ORIGINAL ARTICLE



Gel-emulsions prepared using a low-molecular-weight gelator and their use in the synthesis of porous polymers

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Abstract

Water-in-oil (W/O) gel-emulsions consisting of water and a monomer were successfully prepared using *N*-3-hydroxypropylcarbonyl-L-isoleucyl-aminooctadecane as a gelator. Low-temperature polymerization of the gel-emulsions with a redox initiator was performed to obtain the corresponding porous polymers. Furthermore, polymerization of gelemulsions containing bifunctional monomers gave crosslinked porous PMMA-HDODA, PMMA-EGDMA, PMMA-DVB, and PSt-DVB, which were found to be mechanically robust and solvent resistant. The microstructures of the porous polymers toward methanol, dichloromethane, acetone, tetrahydrofuran, toluene, hexane, and kerosene were assessed and rationalized in terms of the surface microstructures of the polymers. The time courses of the adsorptions were investigated, revealing a two-step adsorption process comprising rapid permeation into the cavities of the porous polymers followed by a slow swelling step. The high water-repellency of the crosslinked porous polymers was confirmed by contact angle measurement. The reusabilities of the polymers as solvent absorbents were evaluated through repeated adsorption and drying.

Introduction

Recent years have seen increased research interest in lowmolecular-weight gelators that can physically gel liquids such as water and organic solvents. They are particularly attractive because large volumes of liquid can be immobilized through self-assembly using very small amounts of the gelator. Consequently, advances in the area of supramolecular chemistry have led to a number of studies on gelators being published in recent years [1–20]. Low-molecularweight gelators have unique characteristics, including good solubility upon heating and the ability to induce the smooth gelation of liquids. Gelators are characterized by thermally reversible sol-gel transitions because the three-dimensional

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Kenji Hanabusa hanaken@shinshu-u.ac.jp network structures responsible for gelation are built up through noncovalent interactions such as hydrogen bonding, electrostatic interactions, van der Waals interactions, and $\pi - \pi$ interactions. Although gelators are already used as hardeners for cooking oils, cosmetic materials, and thickeners for paint, recent gelator research has focused on their application in fields such as drug delivery and drug release in biomaterials [21-27], scaffold materials for cells in tissue engineering [28, 29], sensors [30-34], templates for the synthesis of inorganic nanostructures [35-39], auxiliary agents for producing organic electronics [12, 40], electrolytes that prevent liquid leakage [41], and detectors for explosives [42-45]. Furthermore, porous materials receive considerable research attention owing to their wide applicability in areas such as adsorption [46, 47], gas storage and separation [48–54], tissue engineering [55–59], drug delivery [60], and catalyst immobilization [61–65].

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Several studies on the preparation of porous polymers using emulsions have been reported. For example, Tokuyama et al. succeeded in preparing porous poly(Nisopropylacrylamide) using oil-in-water (O/W) emulsions stabilized by polyethylene glycol (PEG)-type surfactants [66, 67], Zhou et al. prepared porous polystyrene materials using O/W emulsions stabilized by amphiphilic carbonaceous microspheres [68], and Jiang et al. reported the preparation of poly(styrene-divinylbenzene) foam from highinternal-phase emulsions (HIPEs) stabilized by Span 80 [69]. Fang et al.'s work on gel-emulsions formed by lowmolecular-weight gelators and their use in the preparation of porous polymers is particularly interesting. They reported the preparation of porous polymers via the gelation of emulsions containing a cholesteryl derivative of diethanolamine [47] and a polymerizable cholesteryl derivative [70] as low-molecular-weight gelators. However, to the best of our knowledge, Fang's work is the only example of the use of low-molecular-weight gelators to prepare gel-emulsions and their subsequent polymerization.

Over the last two decades, we have developed many lowmolecular-weight gelators and studied their applications [8, 37–41, 44, 71]. Herein, we report the preparation of gelemulsions using a novel low-molecular-weight L-valinederivative gelator. The successful preparation of porous polymers by the radical polymerization of gel-emulsions and their application as oil absorbents were also investigated.

Experimental

Instrumentation

Elemental analysis was performed with a Perkin-Elmer 240B analyzer. Infrared spectra were recorded on a Jasco FTIR-7300 spectrometer using KBr plate. ¹H NMR spectra were recorded on a Bruker AVANCE 400 spectrometer. Scanning electron microscopy (SEM) was done with a Hitachi SU1510. The stirring for preparation of gelemulsion was performed with an AS ONE Test Tube Mixer HM-2F. Contact angle was measured by a Kyowa Interface Science DMs-400 Contact Angle Meter. Fluorescence microscopy was performed with an Olympus FV10-ASW.

Reagents

Methyl methacrylate (MMA), styrene (St), and γ butyrolactone were purchased from Wako Pure Chemical Industries, Ltd. Benzoyl peroxide (BPO), divinylbenzene (DVB), 1,6-hexanediol diacrylate (HDODA), ethylene glycol dimethacrylate (EGDMA), 3-ferrocenoylpropionic acid (3-Fepa), and sorbitan monostearate (Span 60) were purchased from Tokyo Chemical Industry Co., Ltd.

Synthesis of *N*-3-hydroxypropylcarbonyl-L-isoleucylaminooctadecane

N-Carbobenzyloxy-L-isoleucylaminooctadecane [41] (51.68 g, 0.10 mol) was hydrogenated in the presence of Pd-C in 500 mL of 1-propanol for 5 h at room temperature under a hydrogen atmosphere. After confirming the complete removal of protecting group by TLC (chloroform: methanol: acetic acid = 95:5:1 as volume ratio), the solution was filtered off. The filtrate was evaporated and recrystallized from 300 mL of ligroin to provide 35.3 g (92%) of L-isoleucylaminooctadecane. A mixture of 6.50 g (17 mmol) of L-isoleucyl-aminooctadecane and 1.46 g (17 mmol) of y-butyrolactone in 60 mL of dry THF was refluxed overnight under an argon atmosphere. After evaporating, the crude product was recrystallized from 50 mL of ethyl acetate. N-3-hydroxypropylcarbonyl-L-isoleucylaminooctadecane was obtained in a yield of 5.1 g (64%). The product was recrystallized again from methanol for elemental analyses. IR (KBr, cm⁻¹): 3380 (vOH), 3301 (νNH), 1639 (νC=O amide I), 1552 (δN-H amide II). Found: C 72.11, H 11.79, N 6.15%. Calcd for C₂₈H₅₆N₂O₃: C 71.74, H 12.04, N 5.98%. ¹H-NMR (400 MHz, CDCl₃, TMS, 25 °C): $\delta = 0.86-0.97$ (m, 9H, CH₃), 1.25 (br, 32H, alkyl), 1.49-2.06 (m, 6H, CONHCH₂CH₂ HOCH₂CH₂, CH₂CONH), 2.33–2.45 (m, 1H, CH(CH₃)(CH₂CH₃)), 3.14-3.33 (m, 2H, CONHCH₂), 3.67-3.72 (m, 2H, HOCH₂), 4.20 (t, J = 8.10, 1H, CONHCHCONH), 6.00 (t, J = 5.24, 1H, CONHCH₂), 6.43 (d, J = 8.84, 1H, CONHCH).

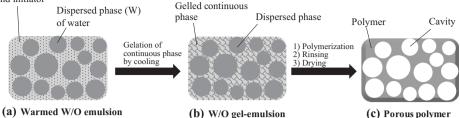
Preparation of gel-emulsion

Gel-emulsions were prepared as follows: A mixture of the weighed gelator, monomer, and Span 60 in a test tube was heated until the solid dissolved. A predetermined amount of water was added to the resulting solution and stirred vigorously by a test tube mixer. After standing at 25 °C for 2 h, the formation of gel-emulsion was checked visually. When no fluid ran down the wall of the test tube upon inversion of the test tube, we judged it to be gel-emulsion.

Polymerization of gel-emulsion

A mixture of the weighed gelator, monomer, Span 60, and 3-Fepa in a test tube was heated until the solid dissolved. A predetermined amount of water was added to the solution and

stirred vigorously at room temperature to form a gelemulsion. BPO was added to the gel-emulsion while stirring **Fig. 1** Concept of preparation of porous polymers from gelemulsion. (Color figure online) Continuous phase (O) consisting of monomer, gelator, surfactant, and initiator Dispersed phase (W)



and then left to stand at 40 °C overnight. Polymerized matter was taken out by breaking the test tube and washed with methanol to remove unreacted monomer, gelator, Span 60, and 3-Fepa.

Organic liquid adsorption test

To estimate the maximum adsorption capacity of the porous polymer, a porous polymer with known weight was placed in a beaker filled with a liquid. After 30 min of adsorption, the wet porous polymer was drained for 5 min until no residual droplets were left on the surface. The adsorption capacity was calculated by the following formula. The *q* is the adsorption capacity (mL g⁻¹), m_s is the weight of the wet porous polymer after 5 min of drainage (g), m_0 is the initial weight of the porous polymer (g), and *d* is the density of the liquid.

Results and discussion

Porous polymers

Figure 1 illustrates the concept of preparation of porous polymers from gel-emulsions. Figure 1a shows a warmed W/O emulsion in which "W" indicates the dispersed water phase and "O" indicates the continuous oily monomer phase, which contains the gelator, surfactant, and initiator. Gentle heating is necessary to dissolve the gelator in the continuous phase. Figure 1b illustrates a gel-emulsion formed upon cooling the warmed W/O emulsion to room temperature, in which the continuous phase "O" is gelled by the gelator. Low-temperature redox polymerization proceeds in the gelled continuous phase of the gel-emulsion to form a polymerized gel-emulsion. Figure 1c illustrates the porous polymer after removing the gelator, Span 60, and 3-Fepa by rinsing. The dispersed water phase shown in Fig. 1b imparts cavities to the porous polymer, as shown in Fig. 1c. Thus, porous polymers prepared from gelemulsions with high aqueous phase fractions (APFs) possess many cavities and exhibit low density.

The preparation of a porous polymer is illustrated in Fig. 2. The process consists of the following four steps: (1) the formation of an isotropic solution containing the gelator, Span 60, 3-Fepa, and monomer upon heating; (2) the addition of water; (3) stirring and the addition of the benzoyl peroxide (BPO) initiator followed by standing at 40 °C overnight; and (4) rinsing the polymer with methanol.

In this study, N-3-hydroxypropylcarbonyl-L-isoleucylaminooctadecane and Span 60 were used as the gelator and surfactant, respectively (Fig. 2). Both gelator and surfactant are indispensable in the preparation of stable gel-emulsions, with the surfactant being responsible for emulsification and the gelator being responsible for gelation of the emulsion. The gel-emulsions formed were so stable that no separation or collapse occurred, even after several months. The gelator is insoluble in water. Therefore, only the oily monomer layer in the emulsion undergoes gelation. The minimum gelator concentrations required to form gels at 25 °C from typical liquids are 40 g L^{-1} for methyl methacrylate (MMA), 10 g L^{-1} for styrene (St), 4 g L^{-1} for dodecane, 30 $g L^{-1}$ for toluene, 20 g L^{-1} for dimethyl sulfoxide (DMSO), 10 g L^{-1} for propylene carbonate, 10 g L^{-1} for isopropyl myristate, 4 g L^{-1} for silicone oil, and 4 g L^{-1} for ethylene glycol. The compositions of gel-emulsions with APFs of 90, 85, and 80 vol% are summarized in Table 1. BPO and 3-Fepa were added to these emulsions as redox initiators for low-temperature polymerization. The addition of a small amount of the gelator and Span 60, ca. 4.2 wt% against the monomer, was sufficient to form gel-emulsions. The gelemulsions were composed of water and MMA (or St), and the oil phase was gelled by the gelator. The gel-emulsions formed were confirmed to be W/O-type by fluorescence microscopy images (Fig. S1) using bis(hexadecyloxy) fluorescein [71], which dyes the oil phase orange.

Figure 3 shows the SEM images of the porous PMMA obtained via polymerization of the gel-emulsions with the compositions shown in Table 1. It should be noted that the gelator, Span 60, and 3-Fepa were completely removed from the polymers upon rinsing with methanol, as evidenced by the complete absence of ν C=O stretching vibrations for the gelator (1640 cm⁻¹), Span 60 (1738 cm⁻¹), and 3-Fepa (1714 cm⁻¹) from the FT-IR spectra of the

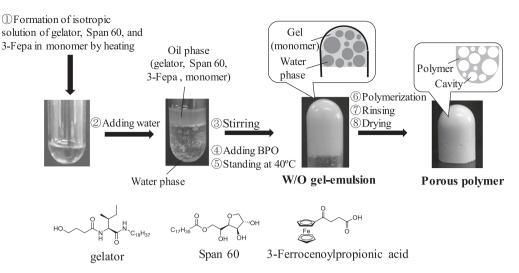


Fig. 2 Preparation process of porous polymer. (Color figure online)

Table 1 Compositions of gel-emulsions for preparation of porous PMMAs

APFs (vol-%)	Water (ml)	MMA (ml)	Gelator (mg)	Span 60 (mg)	3-Fepa (mg)	BPO (mg)
90	3.6	0.4	16	16	1.7	1.5
85	3.4	0.6	24	24	2.6	2.2
80	3.2	0.8	32	32	3.4	3.0

APFs aqueous phase fractions, MMA methyl methacrylate, Span 60 sorbitan monostearate, 3-Fepa 3-ferrocenoylpropionic acid, BPO benzoyl peroxide

porous polystyrene (PSt) samples after rinsing (see Fig. S2 for porous PMMA' IR spectrum). It is clear from the images in Fig. 3 that the porous PMMAs comprise spherical structures whose diameters are several tens of micrometers and that their walls are brittle and partially broken. The spherical structures have internal cavities, and the densities of the porous PMMAs were 0.19 g cm^{-3} (APF 80 vol%), 0.14 g cm^{-3} (APF 85 vol%), and 0.11 g cm^{-3} (APF 90 vol %). The adsorption capacities of the porous PMMA materials toward kerosene increase with increasing APF. The adsorption capacities after 30 min are 1.4 mL g⁻¹ (APF 80 vol%), 2.7 mL g^{-1} (APF 85 vol%), and 4.0 mL g^{-1} (APF 90 vol%). The adsorption capacities of PMMA (APF 90 vol %) toward methanol, toluene, and hexane are 11.6, 5.76, and 3.51 mL g^{-1} , respectively. However, all of the porous PMMAs dissolve in dichloromethane, acetone, and THF within 30 min.

Crosslinked porous PMMAs

In order to improve the solvent resistances of the porous PMMAs, we attempted crosslinking using bifunctional

vinyl monomers. The compositions of the gel-emulsions used for the preparation of crosslinked porous PMMAs are given in Table 2, where the amounts of 1,6-hexanediol diacrylate (HDODA), ethylene glycol dimethylacrylate (EGDMA), and divinylbenzene (DVB) are 0.2 molar equivalents with respect to MMA.

Figure 4 shows the SEM images of the crosslinked porous PMMA-HDODA obtained by polymerization of gel-emulsions containing HDODA. The spherical diameters of the crosslinked porous PMMA-HDODA particles are several tens of micrometers, and they increase with increasing APF. Because the gel-emulsions are of the W/Otype, a high APF results in the formation of large spherical structures. The spherical structures seem robust and independent compared to those shown in Fig. 3. Indeed, crosslinked porous PMMA-HDODA does not collapse under finger pressure, unlike the porous PMMAs. The densities of PMMA-HDODA, PMMA-EGDMA, and PMMA-DVB prepared at an APF of 90 vol% are 0.11, 0.092, and 0.078 g cm⁻³, respectively. The adsorption capacities of PMMA-HDODA toward kerosene are 0.4 mL g^{-1} (APF 80 vol%), 1.1 mL g^{-1} (APF 85 vol%), and 2.8 mL g^{-1} (APF 90 vol%). Although crosslinking by HDODA decreases adsorption capacity as compared to those of the porous PMMAs, they successfully absorb dichloromethane, acetone, and THF owing to their solvent resistances (Fig. 5). Thus, although solvent resistance and mechanical strength can be improved by crosslinking, the spherical structures are so robust that they possibly do not absorb solvents on the inside.

To study the effects of the crosslinking agents on adsorption capacity, we substituted HDODA with EGDMA or DVB (Table 2). Figure 6 shows the SEM images of crosslinked porous PMMA-HDODA, PMMA-EGDMA,

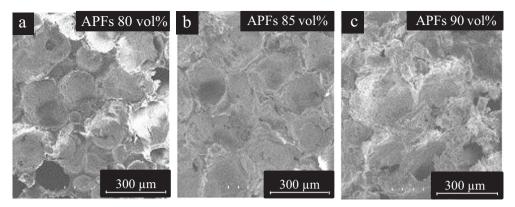


Fig. 3 SEM images of the porous composite monoliths produced by using the gel emulsion. **a** APFs 80 vol%—water/MMA. **b** APFs 85 vol%—water/MMA. **c** APFs 90 vol%—water/MMA. APFs aqueous phase fractions

Table 2 Compositions of gel-emulsions for preparation of crosslinked porous PMMAs

APFs (vol-%)	Water (ml)	MMA (ml)	Crosslinking agent (ml)	Gelator (mg)	Span 60 (mg)	3-Fepa (mg)	BPO (mg)
90	3.6	0.333	0.067 (HDODA)	16	16	1.7	1.5
85	3.4	0.50	0.10 (HDODA)	24	24	2.6	2.2
80	3.2	0.67	0.13 (HDODA)	32	32	3.4	3.0
90	3.6	0.333	0.067 (EGDMA)	16	16	1.7	1.5
90	3.6	0.333	0.067 (DVB)	16	16	1.7	1.5

HDODA 1,6-hexanediol diacrylate, EGDMA ethylene glycol dimethacrylate, DVB divinylbenzene

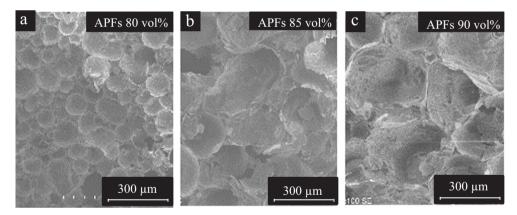


Fig. 4 SEM images of the porous composite monoliths produced by using the gel emulsion. **a** APFs 80 vol%—water/MMA and HDODA. **b** APFs 85 vol%—water/MMA and HDODA. **c** APFs 90 vol%—water/MMA and HDODA

and PMMA–DVB. The image of PMMA–EGDMA is very similar to that of PMMA–HDODA in that the size of the spherical structures is several tens of micrometers and their walls are independent and robust. In contrast, the spherical surfaces of the PMMA–DVB particles are characterized by many cracks. The adsorption capacities of PMMA–HDODA, PMMA–EGDMA, and PMMA–DVB toward methanol, dichloromethane, acetone, THF, toluene, hexane, and kerosene are shown in Fig. 7. The order of

adsorption capacities is PMMA–DVB > PMMA–HDODA > PMMA–EGDMA. The high adsorption capacity of PMMA–DVB may be attributed to the cracks in the spherical surfaces. The formation of cracks is unclear at this time, but they will be formed by shrinking associated with the polymerization.

The time courses of the adsorption of kerosene (Fig. 8a) and toluene (Fig. 8b) were obtained. The adsorption capacities after 5 s kerosene adsorption are 0.64 mL g^{-1}

(PMMA-HDODA), 1.6 mL g^{-1} (PMMA-EGDMA), and $4.3 \,\mathrm{mL}\,\mathrm{g}^{-1}$ (PMMA-DVB). indicates This that PMMA-HDODA, PMMA-EGDMA, and PMMA-DVB absorb kerosene almost instantly. In the case of toluene (Fig. 8b), the adsorption capacities after 5 s are 1.3 mL g^{-1} (PMMA-HDODA), 0.93 mL g^{-1} (PMMA-EGDMA), and 2.0 mL g^{-1} (PMMA–DVB). When the immersion time is extended, the adsorption capacities drastically increase. The large adsorption capacities upon extended immersion are due to the swelling effect. The volume of PMMA-HDODA after 3 days of adsorption is 1.9 times its original volume. The results shown in Fig. 8 indicate that the adsorption of solvents proceeds via two steps: rapid permeation into the cavities of the porous polymers and a subsequent slow swelling, which is a characteristic of crosslinked polymers. The swelling aspects of crosslinked PMMAs before and after adsorbing kerosene and toluene are shown in Figs. S3 and S4.

Crosslinked porous PSt

We also prepared crosslinked porous polymers using St instead of MMA. The compositions of the gel-emulsions for

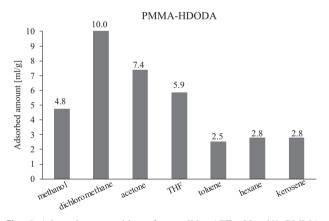


Fig. 5 Adsorption capacities of monolith. APFs $90\,\mathrm{vol}\%$ PMMA-HDODA

APFs of 90, 85, and 80 vol% are similar to those in Table 2, except for the monomer. Figure 9 shows the SEM images of crosslinked porous PSt-DVB obtained from polymerization of the gel-emulsions. The spherical structures in PSt-DVB are smaller than those in the crosslinked porous PMMAs, and many holes are observed on their surfaces. The densities of PSt–DVB are 0.19 g cm^{-3} (APF 80 vol%), 0.14 g cm^{-3} (APF 85 vol%), and 0.078 g cm⁻³ (APF 90 vol%). The adsorption capacities of PSt-DVB toward kerosene after 30 min are 2.8 mL g^{-1} (APF 80 vol%), 4.1 mL g^{-1} (APF 85 vol%), and 10.0 mL g^{-1} (APF 90 vol%). Figure 10 shows the adsorption capacities of PSt-DVB (APF 90 vol %) toward methanol, dichloromethane, acetone, THF, toluene, hexane, and kerosene. In all solvents, the adsorption capacities are higher compared with those of PMMA-DVB (cf. Fig. 5). When PSt-DVB (APF 90 vol%) is immersed in kerosene for 5 s, the adsorption capacity is 8.8 mL g^{-1} , which is two times that of PMMA–DVB (Fig. S5). The rapid adsorption by PSt-DVB is thought to be due to the high porosity ($d = 0.078 \text{ g cm}^{-3}$) and the small spherical structures with many holes. It is thought that contact zones between the dispersed water phase in the gelemulsion remained as holes on polymer surface.

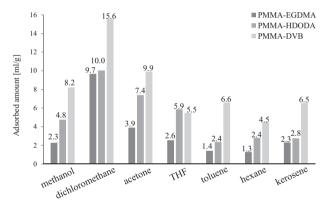
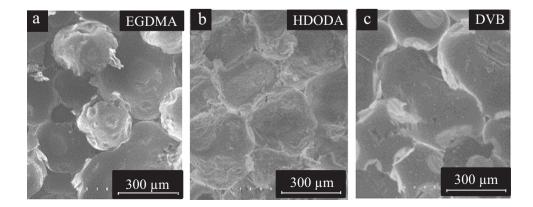
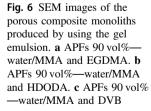


Fig. 7 Adsorption capacities of the monolith. APFs 90 vol% PMMA-EGDMA, APFs 90 vol% PMMA-HDODA, APFs 90 vol% PMMA-DVB. APFs aqueous phase fractions





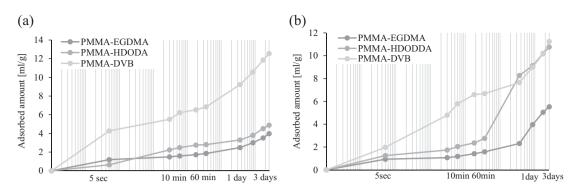
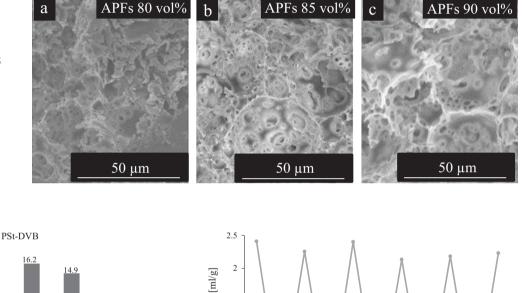


Fig. 8 a Adsorption capacity of the materials to kerosene as function of time. b Adsorption capacity of the materials to toluene as function of time

Fig. 9 SEM images of the porous composite monoliths produced by using the gel emulsion. **a** APFs 80 vol% water/St and DVB. **b** APFs 85 vol%—water/St and DVB. **c** APFs 90 vol%—water/St and DVB



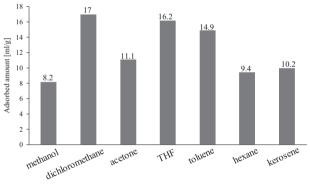


Fig. 10 Adsorption capacities of the monolith. APFs $90\,\mathrm{vol}\%$ PSt-DVB

Water-repellency and absorbent reusability

The water contact angles of the crosslinked porous polymers were measured to investigate their water-repellencies. The contact angles of PMMA–HDODA, PSt–DVB, and PMMA–DVB (APF 90 vol%) are 117.3°, 125.4°, and 117.0°, respectively (Fig. S6), confirming their high waterrepellencies, which are most likely due to the unevenness of their surfaces. The high water-repellencies allow these

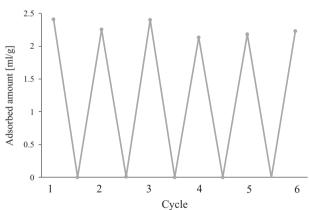


Fig. 11 Reversibility of PMMA–HDODA for adsorption processes against kerosene. APFs 90 vol%

crosslinked porous polymers to recover oils from water easily.

The reusability of PMMA–HDODA as a kerosene absorbent was evaluated by repeated adsorption and drying cycles. As shown in Fig. 11, the adsorption/recovery cycle can be repeated several times with very little impact on capacity (see Fig. S7 for reversibility of adsorption processes of porous PMMA).

Conclusion

W/O-type gel-emulsions consisting of water and a monomer were prepared using *N*-3-hydroxypropylcarbonyl-L-isoleucylaminooctadecane as a gelator and Span 60 as a surfactant. Low-temperature polymerization of the gel-emulsions with a redox initiator gave the corresponding porous polymers with low densities. The porous PMMAs have spherical structures with internal cavities, and their walls are brittle and partially broken. The adsorption capacities of the porous PMMAs toward kerosene increase with increasing APF.

Robust crosslinked porous PMMAs showing solvent resistance were obtained by the polymerization of gelemulsions containing bifunctional monomers. The crossporous PMMA-HDODA adsorbs linked methanol. dichloromethane, acetone, THF, toluene, hexane, and ker-The walls of the spherical structures osene. in PMMA-HDODA and PMMA-EGDMA are independent and robust. In contrast, the spherical surfaces in PMMA-DVB contain many cracks. The adsorption capacities are in the order PMMA-DVB > PMMA-HDODA > PMMA-EGDMA. The time courses of the adsorption by the crosslinked porous PMMAs revealed that the adsorption of solvents proceeds through two steps: rapid permeation into the cavities of porous polymers and a subsequent slow swelling, which is a characteristic of crosslinked polymers.

The spherical structures in crosslinked porous PSt–DVB are smaller than those in the crosslinked porous PMMAs, and many holes were observed on the surfaces of the porous PSt–DVB particles. The adsorption capacities of PSt–DVB are higher than those of PMMA–DVB.

The high water-repellencies of the crosslinked porous polymers were confirmed. The adsorption/recovery process could be repeated several times, and the processes were essentially reversible. The extreme lightness, high waterrepellency, and reusability of the crosslinked porous polymers indicate that they are especially promising as oilremoving absorbents.

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Compliance with ethical standards

Conflict of interest The authors declare that they have no conflict of interest.

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