Large-scale turbulent flow around a cylinder in counterflow superfluid ^4He (He(II))

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Published online: 29 September 2005; doi:10.1038/nphys114

The detailed nature of fluid flow over a cylinder is one of the fundamental topics in classical fluid dynamics as it demonstrates flow separation and vortex shedding¹. In superfluid helium, either He(II) or the B phase of ^3He , an important question has been to what extent these quantum fluids show classical fluid turbulent states^{2–4}. Although the existence of turbulent structures can be inferred using precise instrumentation^{5,6}, direct visualization of the flow field can provide unequivocal evidence of these phenomena. Here we show the existence of large turbulent structures in He(II) counterflow across a cylinder as obtained by the particle image velocimetry technique. Compared with classical fluid flow, the particle motion driven by He(II) counterflow shows macroscopic eddies downstream of the cylinder but also similar structures are observed in front of the cylinder, behaviour not seen in classical fluids. As Landau's two-fluid model⁷ for He(II) describes counterflow as the relative motion of the superfluid and normal fluid components, the current results indicate that both components may be undergoing a kind of flow separation as they pass over the cylinder.

Visualizing the flow of superfluid ^4He (He(II)) has long been of interest to the scientific community^{8–11}. Particle image velocimetry (PIV), a quantitative visualization technique that records the motion of micrometre-scale solid particles suspended in the fluid and uses that information to map out the flow field of a dynamic fluid¹², has been used extensively in classical fluids, but only applied in the past few years to the study of liquid helium fluid dynamics^{13,14}. This delay has at least in part been because of the challenges of particle selection and seeding into a fluid of very low temperature and low density. The entire process must occur in an optical He(II) cryostat with the visualization equipment consisting of a charge-coupled-device camera, a dual-head pulse laser, beam-expanding optics, a synchronizer for timing and triggering and a data-acquisition computer. To map the velocity field, sequential images of the suspended particles are collected and divided with a grid into a large number of 'interrogation regions', each of which provides a local velocity vector based on averaging the particle

velocities in that region. The interrogation regions typically contain ten particles and are about $1 \times 1 \text{ mm}^2$, which establishes the approximate spatial resolution of the measurement.

In the two-fluid model for He(II), the viscous normal fluid component density, ρ_n , increases with temperature T and the corresponding inviscid superfluid component density, ρ_s , decreases with T until it vanishes at the transition to He(I), just below 2.2 K. A heat current q produces a normal fluid velocity, v_n , which is given by the relationship⁷

$$q = \rho s T v_n,$$

where ρ is the total density and s is the fluid entropy. In this case, the superfluid component velocity, v_s , is in the opposite sense conserving the zero net momentum condition such that

$$v_s = -\frac{\rho_n}{\rho_s} v_n.$$

This internal convection of the two fluid components is known as thermal counterflow.

As the PIV technique maps out the velocity field of particles suspended in the fluid, it is not a trivial problem to relate the observed particle motion to the individual velocity fields of the normal and the superfluid components in He(II). Our experiments on counterflow in a one-dimensional channel have shown that, in a similar manner to classical fluids, the particle motion is approximately uniform and parallel¹⁵. However, quantitative analysis of these data has indicated that the interaction between the suspended particles and the two fluid components is more complex than one might assume, with the turbulent superfluid component also exerting a force on the particles. This observation is further supported by theoretical studies that have suggested the particle–superfluid interaction may be associated with pinning of the quantized vortex lines in the turbulent superfluid component^{16,17}.

In the present experiment, we have used the PIV technique to visualize counterflow He(II) over a circular cylinder. Counterflow is produced in a one-dimensional rectangular channel that is 200 mm long and has a cross-section of $38.9 \times 19.5 \text{ mm}^2$. The channel is immersed in a constant-temperature He(II) bath and seeded with

Figure 1 Particle seeding in a He(II) counterflow channel containing a 6.35 mm transparent cylinder. The particles are 1.7 μm diameter polymer micro-spheres¹⁴ with a specific gravity of 1.1. In the video, the He(II) is at $T = 2.03\text{ K}$ and $q = 11.2\text{ kW m}^{-2}$ is applied upwards and co-axial to the channel. This flux corresponds to a superfluid vortex line density¹⁸, L_0 , of about $2.6 \times 10^{10}\text{ m m}^{-3}$.

1.7- μm -diameter polymer particles (specific gravity = 1.1)¹⁴. The top end of the channel is open to the helium bath whereas the lower end is closed and contains a nichrome thin-film heater. On each side wall of the channel there is an optical window for the laser sheet in and out. The front wall has a $45 \times 20\text{ mm}^2$ optical window that transmits the images to the charge-coupled-device camera. A 6.35-mm-diameter transparent cylinder is located inside the channel spanning the full width and orthogonal to the fluid flow. In the widest part of the cylinder, the channel cross-section is therefore reduced to 68% of its original area.

An example of the raw data produced by these PIV experiments is shown in Fig. 1, which is an image of the suspended particles in the He(II) channel. See Supplementary Information to view a video of the particle motion at 2.03 K produced by an 11.2 kW m^{-2} steady heat current from below the cylinder. This flux corresponds to a vortex line density L_0 of about $2.6 \times 10^{10}\text{ m m}^{-3}$ and an average line spacing of about 6.2 μm ; ref. 18. In the video, one can easily resolve large convective cells behind the cylinder at the approximate angles of 45 and 135°. These cells are roughly of the same diameter as the cylinder and seem to maintain stable locations over the 10 s duration of the video. In addition, convective cells are also seen in front of the cylinder, at about 225 and 315°. These cells are of similar size but seem to be slightly closer to the channel walls. For comparison, in classical flow over a cylinder the streamlines in front of the cylinder are smooth and large vortices are only observed behind the cylinder. Thus, these vortices in front of the cylinder have no classical analogue.

It should be pointed out that large-scale vortex rings in He(II) were reported while measuring the velocity profile in a He(II) counterflow jet using the laser Doppler velocimetry technique^{10,11}. However, it is believed that the large vortex structures were probably caused by an experimental artefact that resulted in cavitation in the counterflow jet rather than, as in our experiments, the complex interaction between the two fluid components.

Figure 2 Measured particle velocity field (v_{mean}) around the 6.35 mm outer diameter cylinder in counterflow He(II). **a**, $q = 4\text{ kW m}^{-2}$ at $T = 1.6\text{ K}$ corresponding to $\text{Re}_D = 41,000$ and $L_0 = 1 \times 10^{10}\text{ m m}^{-3}$. **b**, $q = 11.2\text{ kW m}^{-2}$ at $T = 2.03\text{ K}$ corresponding to $\text{Re}_D = 21,000$ and $L_0 = 2.6 \times 10^{10}\text{ m m}^{-3}$. The velocity scale at the top is calibrated in pixels ms^{-1} (1 pixel $\text{ms}^{-1} = 22\text{ mm s}^{-1}$).

Two examples of the computed velocity vectors for counterflow across a cylinder obtained from the analysed PIV data are shown in Fig. 2. The coloured contour represents the particle velocity magnitude with the velocity scale indicated at the top of each figure and in the figure caption. Velocity streamlines for the same two cases are shown in Fig. 3. Comparing these two figures, one can clearly see a higher level of turbulence for Fig. 3b than for Fig. 3a.

By analogy to classical fluids, one might expect the scale of the turbulence to increase with Reynolds number, in this case defined in terms of the normal fluid velocity and viscosity, μ_n , as

$$\text{Re}_D = \frac{\rho v_n D}{\mu_n}, \quad (1)$$

where D is the diameter of the cylinder. Note that equation (1) uses the total density rather than the normal fluid density, a form normally used to correlate frictional pressure drop in He(II) flow in

Figure 3 Computed streamlines for particle motion for the two heat flux cases in Fig. 2. **a**, $q = 4 \text{ kW m}^{-2}$ at $T = 1.6 \text{ K}$ corresponding to $\text{Re}_D = 41,000$ and $L_0 = 1 \times 10^{10} \text{ m m}^{-3}$. **b**, $q = 11.2 \text{ kW m}^{-2}$ at $T = 2.03 \text{ K}$ corresponding to $\text{Re}_D = 21,000$ and $L_0 = 2.6 \times 10^{10} \text{ m m}^{-3}$.

tubes¹⁹ and over bluff bodies²⁰. However, computing the Reynolds number for the two cases in Figs 2 and 3 gives $\text{Re}_D \sim 41,000$ for Fig. 2a and $\text{Re}_D \sim 21,000$ for Fig. 2b, which is a value lower by about a factor of two even though it shows more turbulence than Fig. 2a. This suggests that the Reynolds number as defined in equation (1) may not be the appropriate parameter to describe the scale of the turbulence in counterflow He(II). In other experiments not shown here, we have attempted to match the Reynolds numbers at different temperatures and heat currents; however, in all cases, the level of turbulence is greater at higher temperatures.

Furthermore, it is worth noting that for classical fluids at $\text{Re}_D > 10,000$ considerably different flow structures are normally present downstream of a cylinder. In particular, the large-scale vortices behind the cylinder show vortex shedding, where the structures are generated periodically and detach from the cylinder producing a dynamic wake. Such time-dependent phenomena in classical fluids result in pressure fluctuations that are not present in He(II) counterflow in wide channels. In fact, the vortex structures present in these counterflow He(II) experiments show behaviour

that is qualitatively similar to the steady wakes seen in classical flow over a cylinder at low Reynolds number, $\text{Re}_D < 50$ (ref. 21).

Finally, as can be seen in Fig. 3, the location of the large vortices in front of the cylinder seems closer to the channel wall than do those downstream of the cylinder. This asymmetry of particle motion may be further evidence that the normal fluid component interacts more strongly with the particles than does the turbulent superfluid component. As the particle motion in front of the cylinder should be determined by both the counterflowing superfluid component and the normal fluid component, which has a significant horizontal velocity component, one would expect the normal fluid to move the vortex in front of the cylinder farther away from it. Apart from these qualitative observations of particle motion during counterflow around a cylinder and its explanation in terms of interactions with both the superfluid and normal fluid component, we have no theoretical justification for these results at present. This is an area of current research.

It remains to be seen how the present results can help us understand the flow of heat currents in counterflow He(II) around bluff bodies. This topic is of significant interest to scientists and engineers who use He(II) to cool large technical devices such as superconducting magnets and particle physics accelerators. The design of such devices is frequently based on extensions of the two-fluid model and its application in complex geometries. By visualizing counterflow around a cylinder, we show that the corresponding heat current may have more complex behaviour than one might assume.

Received 1 July 2005; accepted 16 August 2005; published 29 September 2005.

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Acknowledgements

This work was supported in part by the National Science Foundation, Division of Chemical Transport Systems and by the Department of Energy, Division of High Energy Physics. The authors would like to thank L. Lourenco, S. Fuzier and S. Maier for assistance in performing these experiments. Correspondence and requests for materials should be addressed to S.W.V.S. Supplementary Information accompanies this paper on www.nature.com/naturephysics.

Competing financial interests

The authors declare that they have no competing financial interests.

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