# ARTICLE

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# Nano-encapsulation: overcoming conductivity limitations by growing MOF nanoparticles in meso-porous carbon enables high electrocatalytic performance

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# Abstract

Among the methods employed for carbon capture, the electroreduction of CO<sub>2</sub> offers both a reduction in CO<sub>2</sub> levels and the possibility of recycling it into commodity chemicals. However, the most efficient catalysts for this reaction are precious metals. To achieve cost-effective processes, other elements should be used. Transition-metal atoms coordinated with metal-organic frameworks (MOFs) exhibit high performance as electrocatalysts. However, the isolating natures of MOFs limit their utilization as electrocatalysts. In this study, we grew MOF nanoparticles inside hierarchically mesoporous carbon instead of mixing the MOFs with conductive carbon. The incorporated MOF nanoparticles showed improved properties compared with those of MOFs mixed with carbon, indicating strong electronic interactions in the composites. The encapsulated MOF nanoparticles demonstrated high electric conductivity while preserving their original crystallinity. When used as electrodes in CO<sub>2</sub> electroreduction, the MOFs exhibited a high electroactive coverage of 155 nmol cm<sup>-2</sup>. Moreover, in a CO<sub>2</sub>-saturated electrolyte, the composites exhibited excellent electrochemical performance, including a small onset potential (-0.31 V vs. RHE) and large reduction currents (-18 mA. cm<sup>-2</sup> at -1.0 V); these were considerably higher than those usually reported for MOFbased materials except in CO electroreduction. Importantly, the composite produced valuable hydrogenated commodity chemicals, including formic acid.

#### Introduction

The increasing level of the greenhouse gas  $CO_2$  in the atmosphere raises serious concerns for modern society<sup>1,2</sup>. Long-running measurements have shown a steady increase in the mean atmospheric  $CO_2$  concentration of 35% in the last 60 years (e.g., the famous Keeling curve)<sup>3</sup>. Decreasing the  $CO_2$  concentration in the atmosphere has become a critical challenge for sustainable development and decoupling economic growth and  $CO_2$  emissions.

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 $\rm CO_2$  conversion into valuable chemicals offers the smallest ecological footprint at the highest resource utilization level<sup>4</sup>. The electrochemical carbon dioxide reduction reaction (CO<sub>2</sub>RR) is attractive in terms of cost, availability, reaction conditions, and product separation feasibility<sup>5,6</sup>. Importantly, the electrocatalytic reactions may result in different products, depending on many factors, including the catalyst, the solution, the applied potential, and time. Generally, at moderately negative potentials (up to -0.8 V vs. SHE), the predominant product is CO<sup>7</sup>. Therefore, lower onset potentials are required to generate more valuable products.

Many metals have been tested as cathode materials in electrocatalytic processes. Both experiments and theory

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have proved that Cu is the only effective pure metal catalyst that effectively forms products beyond CO, namely, hydrocarbons and  $alcohols^{8,9}$ . The relatively weak energy for binding of CO to Cu allows the formation of the highly reduced carbon products. On the other hand, the copper shows adverse performance in terms of Faradaic efficiency (F.E., i.e., the ratio of charge utilized for the desired reaction out of total charge consumed in the system). In addition, Cu electrodes tend to generate wide ranges of reaction products with low selectivities<sup>10</sup>. In aqueous solutions, electrochemical recycling of CO<sub>2</sub> faces another challenge. The redox potentials for CO<sub>2</sub> reduction are similar to those of the hydrogen evolution reaction in aqueous solutions. Therefore, good selectivity of a CO<sub>2</sub> reduction catalyst is essential for achieving a highly efficient system.

Metal-organic frameworks (MOFs) have shown high compatibility and effectiveness in different applications in recent decades. MOFs are hybrid materials containing three well-differentiated sites to which catalytic functions can be allocated, namely, the metal component (d-band center), the organic linker (for example, cyanides (C-N)), and the pore space<sup>11,12</sup>. MOFs exhibit excellent suitability as candidates for adsorption<sup>13</sup>, separation<sup>14</sup>, and reduction during catalyzed reactions<sup>15,16</sup>. Their combined advantageous properties, i.e., large surface area, high porosity, and tunable pore size, provide promising results in electrocatalysis<sup>7,17</sup>. In this regard, the advanced performance characteristics include smaller onset potentials<sup>18</sup>, stability<sup>19</sup>, and high Faradaic efficiency<sup>20,21</sup>.

Although MOFs have many dominant advantages for the CO<sub>2</sub>RR, they suffer from low intrinsic conductivity. Considerable effort has been devoted to improving the electrical conductivity of the material, with only limited success. Recent advanced techniques such as laser graphitization improved the material properties<sup>22,23</sup>. The structural integrity of graphene was improved by patching carbon dots with laser irradiation to form 3D graphene with enhanced electrical conductivity<sup>24,25</sup>. In approaching this challenge, researchers turned to pyrolyzing (also called carbonizing) MOFs to obtain metal atoms embedded in a conductive lattice<sup>19,26–28</sup>. However, carbonized MOFs lack the unique electronic structure that supports catalytic capacity, thus severely diminishing the advantages of MOFs<sup>2,18,29</sup>. To overcome this obstacle, MOF powders are commonly mixed with carbon black, micron-sized grained graphite particles, to enhance the overall conductivity of the electrode. Embedding carbon materials with nonconductive active materials is a known technique for improving conductivity<sup>30,31</sup>. Nevertheless, this does not improve the intrinsic conductivity or performance.

A few years ago, research performed in our laboratory led to a MOF/carbon composite in which MOF nanoparticles were grown inside the pores of porous carbon. These composites demonstrated excellent conductivity and improved electrical response without impairing the structural and chemical properties of the MOFs<sup>32</sup>. Cu-MOF-based catalysts have great potential for the electrochemical recycling of  $CO_2$  into commodity chemicals because of their improved selectivities and high CO binding energies. The compositions of these MOFs with conductive and porous carbons may enhance their electric conductivities and solvent accessibilities, improve their stabilities, decrease onset potentials, and increase material loading.

## **Results and discussion**

To demonstrate the advantages of supporting MOFs on a carbonaceous scaffold, we prepared HKUST-1 nanoparticles inside a porous activated carbon. HKUST-1 is a well-known Cu-based MOF material constructed of dimeric metal units connected by benzene-1,3,5-tricarboxylic acid (BTC) linkers. The MOF/carbon composite was prepared according to the method described previously<sup>32</sup>. The precursors of the MOF, namely, copper chloride and BTC, were separately introduced into the nanopores of activated carbon by continuously stirring the activated carbon particles in a BTC solution and then a copper chloride solution. A subsequent hydrothermal reaction resulted in the MOF nanoparticles (Fig. 1).

X-ray diffraction (XRD) was employed to characterize the crystal structure of the composite (Fig. 2a). Notably, the carbon matrix did not shield the XRD signals of the encapsulated MOFs. Moreover, HKUST-1 is known for its morphological sensitivity to synthetic conditions;<sup>33</sup> however, the porous carbon composition did not adversely affect the MOF crystallinity. The XRD pattern of the composite perfectly matched the pattern for MOFs synthesized from the carbon and also contained a broad peak centered at ~25°, corresponding to the (002) planes of graphitic segments in the carbon. At the proper MOF/ carbon ratio of 1:3 (w/w), almost all of the MOFs were located inside the carbon pores, as indicated by SEM (Fig. S1). Due to the strong interactions of the MOF organic components with the aromatic rings of the host carbon, the originally nonconductive MOFs developed excellent lateral conductivity (up to 17.4 S/m) constituting an 85fold increase compared to 0.2 S/m of the precursor HKUST-1 (Table 1). A simple mixture of the MOFs and carbon in the same mass ratio led to an 8.4-fold conductance improvement (1.69 S/m). Importantly, the composite maintained an extremely high surface area (940  $\text{m}^2 \text{g}^{-1}$ ). The surface area and pore size distribution of the composite are due to the combination of the two materials as a result of partial blockage of the mesopores of the activated carbon host by the MOF nanoparticles. Additionally, the sizes of the nanoparticles perfectly matched the sizes of the pores in which they were grown.





# Table 1 Lateral electrical conductivities of HKUST-1/ carbon composites with different MOF/carbon ratios, which indicate the significant advantages of our composition method compared to simple mixing of the MOFs with carbon.

Sample #	HKUST-1 content in sample	Composited with carbon (S $m^{-1}$ )	Mixed with carbon (S m <sup>-1</sup> )	
1	Carbon	65	65	
2	16%	17.2	1.69	
3	23%	7.6	0.95	
4	37%	0.2	0.09	
5	HKUST-1	0.0003	0.0003	

A large and accessible surface area is of great importance for electrochemical reactions, since it enables good accessibility of the reacting compounds (Fig. 2b; for isotherms, see Fig. S2).

Thermal gravimetric analysis (TGA, Fig. S3) demonstrated the strong physical interactions between the MOFs and the carbon. The excellent adhesion of the MOFs on the carbon scaffold increased its thermal stability. Unmodified HKUST-1 lost approximately half of its original mass at ~400° C, whereas this loss was obtained at a 50° C higher temperature when it was incorporated into the carbon. Furthermore, the electronic interactions between the MOFs and carbon were previously identified by electron paramagnetic resonance (EPR) spectroscopy. The g-value of the unpaired Cu<sup>2+</sup> electron in the composite was lower than that of the bare HKUST-1 (Fig. S4).



This shift toward the free-electron value (g-value of 2.0023) indicated that the  $Cu^{2+}$  unpaired electron in the composite had gained a higher level of mobility (less localized to the Cu atoms). A higher level of freedom for electrons originating from the metal center proved the conductivity of the surrounding carbon. The changes in electronic structure imposed by the composite structure may have affected the catalytic properties of HKUST-1, including the yields, onset potentials and catalytic mechanisms, resulting in various products. Moreover, by analyzing the different g-values recorded for the composite, we simulated the average size of the MOF nanoparticles (considering a HKUST-1 unit cell with a diameter of 0.9 nm). Interestingly, the mean diameter of the MOF nanoparticles was 6 nm and perfectly matched the average pore size of the carbon host, as determined by gas adsorption measurements (Fig. 2b)<sup>32</sup>.

X-ray photoelectron spectroscopy (XPS) provided additional insight into the electronic state of the modified MOFs. XPS analyzes the binding energies of valance electrons in atoms and is therefore sensitive to the oxidation states of the elements. The full survey spectra, including peaks for C 1 s, O 1 s, and Cu 2p binding energies, are presented in Fig. S5. The spectrum for the activated carbon indicated 96% carbon and no detectable copper (Table S1). On the other hand, the spectra of the MOFs indicated 68.4% carbon, 29.8% oxygen, and 2.3% copper, similar to the atomic ratio in HKUST-1. Predictably, the spectrum of the composite was a combination of those for its two precursors. It contained onequarter of the Cu compared to the MOFs, which was in good agreement with the MOF/carbon ratio in the composition. The spectra were normalized with the C 1 s peak at 284.8 eV. Deconvolution of the C 1 s peak revealed the chemical interactions between atoms. The C 1 s spectrum of the activated carbon indicated mainly carbon-carbon bonding (79%). On the other hand, the MOF spectrum showed 60% oxygen-bonded carbon atoms, indicative of the carboxyl groups of the BTC linkers (Fig. 3a and Table S2). Interestingly, the binding energies of the corresponding peaks shifted in each spectrum. While the binding energy of the C-O peak in HKUST-1 was 287.3 eV, the binding energy of the composite was shifted toward a higher binding energy of 288.27 eV. This was closer to the peak found for the activated carbon at 288.65 eV. The shift of the C 1 s peak revealed a higher oxidation state for the carbon atoms in the composite compared to those in the original MOF. The deconvoluted O 1s peak followed the same trend, in which the second peak, which originated from O-C moieties, was



a potential of -0.9 V vs. RHE for 12 h. **b** LSV using the HKUST-1@AC composite as the cathode in N<sub>2</sub>- and CO<sub>2</sub>-saturated 0.5 M KHCO<sub>3</sub> electrolyte. LSV data obtained with 1 M NaCl is shown in dashed lines for comparison. **c** Chronoamperometric measurement at a constant potential of -0.9 V vs. RHE for 12 h. **d** LSV of the same composite catalyst after the first cycle and after 12 h of chronoamperometry at a constant potential.

shifted from 532.6 eV in HKUST-1 to 533.7 eV in the composite (Fig. 3b). The most significant shift was found in the Cu 2p spectrum (Fig. 3c). Importantly, this peak was absent from the spectrum for activated carbon and enables direct tracking of the changes in the electronic state of the MOFs after composition. The fitted XPS data for Cu confirmed the presence of both  $Cu^+$  and  $Cu^{2+}$ ; peaks for binding energies of 933.9 and 953.3 eV corresponded to the  $2p_{3/2}$  and  $2p_{1/2}$  states Cu(I), respectively, and the peaks at 936.2 and 956.0 eV were associated with the same electronic states for  $Cu(II)^{34-37}$ . All copper peaks were shifted to higher binding energies, which was attributed to the strong interaction between HKUST-1 and the activated carbon. Here, the peak for  $Cu^{2+}$  was upshifted from 936.2 eV in the original MOFs to 938.0 eV in the composite. The peak shifts resulted from the electronic interactions of the MOFs with the hosting carbon, and this supported the interpretations of the EPR data that were reconfirmed by the electrochemical activity. When encapsulating the MOF guest, the more oxidized activated carbon acted as an electron withdrawer and applied a partial positive charge on the MOFs, both at the chelating oxygen atoms and the copper centers. The electronic interactions ultimately led to higher electron mobility and electrical conductivity. A comparison of the atomic ratios obtained from XPS data is shown in a histogram (Fig. 3d). Further analyses of the XPS spectra can be found in the supporting information.

To evaluate the electrocatalytic capability of HKUST-1/ C, the composite was used as the cathode in a threeelectrode cell. A conductive ink comprising HKUST-1/C, carbon black (CB) as a conducting agent, and Nafion as an ion-conducting binder was prepared and drop-cast on carbon cloth electrodes. Cyclic voltammetry (CV) studies using the electrode in a CO<sub>2</sub>-saturated KHCO<sub>3</sub> solution showed a widely spaced Cu<sup>+</sup>/Cu<sup>2+</sup> oxidation/reduction couple with peaks at 0.76 and 0.45 V vs. RHE, respectively (Fig. 4a). An important parameter for high surface area composite catalysts is the degree of electroactive coverage, i.e., the number of active sites available in the material for electrochemical reactions. The CV reduction peak at -0.05 V vs. Ag/AgCl was used to measure the concentration of electroactive copper centers (Fig. S6). Integrating the reduction wave produced with a CV scan rate of 10 mV s<sup>-1</sup> revealed that 0.015 Coulombs participated in the electrochemical reaction (Fig. S6). Considering that this reaction involves only single electron transfer, approximately 155 nmol of  $Cu^{2+}$  sites were exposed to the

Cathode	<i>J</i> , mA cm <sup>-2</sup>	E V vs. SHE	Electrochemical coverage nmoles cm <sup>-2</sup>	Main product	Reference
MOF-545Fe/CB	1.2	-0.6	3	CO	49
Al <sub>2</sub> (OH) <sub>2</sub> TCCP-Co	1	-1.7	18	СО	19
COF-367-Co	3.3	-0.67	2	СО	50
MOF-1992/CB	16.6	-0.63	270	СО	29
CuPc	2.8	-1.6	N.A. <sup>c</sup>	$C_2H_4$	18
Fe-TPP	3	-1.0	0.1	СО	20
HKUST-1/carbon	18	<b>-1.0</b>	155	HCOO	This work

Table 2 Performance of different MOF-based cathodes for CO<sub>2</sub> electroreduction.

<sup>c</sup> - could not be extracted from the paper.

electrolyte solution and actively participated in the electrochemical reduction reaction. This is approximately 18% of the Cu atoms in the total electrode. The high electroactive coverage indicated exceptionally high exposure of the metal centers to the electrolyte, among the highest ever reported for MOF-based cathodes (Table 2 and Table S3).

Linear sweep voltammetry (LSV) was employed to study the cathode performance in the CO<sub>2</sub> electroreduction reaction. The selection of a proper electrolytic solution is crucial for enabling the reaction. As bicarbonate is well known to produce  $CO_2$ , a potassium bicarbonate solution was used as the electrolyte for the CO<sub>2</sub> reduction reaction as per the previous studies  $^{38-43}$ . When polarized to negative potentials, the HKUST-1/carbon composite demonstrated an exceptionally high increase in the negative current density, starting at an onset potential of -0.31 V (Fig. 4b, black line). Moreover, at -1.0 V vs. RHE, the LSV with the MOF/carbon exhibited a current density of  $-18 \text{ mA cm}^{-2}$  in the presence of CO<sub>2</sub>. This was considerably higher than the current densities usually reported for MOF-based catalysts, except with CO electrocatalysis (Table 2 and Table S3). The excellent performance resulted from the extremely high electrochemical coverage of the MOFs and the electrical activity originating from amalgamation with the carbon host. The gaseous  $CO_2$  reacted with water to form carbonic acid,  $H_2CO_3$ , which allowed the dissolution of more CO<sub>2</sub>. The resulting  $H_2CO_3$  was in equilibrium with bicarbonate  $(HCO_3^{-})$ , which in turn was in equilibrium with carbonate  $(CO_3^{2-})$ . Under our reaction conditions with a neutral pH, carbonate was protonated to form bicarbonate. Because of this, the CO<sub>2</sub>-saturated solution had more bicarbonate anions undergoing the CO<sub>2</sub> reduction process. To ensure that the cathodic current originated from CO<sub>2</sub> reduction  $(CO_2 + 2H^+ + 2e^- \rightarrow CO + H_2O)$  and not from the hydrogen evolution reaction (HER,  $2H^+ + 2e^- \rightarrow H_2$ ), the electrodes were tested in a similar apparatus with a NaCl solution used as the supporting electrolyte. In this CO<sub>2</sub>free electrolyte solution, the onset potential was shifted down to -0.52 V. Presumably, in the absence of carbonate ions, the reduction was associated with the HER, proving high selectivity for the catalyst. (Fig. 4b, blue dashed line). LSV was run at lower scan rates (2 mVs<sup>-1</sup>), and the identical results confirmed that the source of the current was Faradaic and not capacitive (Fig. S7). These excellent results resulted from the unique chemical structure of the composite material. To prove the superiority of the composite, we tested all of the individual components electrochemically. Fig. S8a shows the LSV results for the HKUST-1 MOF, activated carbon, and a copper salt loaded on activated carbon. Both the currents and the overpotentials observed for the nanocomposite outperformed those observed for all of the separate components. EIS measurements showed the smaller resistivity of the composite compared to that of every individual component (Fig. S8b and Table S4).

The stability of the catalyst during prolonged operation is a major challenge in electrocatalytic processes<sup>28</sup>. To evaluate the stability of electrocatalysis, we applied a constant potential (E = -0.9 V vs. RHE) to a MOF/carbon composite electrode in a CO<sub>2</sub>-saturated solution (Fig. 4c). An average current density of -10.56 mA cm<sup>-2</sup> was measured at the initial stage of the reaction, and -11.85 mA cm<sup>-2</sup> was measured after 12 h. The sustained current density indicated excellent chemical stability. The remarkable stability should be attributed to the stability of the carbon host. Durability was also tested with repeated LSV and CV experiments after 12 h of chronoamperometry (Fig. 4a, d). Both measurements revealed almost identical responses for the fresh electrodes and the electrodes held at constant potential for 12 h. We also tested the stability of the electrode at acidic and basic pHs (3, 6 and 12), and Fig. S9 shows comparisons of chronoamperometry measurements lasting 12 h with galvanostatic measurements in normal bicarbonate solution (pH 8.25). The reduction currents in the acidic solutions were similar, and those in the basic solution (pH =12) were significantly lower. Prolonged stability tests prove the excellent stabilities of the composite electrodes over a large range of pH values. XRD measurements were performed before and after the chronoamperometry tests (Fig. S10). The results showed that the MOF/carbon composite retained its stable structure. These results were promising and encourage further studies of the activities and selectivities of MOF/carbon composites used as catalysts for the  $CO_2RR$ .

To make CO<sub>2</sub> reduction economically feasible, the products of the process must be valuable chemicals. It is worth noting that many studies have measured CO production and calculated the Faradaic efficiency for CO production, which is not a commodity chemical. In this study, we examined the formation of more highly reduced (hydrogenated) species; therefore, the production identification required NMR spectra. To identify the products of the reaction, the electrolyte solution used for the CO<sub>2</sub>RR was collected from the reactor after 0.5 h, 2 h, 3 h, 5 h, and 10 h. The products were analyzed by H-NMR spectroscopy and quantified using maleic acid as the internal standard. Formic acid was identified as the main product via <sup>1</sup>H NMR spectrometry (Fig. 5). Importantly, products were observed even in the first sample taken after 30 min. The amount of each product varied during the 10 h of reaction. A peak at  $\delta = 8.3$  ppm was attributed to formic acid. Two additional peaks near  $\delta = 3.0$  were observed after the initial stages of the reaction. One was attributed to the central methylene (CH<sub>2</sub>) group in malonic acid,  $HOC = OCH_2C = OOH$ . We could not confirm the origin of the other peak near  $\delta = 3.0$ . We tried adding malonic



acid into the NMR tube containing the sample from CO<sub>2</sub> reduction (Fig. S11). The malonic acid showed a new peak, which indicated that the product was not malonic acid. Notably, the concentration of formic acid increased for the first three hours and decreased when the reaction continued for 12 h (Fig. S12). Interestingly, this decline in peak intensity after 3 h of reaction implied a second electrochemical reaction involved reduction of this initial product. It should be noted that when products were left in the reactor cell and subjected to low potentials, more highly reduced products may result;44 earlier studies showed situations where products were seemingly lost from the reaction solution, and this was exacerbated by performing the reactions at low concentrations<sup>45</sup>. Moreover, different potentials resulted in various products (Fig. 6a). The Faradaic efficiencies for formation of formic acid and hydrogen gas at different potentials at displayed in Fig. 6b. More formic acid was formed at lower potential, and less was observed with a higher potential because of competition from the hydrogen evolution reaction. This showed that CO<sub>2</sub> electroreduction predominantly occurs at a low potential at -0.3 V vs. RHE. Although CO is a common product in carbon dioxide reduction, after applying several potentials to the electrode material, we were unable to identify CO as a product of  $CO_2$  reduction. The absence of CO product was confirmed by FTIR and electrochemical CO stripping tests (Figs S13, S14). COfree product mixtures have been reported for many other studies using copper in electrocatalytic reductions<sup>46–48</sup>.

Based on the products identified by NMR, we can propose a reduction mechanism that results in formic acid as the main product. This mechanism is based on multiple recent publications describing the use of a similar copper-based catalyst and formation of similar products<sup>20,44,45</sup>. A plausible mechanism for the HKUST-1/C composite is shown in Fig. 7. In the initial reaction stages, the CO<sub>2</sub> contained in the electrolyte is adsorbed on the copper center and, under a negative potential, it is reduced to the CO<sub>2</sub>.<sup>-</sup> radical ion at the HKUST-1/Csurface. The adsorbed CO<sub>2</sub>.- binds at the active sites on the catalyst surface and reacts with a proton to form a carboxyl radical (COOH) intermediate, which results in the formation of formic acid.

#### Conclusions

This work shows the high efficiency of a composite produced from the well-studied MOF HKUST-1 and activated carbon as an electrocatalyst for  $CO_2$  electroreduction. To enable the use of MOFs in electrochemical applications, conductivity must first be established in naturally occurring materials. To achieve this conductivity, HKUST-1 nanoparticles were grown inside a conductive porous carbon. The strong interactions originating from  $\pi$ -  $\pi$  bonds between the aromatic linkers and





the graphitic carbon induced high lateral conductivity of up to  $17.2 \,\mathrm{S \,m^{-1}}$  for the composite. Moreover, an EPR study of the unpaired electrons on the Cu atoms revealed that the induced conductivity influenced the metal centers. Importantly, the conductivity achieved by the composite did not impact the crystal structure of the MOFs, as observed by XRD. Electrochemical studies revealed a high electroactive coverage of 155 nmol  $cm^{-2}$ . When operated in a CO<sub>2</sub>-saturated aqueous solution, the composite electrode exhibited excellent electrocatalytic performance. The onset potential for carbon dioxide electroreduction was -0.31 V vs. RHE, and the reduction current density at -1.0 V was -18 mA cm<sup>-2</sup>, which may be the largest reduction current density ever reported, except for CO reduction. In addition, the composite stabilized the active material, and after 12 h of constant operation, the electrochemical response showed minor changes. The main product observed via <sup>1</sup>H-NMR was formic acid. These excellent results suggested the effectiveness of the composition method in allowing nonconductive MOFs to participate in electrochemical processes.

#### **Experimental section**

# MOF/carbon composite synthesis

The synthesis of the MOF/carbon composite was described elsewhere<sup>32</sup>. The activated carbon used in this

research was obtained from Energy2, USA. HKUST-1/ carbon composites were prepared by suspending 250 mg of oven-dried activated carbon in 10 mL of a dimethylformamide (DMF) solution of H<sub>3</sub>BTC (103 mg,  $4.9 \times 10^{-4}$ mol). The suspension was stirred at room temperature for several hours. Cu(OAc)<sub>2</sub>·H<sub>2</sub>O (147 mg, 7.3 ×  $10^{-4}$  mol, 1.5 equiv. with respect to H<sub>3</sub>BTC) was added, and the mixture was stirred for another 2 h at room temperature. The mixture was held overnight in an oven at 40 °C in an autoclave. The resulting suspensions were centrifuged and decanted. Subsequently, the solid precipitate was washed with 15 mL of DMF. These washing cycles involving centrifuging and decanting were repeated three times. The resulting solid powders were suspended in acetone (5 mL) overnight and dried on a rotary evaporator. The dried samples were placed in an oven at 40 °C and gradually heated to 150 °C (1 °C/min) for approximately 4 h. The prepared composites were stored under an inert atmosphere. To compare our results with those from recent work, we also prepared HKUST-1/carbon mixtures by mixing appropriate quantities of HKUST-1 and AC. The obtained mixtures had the same HKUST-1/carbon ratios.

# Gas adsorption measurements

Gas adsorption was measured using an Autosorb-1 MP (Quantachrome) system. The specific surface area was calculated using the Brunauer–Emmett–Teller (BET) model. The MOF was activated (solvent removal) by drying under a high vacuum of  $1.5 \cdot 10^{-3}$  bar at  $150 \,^{\circ}$ C for 12 h before the surface area measurements.

## Powder X-ray diffraction (PXRD)

Spectra were recorded using a Bruker AXS D8 Advance XRD. The MOF was activated (solvent removal) by drying under a high vacuum of  $1.5 \cdot 10^{-3}$  bar at  $150 \,^{\circ}$ C for 12 h before XRD measurements.

#### X-ray photoelectron spectroscopy (XPS)

The XPS data were obtained with an (XPS/AES) ESCALAB 250 ultrahigh vacuum ( $1 \times 10^{-9}$  bar) apparatus equipped with an Al-K $\alpha$  X-ray source and a monochromator. The measured spectra were calibrated relative to the C 1 s peak at 284.6 eV. The survey spectra were analyzed with a pass energy (PE) of 150 eV, and the high energy resolution was realized with a PE of 20 eV.

## Composite electrodes for electrochemical characterization

Electrodes were prepared by mixing the composite powder (active mass – MOF/carbon) with 5% Nafion as a binder and 5% carbon black serving as a conducting agent. While encapsulation of the MOF inside the carbon improved the intrinsic conductivity of the active material, the role of the conducting agent was to improve the conductivity between particles and bridge gaps in the electrode film. The ink was coated on a carbon cloth. The average active mass weight was 1.40 mg for a 1 cm<sup>2</sup> electrode.

#### **Electrochemical measurements**

For all experiments, 0.5 M potassium bicarbonate was used as the electrolyte. Prior to electrochemical testing, the electrolyte was saturated with CO<sub>2</sub>. A standard threeelectrode setup was employed with a platinum counter electrode and a Ag/AgCl reference electrode. These experiments were carried out with potentiostat/galvanostat computerized instruments from Bio-Logic Inc, France.

*Cyclic voltammetry:* The electrolyte solution was sparged for 15 min with N<sub>2</sub> or CO<sub>2</sub>. The scan rate was 10 mV/s within the presented electrochemical potential windows. *Chronopotentiometry:* The electrolyte solution in the working compartment was sparged for 10 min with N<sub>2</sub> or CO<sub>2</sub>. The applied potential was -0.3 V vs. RHE, based on the optimal performance of the cobalt phthalocyanine catalyst at that potential. The chronoamperograms were corrected for uncompensated resistance. The current density at E = -0.3 V vs. SHE was averaged from three independent MOF-1992/CB electrodes, and the standard deviation was used as the error.

Faradaic efficiency was calculated as

$$FE = n * F * Z/A * t$$

where n = 2 for a two-electron reaction, F = 96485 C/mol, Z = number of moles of formic acid produced, A is the measured current, and t is the time.

The conductivity measurements were conducted with two copper portals distanced 1 centimeter apart and pressed on the composite film. We measured the lateral conductivity rather than the bulk conductivity since it is difficult to determine the thickness of the electrode, and cross-sectional microscope images showed that the thickness varied considerably (from  $\sim 0.8$  to 2 micrometers).

More experimental and instrumental details can be found in the supplementary information.

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K.S. and A.D.- Sample preparation, analysis and electrochemical measurements. Manuscript writing. A.F.- Model and concept development, consultation. T.Z. and R.W.- Research planning, consultation. Manuscript review. A.B.-Supervising, conceptualization.

#### Conflict of interest

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