Thermodynamics of Polymer–Polymer–Solvent and Block Copolymer–Solvent Systems II. Theoretical Treatment of Data with the Nonrandom New Flory Theory

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ABSTRACT: Experimental data previously reported¹ are treated with the nonrandom new Flory theory of polymer solutions. The theory is applied to polymer–polymer–solvent systems and extended to the block copolymer–solvent case. Polymer–polymer binary interaction parameters are determined. Equations for χ interaction parameters are identical in form for the polymer–solvent, polymer–solvent and block copolymer–solvent case. The ability of the theory to fit the experimental data is satisfactory.

KEY WORDS Polymer Mixtures / Block Copolymers / New Flory Theory / Nonrandom Mixing /

Most of the reported polymer pairs^{2,3} showing an appreciable degree of compatibility are by no means simple nonpolar molecules. Specific interactions imply a certain degree of nonrandomness in molecular arrangements in the mixture, although they are not, probably, the only cause for nonrandom arrangements in liquids and their mixtures. Orientational order has been observed even in *n*-alkane liquids.⁴ The need for corrections for nonrandomness was suspected several times in the past⁵⁻⁷ partly as a cause of discrepancies between theoretical and experimental results.

In this work, we treat the experimental data reported previously¹ with the equation of state theory of Flory and coworkers⁸ corrected for nonrandomness. The correction for nonrandomness follows closely the lines of our previous work.^{7,9} Working equations are presented for ternary systems and the theory is extended to include the solvent–block copolymer case. The new Flory theory⁸ has been

chosen because of its simplicity and the fact that the pure component equation of state parameters are frequently available in the literature.

POLYMER-POLYMER-SOLVENT CASE

The configurational partition function (the other factors of the partition function are of no concern to us here) in its maximum term approximation may be written as^{8,9}

$$Q_{\rm N} = g_{\rm c} g_{\rm NR} \psi^{\rm N} \exp\left(-E_0/RT\right) \tag{1}$$

where g_c is the combinatorial contribution accounting for the number of distinguishable random arrangements of the molecules in the system; $g_{\rm NR}$ is a correction to g_c for nonrandom arrangements. ψ is the "cell" partition function or otherwise the "free volume" contribution of each of the N molecules; E_0 is the mean intermolecular (attractive) energy of the system; R, gas constant and T, the

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temperature.

For simplicity, we keep for g_c the approximation of Flory¹⁰ for a system of N_1 monomers, \dots , $N_i r_i$ -mers, namely

$$g_{c} = \frac{(rN)!}{\prod_{i} N_{i}!} \left(\frac{Z-1}{rN}\right)^{N(r-1)}$$
(2)

where

$$rN = \sum_{i} N_{i} r_{i} \tag{3}$$

and

$$N = \sum_{i} N_i \tag{4}$$

The quasi-lattice coordination number Z has been arbitrarily set equal to ten.

For the free volume term, we assume

$$\psi = [\gamma v^* (\tilde{v}^{1/3} - 1)^3]^{rc} \tag{5}$$

with

$$rc = \sum \phi_i r_i c_i \tag{6}$$

 $3r_ic_i$ are the equivalent number of external degrees of freedom per r_i -mer in the Prigogine¹¹ sense.

If N_{ij} is the total number of i-j contact pairs in the system then, in the van der Waalstype energy interaction form the intermolecular energy of the system may be written as

$$-E_0 = \sum_{j \ge i} \frac{N_{ij} \varepsilon_{ij}}{v} \tag{7}$$

where ε_{ij} is an interactional constant characteristic of pair *i*-*j*.

The quasi-chemical¹² correction for nonrandomness may be written as:

$$g_{\mathbf{NR}} = \frac{\prod_{i}^{N} N_{ii}^{0}! \prod_{j \ge i} \left[\frac{N_{ij}^{0}}{2}! \right]^{2}}{\sum_{i}^{N} N_{ii}! \prod_{j \ge i} \left[\frac{N_{ij}}{2}! \right]^{2}}$$
(8)

where superscript $_0$ indicates random values of N_{ii} 's.

The segment fraction is defined as

$$\phi_i = \frac{N_i r_i}{\sum_j N_j r_j} \tag{9}$$

For an r_i -mer it is assumed that the number of intermolecular contacts in which molecule *i* participates is given by¹²

$$Zq_i = (Z-2)r_i + 2$$
 (10)

The surface fraction θ_i is given by

$$\theta_i = \frac{N_i Z q_i}{N Z q} \tag{11}$$

where

$$NZq = \sum_{i} N_i Zq_i \tag{12}$$

Due to nonrandom arrangements, the local surface fractions θ_{ij} are different from the overall surface fractions given by eq 11. Thus, the total number of *i*-*i* contacts is approximated as

$$N_{ii} = \frac{N_i Z q_i}{2} \theta_{ii} \tag{13}$$

and, similarly, for *i*-*j* contacts

$$N_{ij} = N_i Z q_i \theta_{ji} = N_j Z q_j \theta_{ij} \tag{14}$$

 θ_{ii} is the fraction of nearest neighbors of type *i* around a central segment of type *i* and θ_{ij} is the fraction of nearest neighbors of type *i* around a central segment of type *j*. The factor 1/2 in eq 13 is necessary in order to account for the symmetry of the arrangement *i*-*i*. In terms of nonrandom factors, the above local surface fractions may be written as

$$\theta_{ii} = \theta_i \Gamma_{ii} \tag{15a}$$

$$\theta_{ii} = \theta_i \Gamma_{ii} \tag{15b}$$

$$\theta_{ii} = \theta_i \Gamma_{ii} \tag{15c}$$

In contrast to θ_{ij} 's the nonrandom factors Γ_{ii} 's have no directional character ($\Gamma_{ii} = \Gamma_{ii}$).

Following Guggenheim's quasi-chemical treatment,¹² the values of the N_{ij} 's $(i \neq j)$ are those that minimize the free energy of the system, leading to the quasi-chemical

Thermodynamics of Polymer-Solvent Systems II.

conditions9

$$\frac{\theta_{ii}\theta_{jj}}{\theta_{ij}\theta_{ji}} = \exp\frac{\varepsilon_{ii} + \varepsilon_{jj} - 2\varepsilon_{ij}}{vRT} = G_{ij} \qquad (16)$$

In the case of ternary systems, there are three quasi-chemical conditions, eq 16. In terms of local surface area fractions, the energy term $-E_0$ may be written for the ternary case as:

$$-E_{0} = \frac{Nrv^{*}}{v} (\phi_{1}P_{1}^{*} + \phi_{2}P_{2}^{*} + \phi_{3}P_{3}^{*} - \phi_{1}\theta_{21}X_{12} - \phi_{2}\theta_{32}X_{23} - \phi_{3}\theta_{13}X_{31})$$
(17)

where

$$P_i^* = \frac{Zq_i}{2r_i} \frac{\varepsilon_{ii}}{v^{*2}} \tag{18}$$

and

$$X_{ij} = \frac{Zq_i}{2r_i} \frac{\varepsilon_{ii} + \varepsilon_{jj} - 2\varepsilon_{ij}}{v^{*2}} \quad (i \neq j)$$
(19)

The characteristic pressure, P^* , of the system is then given by

$$P^* = \phi_1 P_1^* + \phi_2 P_2^* + \phi_3 P_3^* - \phi_1 \theta_{21} X_{12} - \phi_2 \theta_{32} X_{23} - \phi_3 \theta_{13} X_{31}$$
(20)

while the characteristic temperature T^* is obtained from the relation

$$P^*v^* = cRT^* \tag{21}$$

Each of the three nonrandom factors Γ_{ij} $(i \neq j)$ is given by a relation of the form

 $\Gamma_{ij} =$

$$\frac{2(1-2\lambda\theta_t)}{(1-2\theta_t) + [(1-2\theta_t)^2 - 4(1-G_{ij})\theta_i\theta_j(1-2\lambda\theta_t)]^{1/2}} (i \neq j \neq t)$$
(22)

Details for the computation of the Γ_{ij} 's have been given previously.⁹

With the above definitions, the equation of state in terms of reduced variables has the form⁸

$$\frac{\tilde{P}\tilde{v}}{\tilde{T}} = \frac{\tilde{v}^{1/3}}{\tilde{v}^{1/3} - 1} - \frac{1}{\tilde{v}\tilde{T}}$$
(23)

where

$$\tilde{P} = \frac{P}{P^*} \tag{24}$$

and

$$\tilde{T} = \frac{T}{T^*} \tag{25}$$

The chemical potential is obtained from

$$\mu_1 = \left(\frac{\partial \ln Q_N}{\partial N_1}\right)_{T,V,N_{j\neq 1}} \tag{26}$$

The activity a_1 of component 1 is then given by:

$$\ln a_{1} = \frac{\mu_{1} - \mu_{1}^{0}}{RT}$$

$$= \ln \phi_{1} + \left(1 - \frac{r_{1}}{r_{2}}\right) \phi_{2} + \left(1 - \frac{r_{1}}{r_{3}}\right) \phi_{3}$$

$$+ \frac{P_{1} * r_{1} v^{*}}{RT} \left[3\tilde{T}_{1} \ln \frac{\tilde{v}_{1}^{1/3} - 1}{\tilde{v}^{1/3} - 1} + \left(\frac{1}{\tilde{v}_{1}} - \frac{1}{\tilde{v}}\right)\right] + \frac{Zq_{1}}{2} \ln \Gamma_{11} \qquad (27)$$

Comparison of eq 27 with eq 8 of ref 1 gives for the $\chi_{1,23}$ parameters with $\phi_{23} = \phi_2 + \phi_3$

$$\chi_{1,23} = \frac{1}{\phi_{23}^2} \left\{ \frac{Zq_1}{2} \ln \Gamma_{11} + \frac{P_1 * r_1 v^*}{RT} \times \left[3\tilde{T}_1 \ln \frac{\tilde{v}_1^{1/3} - 1}{\tilde{v}^{1/3} - 1} + \left(\frac{1}{\tilde{v}_1} - \frac{1}{\tilde{v}} \right) \right] \right\}$$
(28)

In the random case (zeroth approximation) the first term in eq 28 should be replaced by

$$\frac{v^{*}}{\tilde{v}RT\phi_{23}^{2}} \left(r_{1}X_{12}\theta_{2}(1-\theta_{1}) + r_{1}X_{13}\theta_{3}(1-\theta_{1}) - \frac{Zq_{1}}{Zq_{2}}r_{2}X_{23}\theta_{2}\theta_{3} \right)$$

Equation 28 is valid for binaries as well.9

The treatment of polymer–polymer–solvent systems with the above formulation involves the following three steps:

—Determination of the X_{12} parameter from data on the Flory–Huggins χ_{12} interaction

Durant	P^*	T* K 4709	$\frac{v_{\rm sp}^*}{\rm cm^3g^{-1}}$ 0.8860	Refer- ence
Pure component	atm			
Benzene (25°C)	6194			
Benzene (58°C)	6054	4829	0.8948	14
Polystyrene	5395	7420	0.8100	15
Poly(vinyl methyl ether)	5390	7201	0.8284	16
<i>n</i> -Pentane	4010	4158	1.1828	17
Polyisobutylene	4418	7580	0.9493	17
n-Heptadecane	4418	5760	1.063	8
Chloroform	6274	4450	0.5124	7
Poly(vinyl chloride)	8645	7960	0.6240	18
Poly(<i>e</i> -caprolactone)	5905	6363	0.769	18
Carbon tetrachloride	5586	4700	0.487	18
Poly(ethylene oxide)	6628	6469	0.7532	14
<i>n</i> -Tetracosane	4542	6020	1.0544	8

 Table I. Equation of state parameters for pure components

parameter for the system: solvent-polymer 2.

- -Determination of the X_{13} parameter from data on the Flory-Huggins χ_{13} interaction parameter for the system: solvent-polymer 3.
- -Use of X_{12} and X_{13} for the determination of X_{23} parameter from data on $\chi_{1,23}$ parameter for the system: solvent-polymer 2-polymer 3.

The pure component equation of state parameters are presented in Table I. Although the pure component parameters may change with temperature, the limited information available does not allow to consider this effect. In Figure 1 experimental and calculated values of the $\chi_{1,23}$ parameter are presented for the system chloroform (1)-polystyrene (2)poly(vinyl methyl ether) (3) at 25°C. The density of chloroform at 25°C is¹⁹ 1.4794 $g \, cm^{-3}$. The values of X_{ij} parameters for this system are: $X_{12} = -2.27$ cal cm⁻³, $X_{13} =$ -16.19 cal cm⁻³, $X_{23} = 0.015$ cal cm⁻³. No substantial improvement has been found by introducing a second parameter with the treatment as suggested previously.9

In Figure 2, experimental and calculated

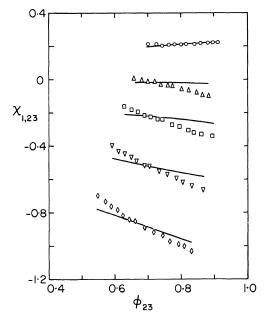


Figure 1. Experimental and calculated $\chi_{1,23}$ parameters *versus* polymer mixture segment fraction ϕ_{23} for the system chloroform (1)–polystyrene (2)–poly(vinyl methyl ether) (3) at 25°C. —, calculated; experimental points (w_{2p}) : \bigcirc , 1.0; \triangle , 0.8012; \square , 0.6023; \bigtriangledown , 0.3337; \diamondsuit , 0.0.

values of the $\chi_{1,23}$ parameter are presented for the system benzene (1)-polystyrene (2)poly(vinyl methyl ether) (3) at 25°C. The specific volume of benzene at 25°C is¹³ 1.1444 cm³g⁻¹. The values of the X_{ij} parameters for this system are: $X_{12}=0.13$ cal cm⁻³, $X_{13}=$ -1.20 cal cm⁻³, $X_{23}=0.019$ cal cm⁻³. Once again, no substantial improvement has been found by using a second parameter. The interesting result is the surprising good agreement in the X_{23} parameter obtained from data using two different probes. A minor difference in X_{23} 's arising from the different size of the two probes, as indicated by the defining eq 19, is always expected.

In Figure 3, experimental and calculated values of the $\chi_{1,23}$ parameter are presented for the system carbon tetrachloride (1)–poly(vinyl chloride) (2)–poly(ε -caprolactone) (3) at 65°C. The specific volume of carbon tetrachloride is

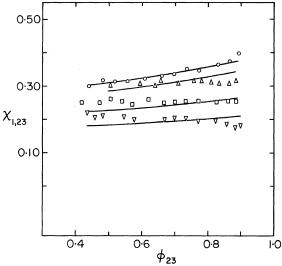


Figure 2. Experimental and calculated $\chi_{1,23}$ parameters *versus* polymer mixture segment fraction ϕ_{23} for the system benzene (1)-polystyrene (2)-poly(vinyl methyl ether) (3) at 25°C. —, calculated; experimental points (w_{2p}) : \bigcirc , 1.0; \triangle , 0.8012; \square , 0.3337; \bigtriangledown , 0.0.

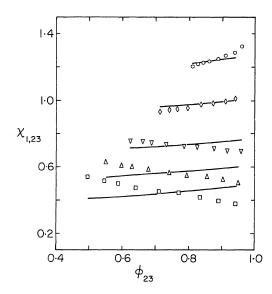


Figure 3. Experimental and calculated $\chi_{1,23}$ parameters *versus* polymer mixture segment fraction ϕ_{23} for the system carbon tetrachloride (1)–poly(vinyl chloride) (2)–poly(ε -caprolactone) (3) at 65°C. —, calculated; experimental points (w_{2p}): \bigcirc , 1.0; \diamondsuit , 0.7653; \bigtriangledown , 0.4784; \triangle , 0.2171; \Box , 0.0.

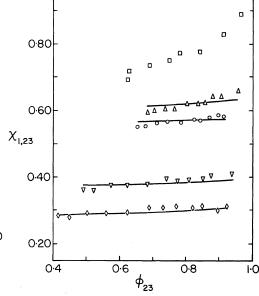


Figure 4. Experimental and calculated $\chi_{1,23}$ parameters *versus* polymer mixture segment fraction ϕ_{23} for the system *n*-pentane (1)-polyisobutylene (2)-*n*-heptadecane (3) at 25°C. —, calculated; experimental: \Box , *n*-pentane-polyisobutylene molecular weight 40000¹⁷; \triangle , *n*-pentane-polyisobutylene molecular weight 2700; \bigcirc , *n*-pentane-polyisobutylene molecular weight 1350; \bigtriangledown , *n*-pentane-polymer mixture, $w_{2p}=0.3854$; \diamondsuit , *n*-pentane-*n*-heptadecane.

taken $as^{20} 0.6639 cm^3 g^{-1}$. The values of the X_{ij} parameters for this system are $X_{12} = 7.99$ cal cm⁻³, $X_{13} = 3.32$ cal cm⁻³, $X_{23} = 1.59$ cal cm⁻³. Olabisi,²¹ from gas-liquid chromatog-raphy measurements, has calculated X_{23} at 120°C for this system to be 2.2 cal cm⁻³ (30% poly(vinyl chloride) per weight) and 3.0 cal cm⁻³ (50% poly(vinyl chloride)). In view of the difference in temperatures, the reported values in the two works may be considered in satisfactory agreement with each other.

In Figure 4, the experimental and calculated values of the $\chi_{1,23}$ parameter are presented for the system: *n*-pentane (1)–polyisobutylene (2)–*n*-heptadecane (3) at 25°C. In the same figure data on χ_{12} parameter for the system pentane–high molecular weight polyisobutylene¹⁷ are presented for the sake of comparison. The specific volume of pentane at 25°C is¹⁷ 1.6094

cm³ g⁻¹. The values of the X_{ij} parameters for this system are: $X_{12} = -0.12$ cal cm⁻³, $X_{13} =$ 0.83 cal cm⁻³, $X_{23} = -0.31$ cal cm⁻³. The calculated line for the polyisobutylene sample of molecular weight 2700 was obtained with $X_{12} = 0.49$ cal cm⁻³. Discrepancies may be expected because of possible "end effects" in this range of molecular weights.

BLOCK COPOLYMER–SOLVENT SYSTEM

In this section the nonrandom new Flory theory is extended to the case of block copolymer-solvent systems. The treatment is limited to the case of two different types of blocks containing units of types A and B. Each block may have any number of units of a single type and the larger the blocks the better the approximation of the model is likely to be.

In the following treatment subscript 1 indicates the solvent containing units S; subscript 2 indicates the block copolymer containing units A and B; subscript 3 indicates the model homopolymer containing only units A; subscript 4 indicates the model homopolymer containing only units B. r_{LM} is the number of units of type L in the molecule of type M. Thus, L may be S, A or B and M may be 1, 2, 3, or 4.

Following Flory's convention⁸ the size of each unit (segment) will be set equal to the size of the solvent. For the solvent it will be set

$$r_1 = r_{\rm S1} = 1 \tag{29}$$

with a total number of external contacts per molecule:

$$Zq_1 = Z \tag{30}$$

The total number of units in molecule 2 is

$$r_2 = r_{\rm A2} + r_{\rm B2} \tag{31}$$

With a corresponding number of external contacts

$$Zq_2 = (Z-2)r_2 + 2 \tag{32}$$

The number of external contacts in which units A of the molecule 2 are participating is

$$Zq_{A2} = (Z-2)r_{A2} + l$$
 (33)

where l=0 or 1 or 2 depending on how many times block of type A is an end block. The rest of the external contacts of molecule 2 are then

$$Zq_{B2} = Zq_2 - Zq_{A2}$$
 (34)

The fraction of contact sites A on each copolymer molecule is

$$v_{A2} = \frac{Zq_{A2}}{Zq_2}$$
(35)

and similarly for contact sites B

$$v_{\rm B2} = \frac{Zq_{\rm B2}}{Zq_2} = 1 - v_{\rm A2} \tag{36}$$

In the solvent-block copolymer system there are two types of molecular surface fractions, namely

$$\theta_1 = \frac{N_1 Z q_1}{N_1 Z q_1 + N_2 Z q_2} = \frac{N_1 Z q_1}{N Z q}$$
(37)

and

$$\theta_2 = \frac{N_2 Z q_2}{N Z q} = 1 - \theta_1 \tag{38}$$

The three types of unit surface fractions are

$$\Theta_{\rm A} = \frac{N_2 Z q_{\rm A2}}{N Z q} = \frac{N_2 Z q_2}{N Z q} v_{\rm A2} = \theta_2 v_{\rm A2} \qquad (39)$$

$$\Theta_{\rm B} = \frac{N_2 Z q_{\rm B2}}{N Z q} = \frac{N_2 Z q_2}{N Z q} v_{\rm B2} = \theta_2 v_{\rm B2} \qquad (40)$$

$$\Theta_{\rm S} = \frac{N_1 Z q_1}{N Z q} = \theta_1 = 1 - \Theta_{\rm A} - \Theta_{\rm B} \tag{41}$$

If the total number of external contact pairs L-K in the system is N_{LK} , the local unit surface fractions are defined by the relations:

$$N_{\rm AA} = \frac{NZq}{2} \,\Theta_{\rm A} \Theta_{\rm AA} \tag{42}$$

$$N_{\rm BB} = \frac{NZq}{2} \,\Theta_{\rm B} \Theta_{\rm BB} \tag{43}$$

$$N_{\rm ss} = \frac{NZq}{2} \Theta_{\rm s} \Theta_{\rm ss} \tag{44}$$

$$N_{\rm AB} = NZq\Theta_{\rm A}\Theta_{\rm BA} = NZq\Theta_{\rm B}\Theta_{\rm AB} \qquad (45)$$

$$N_{\rm AS} = NZq\Theta_{\rm A}\Theta_{\rm SA} = NZq\Theta_{\rm S}\Theta_{\rm AS} \tag{46}$$

$$N_{\rm BS} = NZq\Theta_{\rm B}\Theta_{\rm SB} = NZq\Theta_{\rm S}\Theta_{\rm BS} \tag{47}$$

From the principle of conservation of the external contacts,⁷ the above definitions lead to the following relation:

$$\sum_{\mathbf{L}} \boldsymbol{\Theta}_{\mathbf{L}\mathbf{K}} = 1 \qquad \mathbf{L}, \mathbf{K} = \mathbf{A}, \mathbf{B}, \mathbf{S} \qquad (48)$$

The nonrandom factors Γ_{LK} are defined in a manner analogous to that described in the first section. For example

$$\Theta_{AB} = \Theta_A \Gamma_{AB} \tag{49}$$

With the above nomenclature, the exponential term of the partition function may be written as:

$$-\frac{E_0}{vRT} = \frac{NZq}{2vRT} \left[\sum_{L} \Theta_L \varepsilon_{LL} - \sum_{L} \sum_{K \neq L}' \Theta_L \Theta_{KL} \varDelta \varepsilon_{LK} \right]$$
(50)

Where, in the sum \sum' each pair should be taken once, and

$$\Delta \varepsilon_{LK} = \varepsilon_{LL} + \varepsilon_{KK} - 2\varepsilon_{LK}$$
(L, K being A or B or S) (51)

The determination of the local unit fractions is done in exactly the same manner as it was done previously in the first section for the ternary case. Similarly the quasi-chemical conditions (eq 16), written in terms of local unit surface fractions, have the general form

$$\frac{\Theta_{AA}\Theta_{BB}}{\Theta_{AB}\Theta_{BA}} = \exp\frac{\Delta\varepsilon_{AB}}{vRT} = G_{AB} \qquad (16a)$$

Equation 22 is modified in a similar manner. The segment fractions are given by eq 9 for the case of two components (i=1, 2). The characteristic equation of state parameters are defined by the relations

$$P^* v^{*2} = \frac{Zq}{2r} \left(\sum_{L} \Theta_L \varepsilon_{LL} - \sum_{L} \sum_{K \neq L} \Theta_L \Theta_{KL} \varDelta \varepsilon_{LK} \right)$$
(52)

where

$$Nr = N_1 r_1 + N_2 r_2 \tag{53}$$

Again,

$$P^*v^* = cRT^* \tag{54}$$

where now

$$c = \phi_1 c_1 + \phi_2 c_2 = \phi_1 c_1 + \phi_2 \left(\frac{r_{A2} c_3 + r_{B2} c_4}{r_2} \right)$$
(55)

The inherent assumption in eq 55 is that each unit has the same value for the Prigogine c parameter,¹¹ in both the homopolymer and in the block copolymer, which is likely to be true if the blocks are long enough.

With all these definitions the equation for the χ_{12} interaction parameter takes the simple form

$$\chi_{12} = \frac{1}{\phi_2^2} \left\{ \frac{Zq_1}{2} \ln \Gamma_{\rm ss} + \frac{P_1 * r_1 v^*}{RT} \right. \\ \times \left[3\tilde{T}_1 \ln \frac{\tilde{v}_1^{1/3} - 1}{\tilde{v}^{1/3} - 1} + \left(\frac{1}{\tilde{v}_1} - \frac{1}{\tilde{v}} \right) \right] \right\}$$
(56)

which is formally identical to eq 28.

Application to the System: Benzene– α , ω -Alcoxy Poly(ethylene oxide)

Data previously reported¹ will be used to estimate the polyethylene (high *n*-alkane)– poly(ethylene oxide) interaction constant. Each unit of the end blocks $(CH_3(-CH_2)_{17})$ and $(CH_3(-CH_2)_{20})$ is assumed to behave as a similar unit in *n*-tetracosane, while each unit of the internal block is assumed to behave as a similar unit in the poly(ethylene oxide) E600M¹ sample. The reduced volume for benzene at 55°C is^{14,20} 1.3282.

From the treatment of the data on benzene (S) E600M (A) system, the following values are obtained:

$$\varepsilon_{\rm AS} = 166350 \,{\rm cal}\,{\rm cm}^{-3}$$
 and
 $X_{\rm SA} = -0.75 \,{\rm cal}\,{\rm cm}^{-3}$

Similarly, for the system benzene (S)-*n*-tetracosane (B),

$$e_{BS} = 132706 \text{ cal cm}^{-3}$$
 and
 $X_{SB} = 6.03 \text{ cal cm}^{-3}$

Using these binary parameters, the treatment of the data on benzene–block copolymer $18-45-18^1$ gives

$$\varepsilon_{AB} = 160390 \text{ cal cm}^{-3}$$
 and
 $X_{BA} = -3.84 \text{ cal cm}^{-3}$

and, similarly, for the system benzene-block copolymer 21-45-21¹

$$\varepsilon_{AB} = 160368 \text{ cal cm}^{-3}$$
 and
 $X_{BA} = -3.23 \text{ cal cm}^{-3}$

The surprisingly negative values for the X_{BA} parameter may be due to end effects. In order to test this hypothesis, each unit of the internal block has been simulated with a similar unit of the high molecular weight poly(ethylene oxide) molecule (see ref 1).

For this system, the following values have been obtained at 70° C:

$$\varepsilon_{AS} = 169134 \text{ cal cm}^{-3}$$
 and
 $X_{SA} = 0.97 \text{ cal cm}^{-3}$

Using this parameter, the system benzene–(18-45-18) gave

$$\varepsilon_{AB} = 159395 \text{ cal cm}^{-3}$$
 and
 $X_{RA} = 4.54 \text{ cal cm}^{-3}$

which seem to be more reasonable values for this type of pair interaction.

In Figure 5 experimental and calculated data are presented for the solvent-copolymer systems and the corresponding solventhomopolymer systems. In view of the several oversimplistic assumptions in this rather elementary theory, the results may be considered

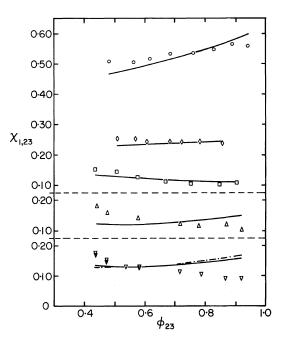


Figure 5. Experimental and calculated $\chi_{1,23}$ parameters *versus* polymer mixture segment fraction ϕ_{23} for the system benzene (1)–poly(ethylene oxide) (2)–*n*-tetracosane (3). —, calculated with parameters at 55°C; ----, calculated with benzene–poly(ethylene oxide) parameters at 70°C; experimental: \bigcirc , benzene–*n*-tetracosane at 55°C; \diamond , benzene–poly(ethylene oxide) molecular weight 100000 at 70°C; \square , benzene–poly(ethylene oxide) molecular weight 600 at 55°C; \diamond , benzene–copolymer 21-45-21 at 55°C; \bigtriangledown , benzene–copolymer 18-45-18 at 55°C.

as gratifying.

CONCLUSIONS

In this paper we have presented one of the many ways in which data on the Flory-Huggins χ interaction parameters for ternary systems may be treated with the new Flory theory. To our knowledge this is the first attempt to treat this type of data (nonzero solvent concentration) with an equation of state approach. The introduction of the $\chi_{1,23}$ parameter leads to a uniform treatment of ternary data for polymer solutions. Extension of the treatment to more than three components is straightforward. In this work only

x

γ

θ

λ

μ

 θ_{ij}

one binary parameter (ε_{ij}) has been used for fitting the data, although previous experience⁷ has shown that just one parameter may not be enough for treating data on other thermodynamic functions of mixing such as heats of mixing and/or volumes of mixing. Due to the lack of more complete information, the binary parameters were determined using only data on χ interaction parameters. Since this information may not be enough to give unique values of the binary parameters, the values of the parameters obtained in this work should be considered with caution. As for the fit of the data, before a final judgement is passed on the validity of the theory, the approximate nature of the pure component equation of state parameters of Table I should be considered, since variations of these parameters with temperature and molecular weight for oligomers and polymers have not been taken into account in this work. Probably one of the merits of this simple approach is its generality. More data and better pure component parameters are necessary to give a more definite judgement on the validity of the approach.

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NOTATION

a_1	=	activity of component 1 (solvent)
E_0	=	mean intermolecular potential energy
G_{ij}	=	binary constant defined by eq 16
g_{c}	=	random combinatorial term
$g_{\rm NR}$	=	nonrandom combinatorial factor
1	=	number indicating how many times a particular
		block is an end block
N	=	number of moles
N_{ij}	=	total number of external contacts of type <i>i-j</i>
Р	=	pressure
$Q_{\rm N}$	===	configurational partition function
R	=	gas constant
r	=	number of segments per molecule
3rc	=	equivalent number of translational degrees of
		freedom per molecule
Т	=	temperature (K)

= volume per segment v

weight fraction of component 2 in the polymer w_{2p} mixture

= mole fraction

 X_{ii} = binary parameter defined by eq 19

Ζ = lattice coordination number

Zq= number of external contacts per molecule

Greek Letters

Г = nonrandom quasichemical factor

= geometric factor in the cell partition function

= property difference ٨

= interaction energy parameter for contact of type ε_{ij} i−j

Θ = unit surface fraction

- = local unit surface fraction for units of type L Θ_{LK} around units of type K
 - = molecular surface fraction
 - = local molecular surface fraction for molecule of type *i* around molecule of type *j*
 - = nonrandom auxiliary parameter
 - = chemical potential
- μ_1^0 = chemical potential of pure component 1
- = fraction of unit contacts of type L in a molecule V_{LM} of type M
- = segment fraction of component *i* ϕ_i

= Flory-Huggins interaction parameter χij

= quantity defined in ref 1 χ1,23

Superscripts

= reducing quantities

= reduced quantities

0 = random values

Subscripts

= quantity pertaining to component *i*

- L = quantity pertaining to unit L
- LM = quantity pertaining to unit L in component M

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