

Efficient urea electrosynthesis from carbon dioxide and nitrate via alternating Cu–W bimetallic C–N coupling sites

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Electrocatalytic urea synthesis is an emerging alternative technology to the traditional energy-intensive industrial urea synthesis protocol. Novel strategies are urgently needed to promote the electrocatalytic C–N coupling process and inhibit the side reactions. Here, we report a CuWO₄ catalyst with native bimetallic sites that achieves a high urea production rate ($98.5 \pm 3.2 \mu\text{g h}^{-1} \text{mg}^{-1}_{\text{cat}}$) for the co-reduction of CO₂ and NO₃[−] with a high Faradaic efficiency ($70.1 \pm 2.4\%$) at -0.2 V versus the reversible hydrogen electrode. Mechanistic studies demonstrated that the combination of stable intermediates of *NO₂ and *CO increases the probability of C–N coupling and reduces the potential barrier, resulting in high Faradaic efficiency and low overpotential. This study provides a new perspective on achieving efficient urea electrosynthesis by stabilizing the key reaction intermediates, which may guide the design of other electrochemical systems for high-value C–N bond-containing chemicals.

Urea is used in nitrogen-based fertilizers and has supported a large proportion of the crop yield increase and assured the food supply of humanity^{1,2}. In industry, urea is synthesized using the Bosch-Meiser process, where CO₂ and liquid ammonia are mixed in urea through an ammonium carbamate intermediate under severe high-pressure conditions (150–250 bar) and elevated temperature (150–200 °C)³. Moreover, industrial ammonia manufacture (Haber-Bosch method) is highly energy-intensive, consumes considerable amounts of fossil fuels, and heavily emits CO₂; thus, the current urea synthetic protocol is far from meeting the demands of society for sustainable development⁴. By contrast, electrosynthesis can convert feedstocks into high-value-added chemicals using renewable energy, being a more sustainable process and enabling the decarbonization of urea production^{2,5}.

To date, direct activation of N₂ coupled to CO₂ for urea in ambient conditions is still challenging, because of the high overpotential requirements for the dissociation of highly stable C=O (806 kJ mol^{-1})

and N≡N (941 kJ mol^{-1}) bonds, as well as the strong competition of the parallel reactions^{6–8}. Reactive nitrogen-oxygen bond-containing species, such as nitric oxide (NO) and nitrate/nitrite (NO₃[−]/NO₂[−]) ions, are more active nitrogen feedstocks. Among these species, NO₃[−] is a nitrogen-containing reactant with a better intrinsic instability, which can be obtained from industrial wastewater; or by potentially sustainable nitrate generation technology in the future, such as non-thermal plasma activation of nitrogen^{9,10}. Moreover, the lower dissociation energy of the nitrogen-oxygen bond (204 kJ mol^{-1}) eases the coupling of NO₃[−] reduction with CO₂ reduction to accomplish urea electrosynthesis¹¹. Thus, the NO₃[−] to urea process is a suitable model reaction to study the electrochemical C–N bond formation; and a potential synthetic protocol for urea synthesis.

Since 1998, NO₃[−] has been reported as a nitrogen-containing feedstock that can be coupled with CO₂ for urea electrosynthesis¹². However, the complex 16-electron reduction process has restricted

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studies on the development of NO_3^- -to-urea¹³; in particular, the comprehensive mechanistic understanding of electrocatalytic C–N bond formation and the structure design of catalysts remain fundamental challenges^{14,15}. To date, urea electro-synthesis with NO_3^- and CO_2 as feedstocks has reached an FE of up to 53% with a current density of 0.3 mA cm^{-2} ¹⁶. Furthermore, the applied potentials for efficient urea electro-synthesis range from -0.6 to -1.5 V vs. reversible hydrogen electrode (RHE)^{15,16}, which are far away from the thermodynamic potential for urea synthesis from CO_2 and NO_3^- (0.48 V vs. RHE)¹⁷. Under such negative applied potentials, kinetically favorable competing side reactions, such as H_2 generation, CO_2 reduction, and NO_2^- , NH_3 production, easily occur and reduce the selectivity of urea electro-synthesis¹⁸.

As the primary intermediate of NO_3^- reduction, the formation of $^*\text{NO}_2$ does not involve complex elementary reactions that may dissociate various by-products. Thus, $^*\text{NO}_2$ serves as a vital N-intermediate that reacts with intermediates of CO_2 reduction, which may reduce the overpotential of urea electro-synthesis and reduce the probability of by-product generation. Cyanobacteria can utilize NO_3^- to photosynthetically synthesize organic nitrogen compounds with the help of nitrate and nitrite reductase metalloenzymes. In the first step of nitrate assimilation, nitrate reductase, a Mo-bis-molybdopterin guanine dinucleotide with a high-valence Mo^{4+} -based reaction center, can convert NO_3^- into $^*\text{NO}_2$ intermediate and rapidly dissociate to NO_2^- at a low reduction potential^{19,20}. A relatively long lifetime of N-related intermediates is expected to provide more opportunities for coupling with the intermediates of CO_2 reduction, which the C–N bond formation can achieve urea electro-synthesis. The reaction of a high-valence metal center can decrease the electron density of the adsorbed species, resulting in a more positive reaction overpotential^{21,22}. As tungsten is a homolog of molybdenum, high-valence tungsten-oxide derivatives are conducive to stabilizing $^*\text{NO}_2$ intermediate(s); such as WO_3 could strongly adsorb NO_2 molecules on the surface^{23,24}. However, WO_3 itself cannot trigger the CO_2 reduction at low overpotentials, because $^*\text{CO}$ intermediate is challenging to be formed²⁵. Contrarily, $^*\text{CO}$ is the common CO_2 reduction intermediate on Cu-

based catalysts, but continuous Cu sites enable the C–C coupling between adsorbed $^*\text{CO}$ and/or $^*\text{CHO}/^*\text{COH}$ intermediates²⁶. For urea electro-synthesis, a higher C–N coupling proportion is expected; separating the Cu sites could reduce the probability of C–C coupling by-products²⁷.

Based on the considerations above, in this study, a Cu–W bimetallic oxide (CuWO_4) catalyst with alternating bimetallic reaction sites was utilized for urea electro-synthesis with CO_2 and NO_3^- as feedstocks (Fig. 1). A milliampere-level current of urea electro-synthesis could be realized at a remarkably operating potential with the highest FE reported to date. The reaction pathways and intermediates were systematically studied by in situ Raman spectroscopy and differential electrochemical mass spectrometry (DEMS), demonstrating that the rate-determining step of the urea generation from CO_2 and NO_3^- is the $^*\text{NO}_2$ and $^*\text{CO}$ intermediates hydrogenation and coupling on CuWO_4 . Combined with thermodynamic adsorption energy analysis and theoretical calculation, the alternating bimetallic sites effectively improve the formation and coverage of the two intermediates on the surface of the catalyst, increasing the probability of C–N coupling and the selectivity for urea electro-synthesis.

Results

Catalyst synthesis and characterization

The CuWO_4 catalyst was prepared by a hydrothermal synthesis approach using tungstate and Cu salts as raw materials²⁸. The X-ray diffraction (XRD) pattern, Raman and Fourier-transform infrared spectrum of the synthesized sample could be assigned to the CuWO_4 triclinic structure (Fig. 2a, Supplementary Fig. 1)^{29,30}. The X-ray photoelectron spectrum (XPS) of Cu 2p (Fig. 2b) and W 4f (Fig. 2c) exhibited two distinct split spin-orbit peaks located at 934.3 ($\text{Cu}^{2+} 2p_{3/2}$), 954.2 ($\text{Cu}^{2+} 2p_{1/2}$), 35.2 ($\text{W}^{6+} 4f_{7/2}$), and 37.4 eV ($\text{W}^{6+} 4f_{5/2}$), which indicated that Cu and W were in the II and VI oxidation states³¹, respectively. The lattice oxygen (O–Cu or W, 530.1 eV) was observed in O 1s XPS (Supplementary Fig. 2)³². The morphology of the CuWO_4 catalyst manifested as nanoparticles with a size of $40\text{--}60 \text{ nm}$ by scanning electron microscopy (SEM, Fig. 2d) and cryogenic

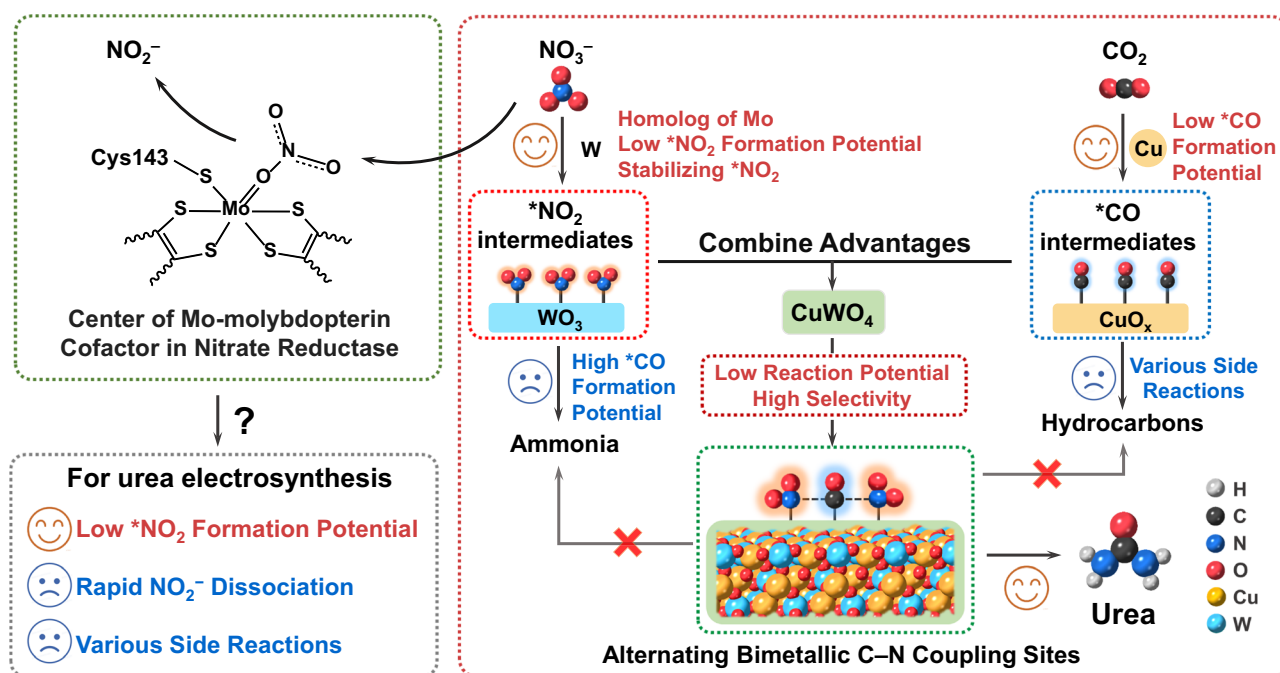


Fig. 1 | Schematic illustration of design strategy for bioinspired alternating bimetallic sites of CuWO_4 catalyst for urea electro-synthesis. The stabilization of the activated $^*\text{CO}$ and $^*\text{NO}_2$ intermediates at Cu and W bimetallic sites may play an important role in the high efficiency of C–N coupling.

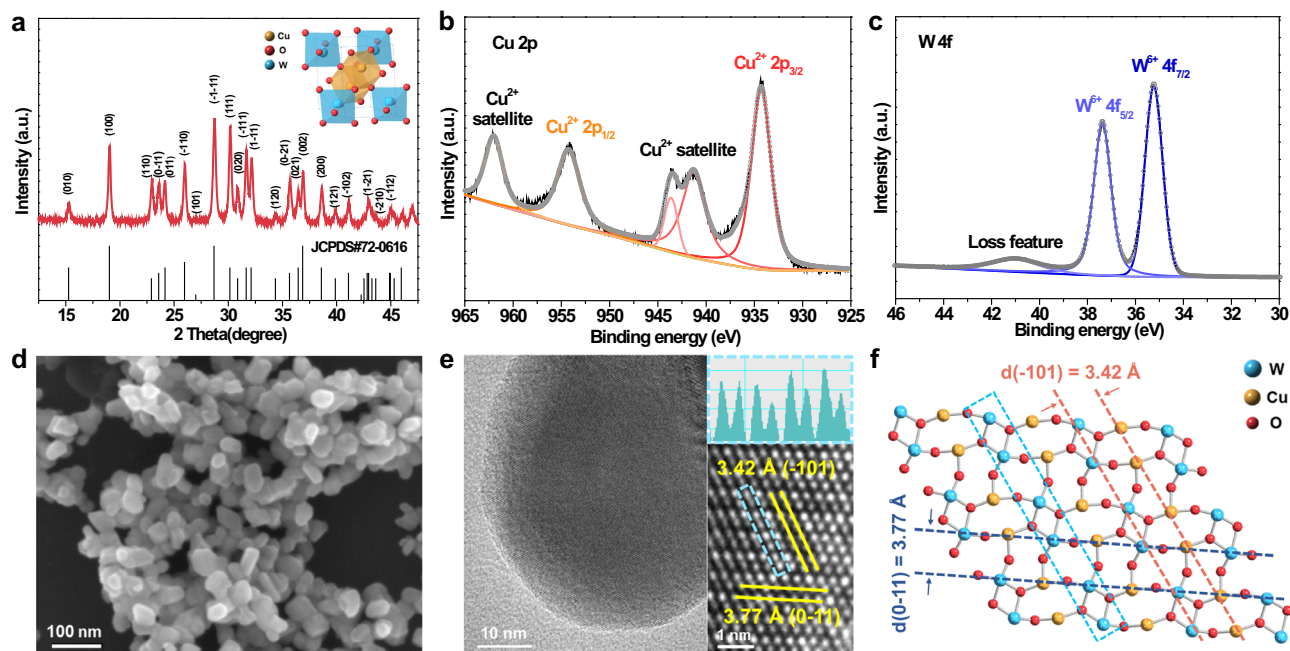


Fig. 2 | Structural and compositional characterization of CuWO_4 catalyst. a XRD pattern. Inset: crystal structure of CuWO_4 . **b**, **c** XPS spectra of Cu 2p (**b**) and W 4f (**c**). **d** SEM image. **e** TEM and atomic-resolution HAADF-STEM image with line profile of the corresponding area. **f** Atomic structure of CuWO_4 (111) facet.

transmission electron microscopy (cryo-TEM, Fig. 2e). Cu, W, and O were homogeneously dispersed throughout the nanoparticle-like catalyst (Supplementary Fig. 3). The entire lattice exhibited highly ordered rectangular arrays with alternating bright and dark columns of atoms (Fig. 2e right), which was revealed by the high-angle, annular dark-field scanning transmission electron microscopy (HAADF-STEM). The transverse and longitudinal array spacings were 3.77 and 3.42 Å, corresponding to the interplanar spacing of (0-11) and (-101) facets, respectively³³. The spacing between metal atoms in the same longitudinal array showed a weak periodic change. The triclinic CuWO_4 crystal structure was constructed (Supplementary Fig. 4) and exhibited the dominant (111) facet (Fig. 2f), which is consistent with the atomic structure in the HAADF-STEM image. Therefore, the synthesized nanoparticles were highly ordered triclinic CuWO_4 and did not contain other detectable impurities such as other derivatives of Cu or W. Pure CuO and WO_3 catalysts were also prepared with similar morphology and valence state to CuWO_4 for comparison; and were fully investigated by various characterization methods (Supplementary Figs. 5–9).

Electrochemical urea synthesis

Electrochemical measurements of urea synthesis were conducted to investigate the catalytic performance of CuWO_4 and other samples (Methods, Supplementary Fig. 10). Figure 3a shows the linear sweep voltammetry (LSV) curves and I - V plots of CuWO_4 , CuO, and WO_3 . When switching the atmosphere of the electrolyzer from Ar to CO_2 , the reduction current of CuWO_4 and CuO increased at the potential range from -0.1 to -0.4 V vs. RHE, indicating that additional CO_2 reduction-related reactions may occur. For WO_3 , no significant difference between the two LSV curves was observed until to the more negative potential region (-0.7 to -0.9 V vs. RHE). For accurately measuring the urea synthesis efficiency of the catalysts at the corresponding potential, the chronoamperometry (CA) method was employed (Methods, Supplementary Fig. 11); and the production of urea was quantified by diacetylmonoxime-thiosemicarbazide (DAMO-TSC) (Supplementary Figs. 12–13) and nuclear magnetic resonance (NMR) methods. As the UV-visible spectral of DAMO-TSC method could be affected by the variation in the concentration of nitrite (Supplementary

Figs. 14–17)^{34,35}. Therefore, the urease decomposition method was further adopted and calibrated by two ammonium ion quantification methods (Supplementary Figs. 18–19). Other N-based by-products such as nitrite, ammonia, and hydrazine were quantitatively analyzed using ion chromatography, indophenol blue, and Watt and Christo's methods, respectively (Methods)^{35,36}. Gas-phase by-products were analyzed by gas chromatography (GC) (Supplementary Figs. 20–25)^{6,37}.

The corresponding FEs and average yield rates were calculated according to Eqs. 1–5. The optimal applied potential for urea synthesis of CuWO_4 was the same as that of CuO (-0.2 V vs. RHE), which is more positive than that of WO_3 (-0.8 V vs. RHE) (Fig. 3b). The peak urea yield rate of $99.5 \pm 3.0 \mu\text{g h}^{-1} \text{mg}^{-1}$ with a remarkable FE as high as $70.9 \pm 2.2\%$ could be obtained for the CuWO_4 catalyst at -0.2 V vs. RHE with a current density of nearly 1.0 mA cm^{-2} . By contrast, the maximum urea yield rate of CuO was $63.9 \pm 2.2 \mu\text{g h}^{-1} \text{mg}^{-1}$ and the maximum FE of $25.4 \pm 2.7\%$. However, for WO_3 , a maximum urea yield rate of $61.7 \pm 1.2 \mu\text{g h}^{-1} \text{mg}^{-1}$ and a urea FE of $24.7 \pm 1.7\%$ could be obtained only at a more negative operating potential (-0.8 V vs. RHE). The electrochemical active surface area (ECSA) was investigated and CuWO_4 still had the highest urea yield after normalization (Supplementary Figs. 26–27). To verify the accuracy of the results, the isotope ^{15}N -labeled potassium nitrate (K^{15}NO_3) was used as the electrolyte for CA measurements, and the yield rates of urea were quantified by ^1H NMR spectroscopy (Fig. 3c, Supplementary Figs. 28–29)⁶. The urea yield rate calibrated by NMR spectra was $98.5 \pm 3.2 \mu\text{g h}^{-1} \text{mg}^{-1}$ with a urea FE of $70.1 \pm 2.4\%$ (Fig. 3d), similar to that measured using the urease method. Other control experiments were also supplemented, and no urea was detected in the absence of CO_2 , NO_3^- , catalyst, or potential (Supplementary Figs. 30–31). Therefore, the generated urea was a result of the coupling of the feeding CO_2 and NO_3^- via the electrocatalysis of CuWO_4 ; and no other C–N coupling products were detected.

Compared with the complex process of coupling CO_2 and NO_3^- to urea, side reactions such as NO_3^- reduction to NO_2^- or NH_3 and HER could occur more easily; as a result, the generation of by-products leads to low FEs of urea for most systems¹⁸. Therefore, investigating the FE of the entire NO_3^- RR (Eq. 6) and the selectivity of products (Eq. 7) will help us understand the advantages of using CuWO_4 (Fig. 3e, f, Supplementary Fig. 21). At the low overpotential region (-0.1 to -0.2 V

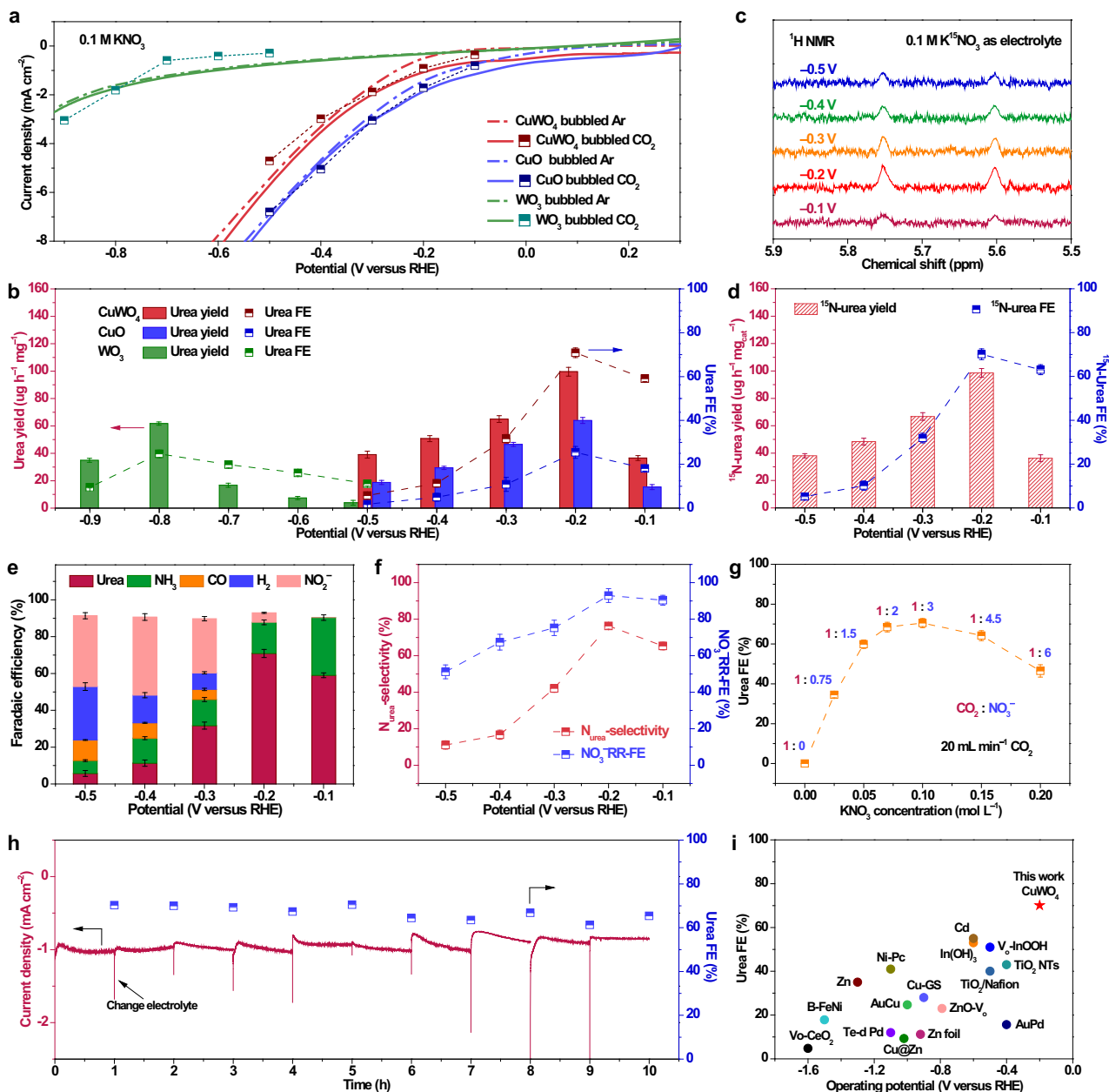


Fig. 3 | Electrochemical synthesis of urea. **a** LSV curves of CuWO_4 , CuO , and WO_3 in 0.1 M KNO_3 with Ar or CO_2 bubbling and I - V plots of CuWO_4 , CuO , and WO_3 in 0.1 M KNO_3 with CO_2 at different potentials. **b** Yield rates and FE values of urea production for CuWO_4 at different applied potentials in 0.1 M KNO_3 with CO_2 bubbling (20 mL min^{-1}). **c** ^1H NMR data of isotope calibration experiment in $0.1\text{ M K}^{15}\text{NO}_3$ with CO_2 bubbling (20 mL min^{-1}) at different applied potentials. **d** ^{15}N -urea yield rates and FEs via integrated peak area from NMR data. **e** FE values of all products for CuWO_4 at different applied potentials in 0.1 M KNO_3 with CO_2

bubbling (20 mL min^{-1}). **f** N_{urea} -selectivity and NO_3^- -RR-FE for CuWO_4 at different applied potentials in 0.1 M KNO_3 with CO_2 bubbling (20 mL min^{-1}). **g** Urea FEs for CuWO_4 at -0.2 V vs. RHE in 0.1 M KNO_3 in different concentrations of KNO_3 electrolyte with CO_2 bubbling (20 mL min^{-1}). **h** Stability test of urea synthesis during 10 h of electrolysis at -0.2 V vs. RHE in 0.1 M KNO_3 with CO_2 bubbling (20 mL min^{-1}). **i** Comparison of the results of this work with state-of-art electrocatalytic synthesis urea catalysts in terms of operation potential and FE. **b**, **d**-**g** Error bars in accordance with the standard deviation of at least three independent measurements.

vs. RHE), the FEs of the entire NO_3^- RR were close to 100%, most of the NO_3^- could react with CO_2 to form urea, and the nitrogen selectivity for urea reached $76.2 \pm 1.7\%$ at -0.2 V vs. RHE. Both the urea yield rate (Fig. 3d) and the nitrogen selectivity (Fig. 3f) gradually decreased under more negative applied potentials, where kinetically favorable competitive reactions occur. Significantly, the CuO could effectively catalyze the reaction of NO_3^- to NO_2^- , which significantly decreased the FE of urea (Supplementary Figs. 16, 23); but WO_3 can effectively avoid the NO_2^- generation (Supplementary Figs. 16, 25). With the assistance of high-valence W reaction center, the competitive reactions for urea synthesis catalyzed by CuWO_4 are effectively suppressed.

The ratio of two reactants may impact the efficiency and selectivity of the reaction. CO_2 with different flow rates was continuously fed, and the performance of CuWO_4 was measured at -0.2 V vs. RHE (Supplementary Fig. 32). When the flow rate of CO_2 was more than 5 mL min^{-1} , the urea FEs remained at approximately 70%; this is because when the flow rates are higher than the consumption rate, the CO_2 concentration remains roughly the same. The flow rate of CO_2 was fixed at 20 mL min^{-1} , and the concentration of KNO_3 in the electrolyte was changed. As shown in Fig. 3g and Supplementary Fig. 33, the urea FEs had a volcano peak-shaped distribution, reaching a peak at the KNO_3 concentration of 0.1 M . As the saturated concentration of CO_2

(0.033 M) in aqueous solution at standard temperature and pressure, the ratios of CO_2 and NO_3^- in different concentrations of KNO_3 aqueous solution were 1:0, 1:0.75, 1:1.5, 1:2, 1:3, 1:4.5, and 1:6. Considering that the mass transfer efficiency of CO_2 may be higher owing to the small amount of bubble transport, the actual ratio of CO_2 and NO_3^- in 0.1 M KNO_3 may be closer to the stoichiometric ratio of C and N atoms in urea, which is more conducive to a higher FE and the formation of urea. In addition, no other C–N coupling products (such as methylamine, ethylamine, formamide, acetamide, etc) were detected when the ratios of CO_2 and NO_3^- changed.

The durability and reproducibility of CuWO_4 toward urea electrosynthesis were also examined. As shown in Fig. 3h, the CuWO_4/CP electrode maintained a relatively stable operation current density of approximately 1.0 mA cm^{-2} for 10 h at -0.2 V vs. RHE with an average urea FE of 68.0%. The longer-term continuous electrolysis was also performed, and after 20 h of electrolysis without electrolyte renewal, the Faradaic efficiency of urea was 56.4% (Supplementary Figs. 34–35). The final Faradaic efficiency remained above 50% after three 20 h long-term repeated tests, demonstrating excellent reproducibility. After the reaction, no appreciable topography and crystal structure changes were observed for CuWO_4 (Supplementary Figs. 36–38). The only change detected is the binding energy of Cu on the surface of the CuWO_4 after electrolysis immediately transfer to the XPS under the protection of Ar (Supplementary Fig. 39)³⁸, indicating that the crystal structure of CuWO_4 is stable, and the lower valence state Cu involved during the electrosynthesis. Moreover, no evident vibrational changes of CuWO_4 (Supplementary Fig. 40) and WO_3 (Supplementary Fig. 41) were found in in situ Raman spectra at operating potentials. By contrast, for CuO, multiple vibration peaks corresponding to Cu_2O and other Cu derivatives appeared after applying the working potentials (Supplementary Fig. 42)^{39,40}. And the valence state of Cu in CuO did not change completely back to Cu^{2+} after exposure to air, due to the structural transformation of CuO (Supplementary Figs. 42–43).

The FE of urea and the operating potential of this work were compared with those of previous reports (Fig. 3i and Supplementary Table 1)^{41–45}; the FEs of urea in previous works were less than 53%, and the operating potentials were more negative than -0.4 V . The CuWO_4 catalyst system significantly improved the urea FE ($70.1 \pm 2.4\%$) and reduced the operating potential (-0.2 V vs. RHE) with a current density of nearly 1.0 mA cm^{-2} .

Unraveling the origin of C–N bond formation and reaction mechanism

As CuWO_4 can obtain high FEs of urea at low operating potentials, an in-depth understanding of the C–N bond formation mechanisms of NO_3^- and CO_2 co-reduction mechanism and structure–function relationship of CuWO_4 is attractive, which may be helpful for the development of more advanced catalytic systems.

In situ Raman spectroscopy (Supplementary Fig. 44 shows the setup) was used to probe the stretching vibrations of generated intermediates on the surface of the CuWO_4 under working conditions. Compared with the vibration peaks of NO_3^- (1048 and 1365 cm^{-1}) under Ar-saturated conditions, new peaks at 1060 and 1351 cm^{-1} corresponding to $^*\text{CO}_3^{2-}$ and $^*\text{HCO}_3^-$ species, respectively, emerged after CO_2 bubbling (Fig. 4a) at the open circuit state^{46,47}. At the working state (potential range from 0.1 to -0.3 V vs. RHE), the peak at 1979 cm^{-1} could be observed when the potential reached -0.1 V vs. RHE, which is assigned to the $^*\text{CO}$ on bridge sites⁴⁸. Moreover, when the applied potential increased, the peak intensities of $^*\text{CO}_3^{2-}$ and $^*\text{HCO}_3^-$ gradually decreased, indicating that $^*\text{CO}$ came from these derivatives of CO_2 . Interestingly, only one NO_3^- reduction species could be detected at 1428 cm^{-1} at the working state, corresponding to the $\nu(\text{N}=\text{O})$ of $^*\text{NO}_2$ intermediate in bridging configuration⁴⁹. Under the potential of -0.2 V vs. RHE, the maximum peak intensities of 1428 and 1979 cm^{-1} were reached, indicating that the highest coverage of $^*\text{NO}_2$ and $^*\text{CO}$

intermediates on the surface of CuWO_4 can be received. It is in agreement with the best-applied potential (-0.2 V vs. RHE) for the highest rate and FE of urea formation. As reaction intermediates irrelevant to the rate-determining step, and the product of rate-determining step could be rapidly consumed, which are difficult to be observed by non-time-resolved characterization methods. Thus, the undissociated intermediates that serve as substrates for the rate-determining step can be observed in Raman spectra³⁷. Therefore, assuming that $^*\text{NO}_2$ and $^*\text{CO}$ are the key intermediates in urea formation is reasonable, and the C–N bond formation between $^*\text{NO}_2$ and $^*\text{CO}$ coupling is very likely the rate-determining step of the urea electrosynthesis reaction on the surface of CuWO_4 . In contrast, various species from NO_3^- and CO_2 reduction can be observed on the surface of the CuO (Supplementary Fig. 45). Stretching peaks of $^*\text{CHO}$ and $^*\text{CH}_3\text{O}$ species at 1048 and 1110 cm^{-1} are observed in the range from -0.3 to -0.5 V vs. RHE, which is consistent with the increased yield rate of methane (Supplementary Fig. 23)⁵⁰. A variety of nitrogenous intermediates with weak peak intensities are observed, indicating that the coverage of nitrogenous intermediates was low, which are in agreement with the low yield rate and FEs of urea for CuO. The WO_3 exhibited a mismatch between the reduction potentials of CO_2 and NO_3^- (Supplementary Fig. 46). The stretching peak at 2000 cm^{-1} , corresponding to the $^*\text{CO}$ on atop sites^{48,51}, could not be observed until the potential reached -0.6 V vs. RHE. As the applied potential changed, the intermediates of NO_3^- reaction on the surface of WO_3 changed. In the range from -0.2 to -0.4 V vs. RHE, the main intermediate of NO_3^- reduction was $^*\text{NO}_2$, which is consistent with the observed for CuWO_4 . When the applied potential increased from -0.5 to -0.7 V vs. RHE, the vibration peaks at 1143, 1163, 1390, and 1533 cm^{-1} gradually appeared, corresponding to $\nu(\text{N}=\text{O})$ and $\nu(\text{N}=\text{O})$ of nitrito orientation, and $\nu(\text{N}=\text{O})$ of nitroxyl for chelating nitrito⁴⁹. These results explain the more negative potential requirement and low selectivity for WO_3 , which is because the generation of $^*\text{CO}$ intermediate requires a relatively negative applied potential; at such a relatively negative potential range, the NO_3^- reaction intermediate transformed from $^*\text{NO}_2$ to other intermediates.

To further verify the speculations above, NO_2 -temperature-programmed gas desorption (TPD) and CO-TPD were conducted to evaluate the thermodynamic adsorption energy of $^*\text{NO}_2$ and $^*\text{CO}$ on the surface of CuO, WO_3 , and CuWO_4 . As shown in Fig. 4b, no evident NO_2 desorption peak was observed on the CuO NO_2 -TPD curve, which means that the CuO surface hardly adsorbed NO_2 . On the contrary, WO_3 showed a good adsorption capacity for NO_2 with a desorption peak in the low-temperature region ($<200 \text{ }^\circ\text{C}$) and multiple desorption peaks in the high-temperature region ($200\text{--}400 \text{ }^\circ\text{C}$), representing the physical and chemical adsorptions of NO_2 on the WO_3 surface, respectively⁵². The NO_2 -TPD curve of CuWO_4 also shows a series of NO_2 desorption peaks. However, the strength is weaker than that of WO_3 , indicating that CuWO_4 has a moderate adsorption capacity for $^*\text{NO}_2$ intermediate by balancing the properties of CuO and WO_3 . It is also consistent with the results of nitrite formation of the three catalysts (Supplementary Fig. 16). For the CO-TPD measurement (Supplementary Fig. 47), the peak strength of CO desorption for WO_3 in both low and high-temperature regions was higher, indicating that WO_3 had a stronger CO-adsorption capacity. CuO also showed a certain degree of chemical adsorption for CO. With the influence of octahedral $[\text{WO}_6]$ clusters, the physical adsorption of CO by CuWO_4 significantly increased; however, the CO chemical adsorption capability of CuWO_4 was the same as that of CuO, suggesting that CuWO_4 maintains the advantages of higher physical adsorption ability of the W sites, and the favorable chemical adsorption capability of Cu sites for the $^*\text{CO}$ intermediate. Therefore, as predicted, CuWO_4 could provide appropriate adsorption and stabilization capability for both $^*\text{NO}_2$ and $^*\text{CO}$ intermediates compared to WO_3 and CuO, which is consistent with the in situ Raman spectroscopy results.

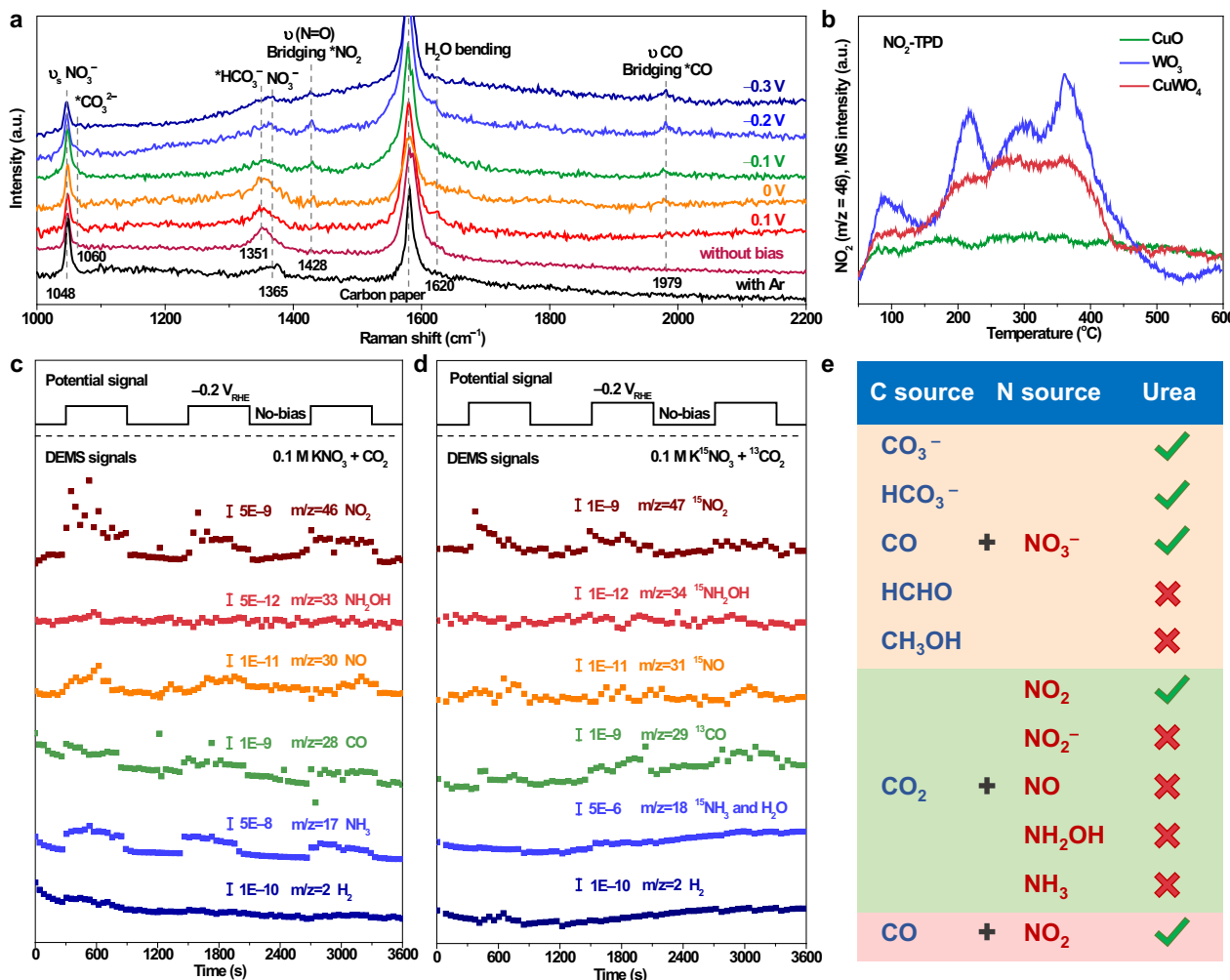


Fig. 4 | In-situ characterization and inference of intermediate species. **a** In situ Raman spectra of CuWO₄ in 0.1 M KNO₃ with CO₂ bubbling at different applied potentials or Ar bubbling at open circuit state. **b** NO₂-temperature programmed gas desorption (TPD) of CuWO₄, CuO, and WO₃. **c** Online DEMS of CuWO₄ in 0.1 M

KNO₃ with saturated CO₂ at -0.2 V vs. RHE. **d** Online DEMS of CuWO₄ in 0.1 M K¹⁵NO₃ with saturated ¹³CO₂ at -0.2 V vs. RHE. **e** Control experiment results of different carbon and nitrogen sources for speculating the urea synthesis mechanism.

Differential electrochemical mass spectrometry (DEMS) can detect the products of the dissociated electrochemical-generated intermediates on the surface of the catalyst (Supplementary Fig. 48)³⁸. The mass-to-charge ratio (*m/z*) signals of 2, 17, 28, 30, 33, and 46 corresponding to H₂, NH₃, CO, NO, NH₂OH, and NO₂, respectively, were recorded (Fig. 4c). For CuWO₄, the signals of NH₃ (*m/z* = 17), CO (*m/z* = 28), NO (*m/z* = 30), and NO₂ (*m/z* = 46) showed fluctuations consistent with the switching cycles of open circuit and working states (at -0.2 V vs. RHE). The high captured signal strengths of NH₃ (*m/z* = 17) corroborate that NH₃ is the main by-product for CuWO₄ at the applied potential of -0.2 V vs. RHE. Considering that a small amount NO may come from the disproportionation reaction of NO₂ and the reaction during NH₃ production, the observation of NO₂ and CO, the dissociated electrochemical-generated intermediates, suggests that *NO₂ and *CO are the critical intermediates for the C-N bond formation on the CuWO₄ surface, which also corroborates the in situ Raman measurements. To confirm these results, the reactants KNO₃ and CO₂ were replaced with K¹⁵NO₃ and ¹³CO₂. As shown in Fig. 4d, corresponding isotopic molecule signals of ¹³CO (*m/z* = 29), ¹⁵NO (*m/z* = 31), and ¹⁵NO₂ (*m/z* = 47) could be detected, indicating that *CO and *NO₂ intermediates were generated from the reduction of CO₂ and NO₃⁻ rather than pollutants. The signals of NH₃ (*m/z* = 17) and NO₂ (*m/z* = 46) could be detected for WO₃ (Supplementary Fig. 49a); however, CO (*m/z* = 28) could not be clearly observed, which confirms that WO₃ can only reduce NO₃⁻ to produce NH₃ rather than trigger urea generation at -0.2 V vs. RHE, and that *CO generation potential is mismatched with that of NO₂ formation (Supplementary Fig. 46). For CuO (Supplementary Fig. 49b), relatively high signal strengths of NO₂ (*m/z* = 46) and CO (*m/z* = 28) could be detected, which is identical to the results that urea generation could occur at -0.2 V vs. RHE. However, these signals displayed a pulse-like intensity decay, which may be attributed to the weaker adsorption capacity of intermediates or insufficient structural stability of CuO. At the same time, considerable CO, H₂, and NH₃ were observed, which is consistent with the lower selectivity of urea electro-synthesis for CuO (Supplementary Fig. 23c).

The C- or N-sources were further changed to screen the C-N coupling process. Derivatives of CO₂ in the aqueous phase (CO₃⁻ and HCO₃⁻) and the desorption species (CO, HCHO, and CH₃OH) of the intermediates generated during the CO₂ reduction were used as the C-source for urea electro-synthesis with NO₃⁻. As shown in Fig. 4e and Supplementary Table 2, CO₃⁻, HCO₃⁻, and CO can be co-reactants with NO₃⁻ for urea electro-synthesis by CuWO₄; HCHO and CH₃OH, the deeper CO₂ reduction products, cannot conduct the process for CuWO₄; which confirms that the *CO should be the key CO₂ reduction intermediate on CuWO₄ before C-N coupling. By contrast, NO₂, NO₂⁻, NO, NH₂OH, and NH₃, possible desorption species of the

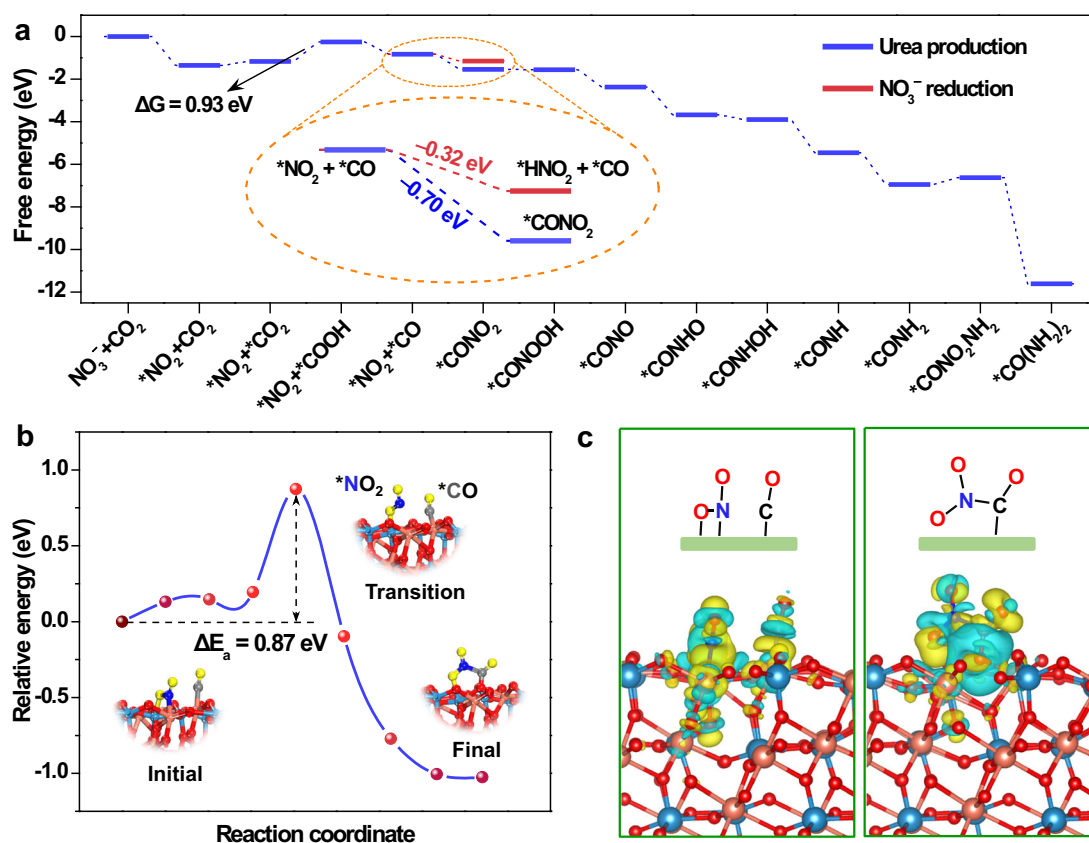


Fig. 5 | DFT calculation of urea synthesis mechanism on bimetallic CuWO_4 (111) surface. a Free-energy diagram for urea production and NO_3^- reduction on the CuWO_4 (111) facet. **b** Mechanism of C–N coupling between $^*\text{CO}$ and $^*\text{NO}_2$. The initial, transition, and final states during the $^*\text{CONO}_2$ formation are presented. Gray, blue, red, orange, cyan, and yellow balls represent C, N, lattice O, Cu, W, and

adsorbate O, respectively. **c** Charge density difference of the co-adsorption state of $^*\text{CO}$ and $^*\text{NO}_2$ (left side), and adsorbate $^*\text{CONO}_2$ (right side) on the CuWO_4 (111) facet. The iso-value is $0.002 \text{ e}/\text{\AA}^3$. Electron accumulation and depletion are represented by yellow and cyan sections, respectively.

intermediates for NO_3^- RR, were used as the N-source for urea electro-synthesis with CO_2 . The results show that only NO_2 can serve as the co-reactant with CO_2 to form urea for CuWO_4 , inferring that $^*\text{NO}_2$ should be the critical NO_3^- reduction intermediate in the process of C–N coupling for urea generation. Electro-synthesis of urea on the surface of CuWO_4 could also occur when CO and NO_2 were used as feedstocks, further proving that $^*\text{CO}$ and $^*\text{NO}_2$ are the critical intermediates in the reaction pathway of urea electro-synthesis on the CuWO_4 surface.

To further unravel the fundamental origins of the high selectivity of CuWO_4 , density functional theory (DFT) calculations (Methods) were conducted on the preferentially oriented in the (111) direction of CuWO_4 crystal (Supplementary Fig. 50) corresponding to the XRD and TEM results. Figure 5a and Supplementary Fig. 51 show the detailed free-energy diagram of the corresponding structures with the lowest energy pathway from CO_2 and NO_3^- to urea. The reaction started with the reduction of NO_3^- to $^*\text{NO}_2$ with strong adsorption-free energy of -1.35 eV. By contrast, CO_2 was first physically adsorbed on the surface of CuWO_4 . The hydrogenation of $^*\text{CO}_2$ is a potential determining step with a 0.93 eV uphill in reaction-free energy; whereafter, the $^*\text{COOH}$ was spontaneously reduced to $^*\text{CO}$ thermodynamically. As shown in Supplementary Fig. 51, in the relevant atomic configurations with the lowest energy, the $^*\text{NO}_2$ intermediate was adsorbed at the bridging nitro with the N bonding to Cu and O bonding to W, suggesting that the W sites play an important role in stabilizing $^*\text{NO}_2$. Whereas, the $^*\text{CO}$ intermediate was located at the bridge site between two Cu atoms, consistent with the in situ Raman results. As the $^*\text{CO}$ was formed,

the $^*\text{NO}_2$ intermediate was involved in the urea production. In contrast to the reaction-free energy for hydrogenation of $^*\text{NO}_2$ to $^*\text{HNO}_2$ (-0.32 eV), the lower reaction-free energy of -0.70 eV for $^*\text{CONO}_2$ formation (insert in Fig. 5a) on the surface of CuWO_4 was beneficial for the direct C–N coupling at a very early stage. Simultaneously, the reaction-free energies of $^*\text{CO}$ to $^*\text{CHO}$ (0.17 eV) and $^*\text{CO}$ to $^*\text{COH}$ (2.12 eV) are higher compared to the C–N coupling process (-0.70 eV, Supplementary Fig. 52). As a result, the NH_3 -related or $^*\text{CO}$ hydrogenation side reactions could be significantly suppressed, which may explain the high selectivity of urea production by CuWO_4 . Although the free energy of C–N bonding between $^*\text{NO}_2$ and $^*\text{CO}$ is lower thermodynamically, an activation energy barrier as high as 0.87 eV for the $^*\text{CONO}_2$ formation process exists (Fig. 5b), making the coupling of $^*\text{CO}$ and $^*\text{NO}_2$ a slow kinetics process compared to the other elementary reactions during urea production, which is in agreement with the experimental results that the C–N bond formation between $^*\text{NO}_2$ and $^*\text{CO}$ is the rate-determining step. Further calculations of the charge density difference of $^*\text{NO}_2$ and $^*\text{CO}$ adsorbed states on the (111) facet of CuWO_4 were investigated (Supplementary Fig. 53). The electrons on the CuWO_4 could transfer to the $^*\text{CO}$ and $^*\text{NO}_2$, corresponding to the nature of the reduction reaction, which enables the improvement of their intrinsic activity and realizes the C–N coupling between the two intermediates¹⁶. Compared with the change of charge region before and after C–N bonding (Fig. 5c) an evident electron exchange between the $^*\text{CO}$ and $^*\text{NO}_2$ intermediates was observed; the electrons mainly flowed from the C atom of $^*\text{CO}$ to the N atom of $^*\text{NO}_2$, and completed the C–N coupling. The further hydrogenation of

*CONO₂ to *CONH₂ intermediate can occur in an energetically favorable pathway, which has an advantage over the formation of *CONONO₂, *CONHONO₂, and *CONHNO₂ in the reaction-free energy (Supplementary Fig. 54). Although the free energy of the coupling of *CONH₂ with the second *NO₂ increased slightly, it was not sufficient to prevent a thermodynamically spontaneous pathway of urea formation. These results theoretically confirm that the rate-determining step is the C–N coupling between the *CO and *NO₂ intermediates on the surface of CuWO₄ for urea electro-synthesis. Furthermore, the lower reaction-free energy of the C–N coupling between the *CO and *NO₂ intermediates and the thermodynamically spontaneous formation pathway determine the extremely high selectivity of urea electro-synthesis on the surface of CuWO₄, in line with the preceding experimental analysis.

Discussion

Inspired by the efficient nitrate assimilation process by the high-valence Mo-based reaction center of nitrate reductase in nature, CuWO₄ catalyst with the high-valence W reaction centers was designed and employed for urea electro-synthesis with CO₂ and NO₃[−] as the feedstocks. The prepared CuWO₄ could achieve highly efficient urea production with a 98.5 ± 3.2 μg h^{−1} mg^{−1}_{cat} urea yield at −0.2 V vs. RHE and high FE of 70.1 ± 2.4%. As evidenced by in situ Raman, TPD, DEMS, C/N-sources changing experiments, and theoretical calculation, early C–N coupling originating for urea electro-synthesis from *NO₂ and *CO intermediates on the surface of CuWO₄ was verified. Owing to the relative positive formation potential and appropriate adsorption ability of *NO₂ and *CO intermediates on the alternating bimetallic W and Cu sites, CuWO₄ optimized the coupling for these critical intermediate species. The lower energy barrier of direct coupling of *NO₂ and *CO enabled the C–N coupling to easily occur. As primary intermediates of NO₃[−] and CO₂ reduction, the coupling of *NO₂ and *CO decreased the possibility of intermediates desorption from complex elementary reactions before the C–N formation, which inhibits other side reactions. This study may also provide new inspiration for designing electrochemical synthesis systems to produce a broader range of high-value C–N bond compounds.

Methods

Preparation of catalysts

CuWO₄ nanoparticles were synthesized by the hydrothermal method. Na₂WO₄·2H₂O (0.33 g) and CuSO₄ (0.16 g) were dissolved in 20 mL of ultrapure water, respectively. In sequence, the Na₂WO₄-solution was slowly dripped into the solution of CuSO₄ under vigorous stirring. The mixture was transferred to a Teflon-lined stainless steel autoclave (50 mL), and maintained at 180 °C for 20 h in an oven. For CuO nanoparticles, 20 mL of 0.5 M Na₂CO₃ was slowly dripped into CuSO₄ solution (0.16 g in 20 mL H₂O) under vigorous stirring. For WO₃ nanoparticles, HCl solution (0.1 M, 20 mL) was slowly dripped into the Na₂WO₄-solution (0.33 g in 20 mL H₂O) under vigorous stirring. The hydrothermal synthesis procedures were the same as that of CuWO₄. After hydrothermal synthesis, all samples were separated and washed by centrifugation. Ultimately, all samples were calcined at 500 °C in the air for 2 h to remove organic pollutants and improve the crystallinity.

Electrode preparation and electrochemical measurements

All electrochemical measurements were conducted on a CHI760E electrochemical instrument. A mass loading of 1 mg cm^{−2} was used on carbon paper (CP) working electrodes in a three-electrode H-cell electrolyzer, at room temperature and atmospheric pressure. 0.01 g of catalyst powders and 50 μL of Nafion solution were dissolved in 1 mL of ethanol as the ink. Subsequently, catalyst ink (100 μL) was coated on carbon paper (Toray O60) (geometric area 1 × 1 cm²), and the working

electrode was obtained after drying (catalyst loading of 1 mg cm^{−2}). A Nafion 117 membrane (Dupont) was used for separation. A ruthenium oxide-coated titanium sheet was used as the counter electrode. A leaking-free Ag/AgCl (saturated KCl) electrode was used as the reference electrode. KNO₃ solutions (0.1 M as N-source) with or without high-purity CO₂ (20 mL min^{−1} with bubbling, as C-source) were employed as the optimized electrolytes for the electrochemical measurements. Before tests, the corresponding gas was used to pre-saturate the electrolyte of the cathode part. In the electrolytic process, the gas flow rate was set as 20 mL min^{−1}. The LSV measurements were performed with a negative scan direction and a scan speed of 10 mV/s. For each experiment, the applied potential was converted to scales of RHE according to $E_{(vs.RHE)} = E_{(vs.Ag/AgCl)} + E_{Ag/AgCl vs. RHE}$, where $E_{Ag/AgCl vs. RHE}$ is the potential difference between the Ag/AgCl electrode and a commercialized RHE (HydroFlex®) under corresponding conditions (such as saturated Ar or CO₂). The same methods were adopted for isotope-labeling experiments and operando Raman measurements.

Quantitative analysis and identification of urea, ammonia, nitrite, and hydrazine

The content of urea, ammonia, and hydrazine was determined by urease, diacetylmonooxime, indophenol blue, and Watt and Christo, respectively^{6,15}. For the urease decomposition method, 0.5 mL of urease solution (urease: 5 mg mL^{−1}) was added into 4.5 mL of electrolyte, and then reacted at 40 °C for 40 min. The urease solution also contained 0.1 g ethylenediaminetetraacetic acid disodium salt and 0.49 g K₂HPO₄ per 100 mL. Then, the NH₃ concentrations of electrolyte before and after decomposition were detected by ion chromatograph and indophenol blue method. The urea yield was calculated according to the NH₃ concentrations before and after decomposition. For the diacetylmonooxime method, two chromogenic solutions, A and B, were prepared. For solution A, 10 mL of phosphoric acid, 30 mL of concentrated sulfuric acid, and 10 mg of ferric chloride were added to 60 mL of deionized water; finally, deionized water was added such that the volume reached 100 mL. For solution B, 0.5 g of diacetylmonooxime and 10 mg of thiosemicarbazide were dissolved in 100 mL of deionized water. 1 mL of the post-test electrolyte was mixed with 2 mL of solution A and 1 mL of solution B and heated at 100 °C for 15 min. After cooling, the absorbance of the solution at 525 nm was measured by a UV-vis spectrophotometer (Thermo One Plus). The calibration was performed using a standard concentration-absorbance curve of urea solution, including urea concentrations in the electrocatalytic test (Supplementary Fig. 12). For the indophenol blue method, 10 mL of electrolyte was added to 2 mL of salicylic acid solution (5 wt%), 1 mL of sodium hypochlorite solution (0.05 mol L^{−1}), and 0.2 mL of sodium nitrosotetrafluoroborate solution (1 wt%). After uniform mixing, the sample solution was placed for 45 min and tested with a UV-vis spectrophotometer (at 655 nm). The calibration was performed using a standard concentration-absorbance curve of ammonia solution, including ammonia concentrations in the electrocatalytic test (Supplementary Fig. 18). The concentration of ammonium ion in the electrolyte was also detected by ion chromatography (Thermo Scientific Dionex Aquion). The calibration was performed using a standard chromatographic curve of ammonium solution, including ammonium concentrations in the electrocatalytic test (Supplementary Fig. 19). For Watt and Christo's method, 5 mL of a reagent consisting of a mixture of p-dimethylaminobenzaldehyde (5.99 g), concentrated hydrochloric acid (30 mL), and ethanol (300 mL) was added to 5 mL of electrolyte. The absorbance of the resulting solution was measured at 455 nm. The concentration of nitrite ions in the electrolyte was detected by ion chromatography (Thermo Scientific Dionex Aquion). The calibration was performed using a standard chromatographic curve of nitrite solution, including nitrite concentrations in the electrocatalytic test (Supplementary Fig. 14).

The FE is the ratio of the number of electrons transferred between the formation of products and the total current flowing through the circuit. As 16 electrons are required to form a urea molecule, and 8 electrons are required to form an NH₃ molecule, the FE of urea and NH₃ can be calculated, respectively, as follows:

$$FE_{\text{urea}}(\%) = (16 \times F \times c_{\text{urea}} \times V) / (60.06(\text{g/mol}) \times Q) \times 100\%, \quad (1)$$

$$FE_{\text{NH}_3}(\%) = (8 \times F \times c_{\text{NH}_3} \times V) / (17(\text{g/mol}) \times Q) \times 100\%, \quad (2)$$

$$FE_{\text{NO}_2}(\%) = (2 \times F \times c_{\text{NO}_2} \times V) / (46(\text{g/mol}) \times Q) \times 100\%, \quad (3)$$

where c_{urea} and c_{NH_3} ($\mu\text{g/mL}$) are the measured urea and NH₃ concentrations, respectively; V (mL) is the total volume of the electrolyte, F is the Faraday constant ($96,485.3 \text{ C mol}^{-1}$); and Q (C) is the total charge passed through the working electrode.

The average yield rates of urea and NH₃ were calculated according to the following equation.

$$R_{\text{urea}} = (c_{\text{urea}} \times V) / (t \times m), \quad (4)$$

$$R_{\text{NH}_3} = (c_{\text{NH}_3} \times V) / (t \times m), \quad (5)$$

where t is the time (h) for electrocatalysis and m is the catalyst loading (mg).

The NO₃-RR-FE was calculated as follows:

$$FE_{\text{NO}_3\text{RR}}(\%) = \frac{Q_{\text{NO}_3\text{RR}}}{Q} \times 100\%, \quad (6)$$

where $Q_{\text{NO}_3\text{RR}}$ represents the charge consumed by the products involved in nitrate reduction.

The $N_{\text{urea-selectivity}}$ was calculated as follows:

$$N_{\text{urea-selectivity}} = n_{\text{urea}} / n_{\text{total}}, \quad (7)$$

where n_{urea} is the number of moles of nitrogen in as-produced urea, and n_{total} is the total number of moles of N atoms in the products from NO₃-RR.

Isotope-labeling product quantification and identification

The isotope-labeling experiments for the identification of products were conducted using a solution of 0.1 M K¹⁵NO₃ as the electrolyte. The concentrations of ¹⁵N-urea and ¹⁵N-ammonia were both quantified by NMR^{6,37}. For NMR sample preparation, the test solution was mixed with dimethyl sulfoxide at a ratio of 9:1 and shaken evenly. The NMR solution used to detect ammonia was adjusted to a pH of 3 by adding an appropriate amount of 1.0 M HCl solution. The NMR test was conducted under the water suppression mode with a scanning circle of 420 times. ¹⁵N-urea and ¹⁵NH₄Cl were used to prepare the standard solution, and the standard linear curves between the NMR signal and the product concentration were established (Supplementary Fig. 28). The yield rates and FEs were calculated by reference to the calculation formula in the spectrophotometer method.

Quantitative analysis of other gas and liquid-phase products

The yield rates of CO, CH₄, H₂, and N₂ in gas products were determined by an online gas chromatograph (GC-2014, Shimadzu) with thermal conductivity and flame ionization detectors. Other liquid-phase products were identified by ¹H NMR.

NO₂ and CO temperature program desorption

The NO₂- and CO-TPD measurements were completed by AutoChem 2920 temperature program instrument and Hiden QIC-20 mass spectrometer. First, the catalyst was pretreated, and the temperature was raised to 200 °C with Ar flow for 0.5 h. In sequence, the catalyst was cooled down to 25 °C and exposed to NO₂ or CO flow of 30 mL min⁻¹ for 30 min. Before desorption, the sample was flushed in Ar gas for 10 min. Subsequently, NO₂ or CO desorption was performed in the range of 25–600 °C at a heating rate of 10 °C min⁻¹ under an Ar flow of 30 mL min⁻¹. The mass-to-charge ratio (m/z) signals of 28, 44, and 46 corresponding to CO, CO₂, and NO₂, respectively, were recorded.

In-situ Raman spectroscopy measurements

In-situ Raman spectra were obtained from a homemade H-type three-electrode spectroelectrochemical cell with an embedded quartz window under the same working conditions of activity measurements (Supplementary Fig. 44 shows the experimental setup). The electrochemical workstation provided the corresponding applied potential. Before electrolysis, Ar or CO₂ was injected into the electrolyte for 20 mins to purge, and the gas flow rate was maintained at 20 mL min⁻¹ during the electrolysis. The Raman data was recorded after 15 mins of electrolysis to ensure that enough intermediates had accumulated on the surface of the catalyst. The laser intensity, the data recording circle, and the sweep speed were kept consistent.

XPS measurement after electrolysis

The CuWO₄ and CuO electrodes were electrolyzed for an hour under at -0.2 V vs. RHE in 0.1 M KNO₃ with CO₂ bubbling (20 mL min⁻¹). After the test, the electrodes were treated instantly with deionized water and vacuum drying (20 °C). The Ar-protected samples were transferred to an Ar-filled sealed chamber for storage. The samples, which were not protected by Ar, were exposed to air for an hour. Then, the two types of samples were tested together by XPS.

DEMS measurements

Differential electrochemical mass spectrometry (DEMS) test employed a high precision three-stage filter quadrupole mass analyzer with softer ionization (Ionic energy: 4–150 eV) (Supplementary Fig. 48a). Hiden QMS has a unique soft ionization technology. By optimizing the tuning of the electron energy of the EI source, the fragmentation peak can be reduced and the prominent molecular ion peak can be strengthened, which achieves the purpose of reducing interference. The DEMS cell was a dual thin-layer flow cell customized by Hiden, which was reported in previous work (Supplementary Fig. 48b)⁵³. The working electrode was a custom-made glass carbon electrode uniformly coated with 50 μL catalyst ink (in Electrochemical measurements). The counter electrode was a ruthenium oxide electrode. Nafion 117 membrane was used as the separation membrane. The reference electrode was an Ag/AgCl electrode calibrated by a commercial RHE (HydroFlex). The electrolyte was 0.1 M KNO₃ solution, and the cathode electrolyte was saturated with CO₂. A microinjector ensured electrolyte flow in the DEMS cell at a flow rate of 200 $\mu\text{L min}^{-1}$. The electrochemical workstation provided the corresponding applied potential. In isotope-labeling experiments, 0.1 M K¹⁵NO₃ and ¹³CO₂ were used as feedstocks.

DFT calculations

All the DFT calculations in this work were conducted using the Vienna ab initio simulation program (VASP)^{54,55}. The core-valence interactions were described by the projector-augmented wave (PAW) method^{56,57}, and the cut-off energy of plane-wave basis expansion was set to 450 eV. All spin-polarized calculations were performed by the generalized gradient approximation (GGA) and Perdew–Burke–Ernzerhof (PBE) for the exchange and association of functions⁵⁸. The lattice constants were calculated to be $a = 4.681 \text{ \AA}$, $b = 5.867 \text{ \AA}$, and $c = 4.898 \text{ \AA}$, consistent with previous results, including calculated constants and experiment

values^{58–61}. For the surface construction, the CuWO₄ surface was cleaved along a (111) direction, which is the dominant surface observed in XRD. A p(2 × 2) CuWO₄ (111) surface with six atomic layers was modeled. The two atomic layers at the bottom remain fixed to mimic the bulk phase, while the other layers were fully relaxed. A -15 Å vacuum layer was employed to eliminate the interaction of adjacent slabs. The free molecules of HNO₃, H₂O, H₂, and CO₂ were placed in a (15 × 15 × 15) Å³ cubic box to diminish the interplay between neighboring molecules. A 2 × 2 × 1 Monkhorst–Pack k-point mesh sampling was utilized for all optimizations. When the forces on the relaxed atoms became less than 0.05 eV/Å, and the energies in the self-consistent iterations reached 10⁻⁵ eV, the optimized structures converged. The van der Waal (vdW) interaction was described using the DFT-D3 method^{62,63}. The climbing image nudged elastic band (CI-NEB) method was used for locating the transition states (TSS)^{64,65}.

The Gibbs free energy can be expressed as:

$$\Delta G = \Delta E + \Delta ZPE - T \cdot \Delta S, \quad (8)$$

where ΔE is the reaction energy calculated by the DFT methods. ΔZPE and $T \cdot \Delta S$ are the thermodynamic corrections of zero-point-energy (ZPE) and entropy (S) derived from the vibrational partition function at 298.15 K, respectively. Gaussian 03 software package was used for gas-phase species to calculate the thermodynamic corrections for the ideal gas approximation.

Reporting summary

Further information on research design is available in the Nature Portfolio Reporting Summary linked to this article.

Data availability

All data that support the findings of this study are present in the paper and the Supplementary Information. Additional data related to the study are available from the corresponding author upon reasonable request.

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Author contributions

Y.Z., L.S., and Fu.L. conceived the project design and initiated the project. Y.Z. performed catalyst synthesis, most of the structural characterization, and electrochemical measurements. All spectra and electrochemical kinetics data were analyzed and interpreted by Y.Z. and Fu.L. Y.D. performed DFT calculations. W.L. and C.L. performed operando Raman spectra measurements and data analysis. Y.L. performed the SEM and TEM measurements. Z.Z. and Fe.L. performed partial product analysis of electrochemical measurements. Y.S. performed the XPS measurements and data analysis. All authors contributed to the discussions. Y.Z. wrote the paper with inputs from the other authors, and

Fu.L., Fe.L., and L.S. revised the manuscript. All authors reviewed the paper. Fu.L. supervised the research.

Competing interests

The authors declare no competing interests.

Additional information

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