing—review & editing. Chengfeng Chen: Investigation, Writing—review & editing.

Competing interests

The authors declare no competing interests.

Additional information

Correspondence and requests for materials should be addressed to Y.L.

Reprints and permissions information is available at www.nature.com/reprints.

Publisher's note Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional affiliations.



Open Access This article is licensed under a Creative Commons Attribution 4.0 International License, which permits use, sharing, adaptation, distribution and reproduction in any medium or format, as long as you give appropriate credit to the original author(s) and the source, provide a link to the Creative Commons licence, and indicate if changes were made. The images or other third party material in this article are included in the article's Creative Commons licence, unless indicated otherwise in a credit line to the material. If material is not included in the article's Creative Commons licence and your intended use is not permitted by statutory regulation or exceeds the permitted use, you will need to obtain permission directly from the copyright holder. To view a copy of this licence, visit <http://creativecommons.org/licenses/by/4.0/>.

© The Author(s) 2021