# ARTICLE OPEN (Check for updates MoCoB metallic glass microwire catalysts for highly efficient and pH-universal degradation of wastewater

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One important goal of the current Fenton-like catalysts is to develop highly efficient and pH-universal catalysts that can operate with little performance degradation over multiple recycles. Herein, we report a ternary MoCoB metallic glass (MG) microwire catalyst, which shows exceptional Fenton-like activity for degrading various dyes in a wide pH range (5–10). Moreover, the MoCoB MG catalyst with an ultrahigh glass-transition temperature of 1002 K exhibits excellent reusability and can be used for more than 46 times without a decay in efficiency. It is regarded that the excellent catalytic activity and sustainability of the MoCoB MG catalyst originates from the bimetallic effect involving Mo<sup>n</sup>/Mo<sup>n+1</sup> and Co<sup>n+1/</sup>Co<sup>n</sup></sup> cycling, which accelerates the electronic transfer kinetics, enabling the generation of multiple reactive oxygen species (•OH and •O<sub>2</sub><sup>-</sup>). First-Principles Calculations revealed again that MG catalysts provide a large electron base for the whole catalytic process.</sup>

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## INTRODUCTION

Metallic glasses (MGs) exhibit excellent physical and chemical properties due to their atomic disordering arrangement and metastability<sup>1</sup>. MGs with simultaneously high catalytic activity and unique selectivity have emerged as a kind of competitive candidate catalyst for hydrogen evolution reaction (HER)<sup>2,3</sup>, and oxygen evolution reaction (OER)<sup>4</sup>, etc. Especially, their excellent catalytic performance in wastewater treatment has attracted increasing attention in recent years<sup>5–7</sup>. For example, the degradation efficiency of Fe<sub>78</sub>Si<sub>7</sub>B<sub>17</sub>Nb<sub>3</sub> MG powders for Direct Blue 6 is 200 times higher than that of commercial iron powder<sup>8</sup>. The degradation efficiency of Fe<sub>78</sub>Si<sub>9</sub>B<sub>13</sub> and Fe<sub>73.5</sub>Si<sub>13.5</sub>B<sub>9</sub>Cu<sub>1</sub>Nb<sub>3</sub> MG ribbons is 5–10 times higher than that of their crystalline counterparts<sup>9</sup>. Beside Fe-based MG system, other MG systems (including Mg-based, Co-based) with high degradation efficiency have also been developed.

Although MGs have shown high catalytic activity in degrading dying wastewater, they still face several challenges and drawbacks. Firstly, most of the MG catalysts reported so far are mainly in the forms of ribbons, the small specific surface area of which usually limits their reactivity<sup>10–12</sup>. Secondly, a trade-off between the catalytic activity and long-term stability remains, that is, the active MG catalysts are not chemically stable while those stable MGs have low catalytic activity. This dilemma typically results in a limited reusability (normally <35 times<sup>13</sup>). For instance, the catalytic process of the FeSiB MG is always accompanied with surface aging and corrosion, resulting in progressively decreased catalytic efficiency and reaction rate constant ( $k_{obs}$ ) decreases progressively with the number of cycles<sup>14,15</sup>. Furthermore, most MGs can only degrade dyes in a narrow pH ranges (2-3.5), and a small change in pH value will cause drastic decay in the degradation rate<sup>16-18</sup>. Although some MG catalyst has been reported to be operate in a wide pH range, the degradation efficiency is actually extremely slow, e.g., the complete degradation of a Direct Blue 2B requires more than 100 h<sup>19</sup>. Since the industry applications usually involve with neutral or alkaline condition, it is necessary to develop highly reusable, efficient, and pH-universal MG catalysts.

In this work, we demonstrate that a ternary MoCoB MG microwire can be a highly active and stable catalysts for Fenton-like reactions. We found the  $Mo_{51}Co_{34}B_{15}$  MG can exhibit high degradation efficiency towards various dying wastewater within a wide pH range (5–10), and shows negligible degradation after operation for 45 times. We attribute the notable catalytic performance of this  $Mo_{51}Co_{34}B_{15}$  MG to Crystal Violet (CV) dye, as well as the large specific surface area of microwires.

#### **RESULTS AND DISCUSSION**

#### Synthesis of MoCoB MG microwire and their characterization

Figure 1a shows a schematic diagram of designing and preparing MG microwire using melt-spinning techniques, raising the microsized tube to bring the metal liquid contacted with the edge of the sharp copper rod. The as-fabricated MG wires can be seen in Fig. 1b, and the surface of the prepared  $Mo_{51}Co_{34}B_{15}$  MG microwire is very smooth, as shown in Fig. 1c. The XRD pattern in Fig. 1d exhibits a broad diffuse scattering peak of 43°, without obvious crystalline peaks, indicating the fully amorphous structure within the resolution limit of XRD. The DTA curve shown in Fig. 1e shows that the Mo<sub>51</sub>Co<sub>34</sub>B<sub>15</sub> MG wires have an obvious glass transition and multi-step crystallization reaction, which further confirms its amorphous nature<sup>20,21</sup>. It should be noted that the present Mo<sub>51</sub>Co<sub>34</sub>B<sub>15</sub> MG catalyst exhibits an ultra-high glass transition temperature  $T_q$  (1002 K) and crystallization temperature  $T_{\rm x}$  (1070 K), which is far higher than those of FeSiB MG catalysts  $(T_q = 693 \text{ K})^{22}$ . The excellent thermal stability could endow the MG with long-term stability and reusability under harsh (e.g., hightemperature) wastewater treatment conditions. The specific surface area (SSA) of the MG microwires catalyst is 5.9  $m^2/q$  (Fig. 1f), which is 1-2 orders of magnitude higher than that of most reported MG ribbons<sup>23</sup>. The high SSA is beneficial for exposing more abundant active sites for catalytic reactions.

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Fig. 1 Catalysts structure. a Schematic illustration of the preparing processes of MoCoB MG microwires. b Photographs of prepared microwire. c SEM image, d XRD pattern, e DTA curve, f Isothermal adsorption and desorption curves of the prepared MoCoB MG wires, respectively.

## **Catalytic performance**

The catalytic performance of the  $Mo_{51}Co_{34}B_{15}$  MG wire catalysts was assessed via degradation of CV solutions (a typical triarylmethane dye in industry). It is found that the current MoCoB MG wires show superior catalytic activity than the typical FeSiB MG ribbons (Fig. 2a), the MoCoB catalysts achieved 99% degradation of the CV solution within 20 min, whereas the latter was only 50%. The degradation reaction follows the pseudo-firstorder kinetic model,  $k_{obs}$  can be obtained from Eq. (1)

$$\ln(C_0/C_t) = k_{\rm obs}t \tag{1}$$

where  $C_0$  is the initial concentration of dye,  $C_t$  is the concentration at t, and t is the reaction time. The calculated  $k_{obs}$  value of  $Mo_{51}Co_{34}B_{15}$  is about 7 times higher than that of  $Fe_{78}Si_9B_{13}$ , again indicating the excellent degradation performance of the current catalyst. To verify the versatility of the microwire catalysis, three typical dyes of Crystal Violet, Malachite Green and Direct Blue 6 were selected for degradation experiments. As shown in Fig. 2b, Crystal Violet and

Direct Blue 6 could be completely removed by the MoCoB wire catalyst within 15 min, and Malachite Green become completely colorless within 10 min. Interestingly, we find that, in our sample of MoCoB MG wire exhibits excellent adaptability to pH changes. It achieves complete degradation of most acidic and alkaline solutions, with a rapid and effective degradation at pH 5-10 (Fig. 2c). This greatly breaks the pH limitation of metallic glasses for dyes degradation and can effectively address the critical issue of degradation under alkaline conditions<sup>24,25</sup>. Interestingly, unlike other metallic glasses, the degradation rate of current MG microwire catalysts accelerates with increasing pH value of the solution. The breaking of the trade-off between pH and catalytic activity indicates that a catalytic mechanism for this MoCoB MG catalyst, which will be discussed later. To further highlight the excellent catalytic performance of this catalyst, the comparable results of applicable pH value versus  $k_{obs}$  for various MG catalysts in wastewater treatment are summarized<sup>9,15–17,26–31</sup> (Fig. 2d), more details can be found at Supplementary Table 1.



**Fig. 2** Catalytic performance. a Comparison of degradation efficiency of the current MoCoB MG microwires with Fe78Si9B13 MG ribbons in CV dye. b Removal rate of three dyes. c Removal rate of CV by using the MoCoB as the catalyst under different pH value. d Summary plots comparing with previous literature results in terms of catalytic activity and suitable pH<sup>9,15-17,26-31</sup>.

The adaptability of the catalyst under different conditions is of great importance. To scientifically and comprehensively evaluate the effects of temperature, pH, H<sub>2</sub>O<sub>2</sub> dosage and original concentration of the solution, an orthogonal matrix L16 (4<sup>4</sup>) was designed to cover the possible degradation effects obtained under all combinations of factors, with  $k_{obs}$  as the final indicator. It is clearly found that  $k_{obs}$  with the maximum value is shown in number 13 (Supplementary Table 2), which is the best condition for MG catalysis (i.e., the best value for multi-factor variation), and a series of subsequent degradation experimental parameters are used as a reference. Notably, we also found that pH was the main factor affecting the degradation efficiency (Supplementary Table 3). Catalytic performance for other individual environmental factors also can be seen in Supplementary Fig. 1a-d. The results show that the degradation rate accelerates continuously as the temperature increases from 293 to 333 K. Moreover, the activation energy ( $\Delta E$ ) can be evaluated by the Arrhenius-type Eq. (2):

$$\ln k_{\rm obs} = -\Delta E/RT + \ln A \tag{2}$$

where *R* is the gas constant, *T* is the temperature, and lnA is the proportionality constant. The  $\Delta E$  of present microwire catalysts of 44.6 KJ/mol is much lower than that of the crystalline catalysts (60–250 KJ/mol), indicating the metallic glasses are more likely to cross the reaction energy barrier for catalytic degradation reactions<sup>25,32</sup>. It is noticed that the degradation rate increases with increasing H<sub>2</sub>O<sub>2</sub> dosage (Supplementary Fig. 1d). Unlike the conventional Fenton-like system, the current MoCoB/H<sub>2</sub>O<sub>2</sub> system breaks the limitation that H<sub>2</sub>O<sub>2</sub> annihilates hydroxyl radicals instead when added in excess<sup>33–35</sup>. As shown in Supplementary Fig. 1c, the microwire catalyst still exhibits excellent degradation ability over a wide range of concentrations. Apparently, the  $k_{obs}$  of the CV solution can be effectively improved by increasing the amount of catalyst, H<sub>2</sub>O<sub>2</sub> and reaction temperature. In addition, the leached Mo/Co ion only contributed less than 10% of dye

degradation during the catalytic activity, indicating that the dye degradation was primarily derived from the contribution of the heterogeneous catalyst (Supplementary Fig. 2).

#### Reusability

The sustainability and stability of catalysts is one of the core issues to be considered in practical wastewater remediation. However, most of the reported metallic glasses often suffer from surface aging or product coverage during the catalytic degradation, especially after multiple cycles<sup>9,18</sup>. In this work, the cycling performance and long-term reactivity of the catalysts in CV solution was systematically investigated. Figure 3 shows the degradation performance of different cycles and compared with other materials, it was found that the degradation efficiency still reaches more than 80% after 46 cycles and the degradation rate always maintains at a stable level, as shown in Fig. 3a. Figure 3b summarizes the comparison graph of  $k_{obs}$  versus reusability of reported metallic glasses for wastewater remediation, with more details presented in Supplementary Table 19,17,28,29,31,36-39. It can be seen that such a durable catalyst with high catalytic activity show great potential for practical wastewater treatment applications.

## **Reaction mechanism**

The current MoCoB catalysts exhibit excellent catalytic performance in terms of catalytic activity, pH adaptation and reusability. To decode the catalytic mechanism of MoCoB MG microwires, we used different methods to analyze the degradation mechanism, Fig. 4 shows the corresponding experimental results of different methods. EPR analysis were conducted using DMPO and TEMP as the spin-trapping agents (see Fig. 4a). Surprisingly, in addition to •OH (1:2:2:1), superoxide radicals  $\cdot O_2^-$  (1:1:1:1) was also produced during the catalytic process. It should be particularly emphasized that we also found singlet oxygen  ${}^{1}O_2$  (1:1:1), which has never

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Fig. 3 The degradation performance of different cycles and compared with other materials. a Reusability of the MoCoB catalysts toward the degradation of CV and b comparison of the catalytic performance with previously reported catalysts in terms of kobs versus reusability.



**Fig. 4** The corresponding experimental results of different methods. a EPR spectra using DMPO and TEMP as trapping agents at room temperature and natural pH and **b** quenching experiments using TBA and PBQ.

been reported previously in amorphous alloy/H2O2 systems for wastewater treatment. To further clarify the role of each reactive intermediate in the degradation process, guenching experiments were performed with tertbutanol (TBA) and p-benzoquinone (pBQ). Strikingly, •OH only assumed a weak effect, while a small amount of pBQ was able to terminate more than 50% of the degradation reaction (see Fig. 4b). In other words,  $\cdot O_2^-$  plays a dominant role in the whole catalytic degradation, and the advanced oxidation mechanism based on the combined action of  $\cdot O_2^-$  and  $^1O_2$  enables the rapid degradation of dyes. According to the Haber-Weiss cycle, <sup>1</sup>O<sub>2</sub> is generated by the further oxidation of the reactive species  $\overline{O_2}^{-40}$ . Moreover, with the increasing of solution pH (from 3.5–10), the content of  $\cdot O_2^-$  and the rate of their deprotonation to produce  ${}^{1}O_{2}$  are also increasing. This fully confirms the nature of the current system that degrades at a faster rate under alkaline conditions than acidic conditions, a similar phenomenon was observed in Fe<sub>2</sub>O<sub>3</sub>@FCNT<sup>41</sup>. This confirms why the current MG catalyst can function in acidic media as well as achieve rapid degradation in most alkaline conditions.

In order to gain insight into the catalytic mechanism of the MG in the degradation process, density functional theory (DFT) was applied in simulations, Fig. 5 shows the decomposition process of  $H_2O_2$  at different sites on the amorphous surface calculated by first principles. The Mo site and Co site were chosen respectively (Fig. 5a, b). It can be concluded that once  $H_2O_2$  is adsorbed by the catalyst, the O-O bond is rapidly elongated to form two hydroxyl radical. Under the strong oxidation of the amorphous matrix, the two •OH quickly turn into  $H_2O$ , which is in excellent agreement with the EPR and quenching results obtained in Fig. 4. To better understand the effect of the atoms on the catalytic process, the

absorption energy of  $H_2O_2$  is calculated with  $E_{ads}$  (Mo) = -0.53 eVand  $E_{ads}$  (Co) = -0.50 eV, which indicates a stronger adsorption capacity of Mo atom. It can be seen from Fig. 5c that the energy is progressively lower during this process, indicating that the transition is completely spontaneous in the presence of the metallic glass catalyst. With respect to the Mo site (Fig. 5d), it was found that significant charge transfer occurs at the catalysis and O-O, respectively. The corresponding electron transfers are 0.4e and 0.6e. These findings indicate that MG catalysts provide a large electronic basis for the catalytic process. Moreover, we also found that the most stable state of O-O is in the triangular structure of Mo/Co atoms, which is once again emphasized the synergistic effect of bimetals.

To fundamentally analyze the role of Mo/Co bimetals in the excellent stability, XPS analysis of the samples were performed at different cycles, and all the results were corrected with the C peak (284.8 eV). Figure 6a shows the Mo3d pattern, wherein the Mo<sup>0</sup> are transformed into Mo<sup>4+</sup> and Mo<sup>6+</sup> in the recycling microwires. Similarly, Co<sup>0</sup> in the original catalysts gradually evolves to Co<sup>2+</sup> and Co<sup>3+</sup> as the reused (Fig. 6b). The transformation of two metallic elements indicating that the Mo<sup>0</sup>/Co<sup>0</sup> is the electron supplier during the catalytic performance. Additionally, the oxidation process from  $Mo^{4+}$  to  $Mo^{6+}$  and  $Co^{2+}$  to  $Co^{3+}$  is the important process for the generation of reactive species. It is well known that from thermodynamics aspect, the higher valence is very difficult to return to the lower valence state again, which greatly limits the production of reactive species. However, in this work, a Co<sup>2+</sup>-rich surface was found to be stable on the cycling catalyst because of the reductive Mo<sup>6+</sup>. To confirm this issue, the ratios of two elements are purposefully summarized in Fig. 6c. As can be seen, the ratio of Mo<sup>4+</sup>/Mo<sup>6+</sup> and Co<sup>3+</sup>/Co<sup>2+</sup> gradually



Fig. 5 The DFT calculations of the decomposition process of  $H_2O_2$  at different sites on the catalysts surface. a Mo site, b Co site, c reaction coordinates of Mo and Co site and d surface structure with electron density difference plots of Mo-doped  $H_2O_2$ .

decreases with the cycles. It is worth noting that the trends in the ratios of the two metal elements are completely opposite. This implies that the stable presence of a Co<sup>2+</sup>-rich surface is necessarily linked to Mo<sup>4+</sup>. In other words, Mo<sup>4+</sup> acts as a reducing agent and electron transfer medium to accelerate the redox cycle from Co<sup>3+</sup> to Co<sup>2+</sup>, as in Eq. 3. Figure 6d also shows the schematic diagram of electron transfer in the catalytic process. The bimetal forms a closed internal cycling system, which becomes the key reason for the current MoCoB MG microwire with 46 cycles. More importantly, the electron enriched MoCoB catalyst allows •OH to further react with H<sub>2</sub>O<sub>2</sub> to produce •O<sub>2</sub><sup>-</sup> and <sup>1</sup>O<sub>2</sub> (Eqs. 4 and 5)<sup>42</sup>. That is also the reason why •OH can be detected in the EPR (Fig. 4a), but does not directly degrade the wastewater.

$$Mo^{4+} + Co^{3+} \rightarrow Mo^{6+} + Co^{2+}$$
 (3)

$$\bullet OH + \bullet OH \to H_2O_2 \tag{4}$$

$$\bullet OH + H_2O_2 \rightarrow H_2O + \bullet HO_2(\bullet HO_2 \leftrightarrow \bullet O_{2^{--}} + H^+)$$
(5)

The long-term reactivity of the catalyst is mainly related to the chemical reaction and stability of the alloy surface. As can be seen in Fig. 7a, the MoCoB shows a stable charge-transfer resistance ( $R_{ct} = 860-881 \Omega.cm^2$ ) after reused compared to the origin catalysts ( $R_{ct} = 1732 \Omega.cm^2$ ). Moreover, the catalysts activated by H<sub>2</sub>O<sub>2</sub> have significantly lower  $R_{ct}$ , indicating the important role of activators in stimulating catalytic activity. The double-layer capacitance (CdI) results and electrochemical surface area (ECSA) values are shown in Fig. 7b and Supplementary Fig. 3. The ECSA result for the original catalyst was 13.8 µF/cm<sup>2</sup>. After 5 to 46 cycles,

the ECSA was maintained at 14.5–20.2  $\mu$ F/cm<sup>2</sup>. Figure 7c analyzes the variation of  $R_{ct}$  and ECSA with the number of cycles. Such results reveal from an electrochemical point of view why the current MG has high reusability. Figure 7d indicates the evolution of the surface morphologies of the catalysts at different cycles, showing some rounded precipitates and nanoparticles after 5 and 10 cycles. In particular, the catalysts display a self-reconfiguration ability to its original smooth state after 46 cycles, which is mainly related to the special structure of the metallic glasses<sup>39</sup>. The EDS results after different cycles show a uniform distribution, except for a very small amount of Mo deprivation after 5 cycles. In particular, it should be noted that O elements did not significantly aggregate after multiple cycles, implying that the reactivity of the catalyst is not limited by the dense oxide layer.

## Conclusion

In summary, the ternary MoCoB MG microwire with high specific surface area were prepared by melt spinning techniques, which showed ultra-high catalytic performance and reusability in wastewater degradation. The results show that the electron enriched Mo-based catalysts also exhibit surprisingly high stability over a wide pH range (5–10), overcoming the limitation in alkaline conditions. Due to the special amorphous structure and alloy system, Mo can accelerate the reduction process of  $Co^{3+}$  to  $Co^{2+}$  on the surface forming a bimetallic internal circulation mechanism. The catalytic mechanism and reactive species are discussed in detail both from experiments and DFT calculations, and the dominant role of  $\cdot O_2^-$  provide a perspective for the subsequent research of the metallic glasses/H<sub>2</sub>O<sub>2</sub> system in wastewater treatment. It also provides insights into practical applications of



Fig. 6 XPS results of MoCoB MG microwire in different states. a Mo 3d. b Co 2p. c The ratio of different elements on the catalysts surface. d Schematic illustration of the electronic transfer.

MG catalysts, making Mo-based MG microwires potential candidate for environmental treatment.

## **METHODS**

#### Material and fabrication process

The  $Mo_{51}Co_{34}B_{15}$  (at. %) MG microwires were manufactured by melt-spinning techniques with a wire speed of ~40 m/s for copper wheels. Before that, high-purity molybdenum (99.9 wt. %), cobalt (99.9 wt. %), and boron (99.5 wt. %) were made into a master alloy ingot by arc melting, which was melted at least 5 times to ensure chemical homogeneity.

Crystal Violet ( $C_{25}H_{30}CIN_3$ ), Malachite Green ( $C_{23}H_{25}CIN_2$ ) and Direct Blue 6 ( $C_{32}H_{20}N_6Na_4O_{14}S_4$ ) dyes were purchased from Chongqing Titanium New Chemical Co. The pH values of the organic solutions were adjusted with 1 M HCl and 1 M NaOH. All the reagents were analytically pure except 30%  $H_2O_2$  without further purified.

## Structure characterization method

The structure of the amorphous catalysts was characterized by X-ray diffraction (XRD, SHIMADZU XRD-6100) using Cu-K $\alpha$  radiation. The thermal stability was studied by differential thermal analysis (DTA, STA409PC) under Ar<sub>2</sub> atmosphere at a heating rate of 20 K/min. The specific surface area of the prepared catalysts was tested by BET (JW-BK400) under N<sub>2</sub> atmosphere.

## Catalytic experiment method

During the catalytic experiments, the temperature of the solution was controlled with a water bath and magnetic stirring was

maintained. During the reaction, 3 mL of the solution was drawn with a syringe at predetermined time intervals (e.g., 2, 5, 10, 12, 15 min, etc.) and the absorbance of the corresponding solution was measured with a UV-visible photometer (Spectrophotometer U-3310). The reusability of the samples was assessed by cycling experiments, which was performed in 20 ppm of CV solution. After one cycle, the catalysts were removed and washed three times with deionized water, then blown dry and continued in a fresh CV solution to start the next cycle, repeating this process until a significant change in catalytic efficiency was observed. Molybdenum chloride (MoCl<sub>5</sub>) and cobalt chloride hexahydrate (CoCl<sub>2</sub>.6H<sub>2</sub>O) were employed as homogeneous catalysts to assess the effect of leached metal ions on the degradation of the dye during the catalytic process. The concentration of metal ions was measured by inductively coupled plasma atomic emission spectrometry (ICP- OES, OPTIMA 8000DV).

The effect of external factors including temperature, pH value, H<sub>2</sub>O<sub>2</sub> dosage and concentration of the solution on the catalytic performance was evaluated using an orthogonal experimental system. If not specifically mentioned, the following conditions were chosen: dye concentration of 20 ppm, catalyst dosage of 2 g/L, H<sub>2</sub>O<sub>2</sub> addition of 0.1 M, and temperature of 323 K. The electrochemical impedance and cyclic voltammetry curve of the samples were tested in CV solution using a standard three-electrode system consisting of a Pt electrode, a saturated calomel electrode, and the catalysts. The surface morphologies and elemental distribution of the catalysts before and after the reaction were observed by scanning electron microscopy (SEM, JSM-6610) with energy spectrum analysis (EDS). Then, the reaction mechanism was comprehensively and deeply analyzed by X-ray photoelectron spectroscopy (XPS, AXIS SUPRA+) and electron paramagnetic resonance (EPR, EMXplus-9.5/12).

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Fig. 7 Electrochemical curves of the original sample and the sample after degradation with different number of cycles. a EIS curve. b Cdl calculated from cyclic voltammetric curves. All electrochemical tests were performed in 20 ppm CV solution. c Variation of Rct and Cdl under different cycles. d Surface morphologies and elemental mapping results of MG microwire after different cycles.

## First-principles calculation process

The First-Principles Calculations were performed by the CASTEP module. The projector augmented wave (PAW) pseudopotential was adopted for the comprehensive density functional theory (DFT) calculations, and the generalized gradient approximation (GGA) using Perdew-Burke-Ernzerhof (PBE) was applied for the description of the electron exchange correlation<sup>43,44</sup>. The structure of MoCoB MG was built by Ab initio molecular dynamics (AIMD) simulations via a traditional melted and guenched process. The kpoints of Monkhorst–Pack was set to be  $2 \times 3 \times 1$  and the energy cutoff was set to be 300 eV, and a DFT-D approach with the Ortmann-Bechstedt-Schmidt (OBS) vdW correction was selected to take into account vdW interactions<sup>45,46</sup>. The energy and maximum force convergence criteria during geometry optimizations were set at 10<sup>-5</sup> eV /atom and 0.03 eV/Å, respectively, and a vacuum zone measuring 25 Å was applied to prevent the interaction between periodical layers.

#### DATA AVAILABILITY

The authors declare that the data supporting the findings of this study are included within the paper and available from the corresponding author on reasonable request.

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## AUTHOR CONTRIBUTIONS

M.T.: validation, investigation, data curation, methodology, formal analysis, writing original draft preparation, visualization. L.L.: methodology, data curation, visualization, investigation. C.S.: validation, investigation. C.L.: software. C.Z.: investigation, writing—reviewing and editing. S.G.: supervision, conceptualization, methodology, writing—reviewing and editing, funding acquisition.

#### **COMPETING INTERESTS**

The authors declare no competing interests.

## **ADDITIONAL INFORMATION**

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