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# Mesoporous carbon originated from non-permanent porous MOFs for gas storage and CO<sub>2</sub>/CH<sub>4</sub> separation

SUBJECT AREAS:

METAL-ORGANIC  
FRAMEWORKS

SYNTHESIS AND PROCESSING

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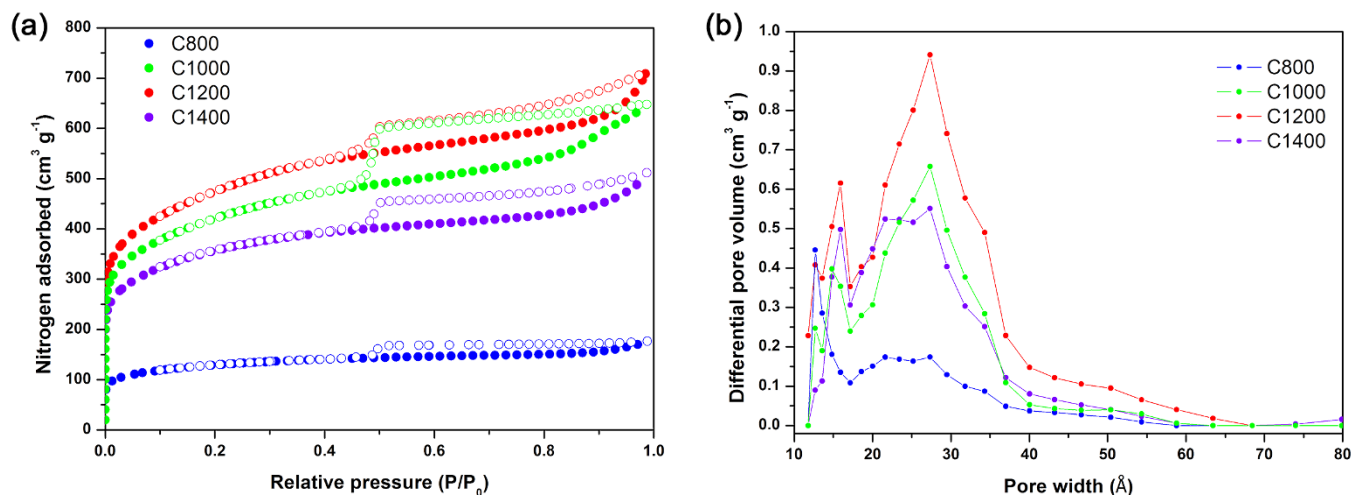
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27 June 2014Published  
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Four nanoporous carbons prepared by direct carbonization of non-permanent highly porous MOF [Zn<sub>3</sub>(BTC)<sub>2</sub>·(H<sub>2</sub>O)<sub>3</sub>]<sub>n</sub> without any additional carbon precursors. The carbonization temperature plays an important role in the pore structures of the resultant carbons. The Brunauer-Emmett-Teller (BET) surface areas of four carbon materials vary from 464 to 1671 m<sup>2</sup> g<sup>-1</sup> for different carbonization temperature. All the four carbon materials showed a mesoporous structure centered at ca. 3 nm, high surface area and good physicochemical stability. Hydrogen, methane and carbon dioxide sorption measurements indicated that the C1000 has good gas uptake capabilities. The excess H<sub>2</sub> uptake at 77 K and 17.9 bar can reach 32.9 mg g<sup>-1</sup> and the total uptake is high to 45 mg g<sup>-1</sup>. Meanwhile, at 95 bar, the total CH<sub>4</sub> uptake can reach as high as 208 mg g<sup>-1</sup>. Moreover the ideal adsorbed solution theory (IAST) prediction exhibited exceptionally high adsorption selectivity for CO<sub>2</sub>/CH<sub>4</sub> in an equimolar mixture at 298 K and 1 bar (*S*<sub>ads</sub> = 27) which is significantly higher than that of some porous materials in the similar condition.

Nanoporous carbon materials have gained much attention owing to their high surface area, narrow pore size distribution, and good thermal and chemical stability. These characteristics allow porous carbon can be utilized for a variety of applications such as adsorbents, catalyst supports, electrode materials, and so on<sup>1-6</sup>. Several synthetic methods were explored to prepare highly porous carbons and control their pore structures, including pyrolysis followed by physical or chemical activation of organic precursors, carbonization of polymeric aerogels, template synthetic procedures, chemical vapor deposition (CVD), and laser ablation<sup>1-14</sup>. Using zeolites and mesoporous silicas such traditional inorganic materials as a template, ordered microporous and mesoporous carbons have been successfully prepared in recent years by the nanocasting technique<sup>4,5,15,16</sup>. The pore structures of carbons obtained by nanocasting with template approach can be further tuned by physical or chemical activation, although it is slightly complex to remove the template and unsuited for mass production.

On the other hand, metal-organic frameworks (MOFs) or porous coordination polymers (PCPs), which are newly emerging porous materials with multiple functionalities, have attracted much attention mainly because of their high surface area, tunable porosity, and wide potential applications in gas storage, separation, catalysis, and sensing<sup>17-20</sup>. Porous MOFs are usually thermally robust and have various pore sizes suitable for small molecules to access. Therefore, they have been considered as templates to construct nanoporous carbon materials. Xu et al. used the MOFs as templates for synthesis of nanoporous carbon materials for the first time<sup>21</sup>. Under the atmosphere of furfuryl alcohol (FA) vapor, they have successfully introduced FA into the micropores of MOF-5 followed by polymerization and carbonization to prepare nanoporous carbons. Since then, some related works were published in succession<sup>22-27</sup>. Recently, some other groups also have reported that nanoporous carbon can be obtained by a simpler method-direct carbonization of MOFs without any additional carbon precursors<sup>28-34</sup>. Though such reported carbon materials have broad pore size distributions and the carbonization condition was not clearly understood, this approach has worked pretty well for preparing porous carbons. The current MOFs template used for porous carbon usually has permanent porosities. However, many MOFs only have an apparent porosity which frameworks may be ruined in the activation process, and how to use these pore structures in MOFs with non-permanent porosities are always a challenge. Recent studies show that even nonporous Zn-based MOFs could also be applied to prepare highly porous carbons, which opens up the way for the use of nonporous MOFs<sup>32,35</sup>. For example, [Zn<sub>3</sub>(BTC)<sub>2</sub>·(H<sub>2</sub>O)<sub>3</sub>]<sub>n</sub> is isostructure with HKUST-1 [Cu<sub>3</sub>(BTC)<sub>2</sub>·(H<sub>2</sub>O)<sub>3</sub>]<sub>n</sub> which is one of the most famous MOFs<sup>36</sup>. Though [Zn<sub>3</sub>(BTC)<sub>2</sub>·(H<sub>2</sub>O)<sub>3</sub>]<sub>n</sub> is also highly porous from the point of crystallography, the framework will collapse during activation. Here, we reported using



**Figure 1** | (a)  $N_2$  adsorption-desorption isotherms at 77 K; (b) pore size distributions of all carbon samples.

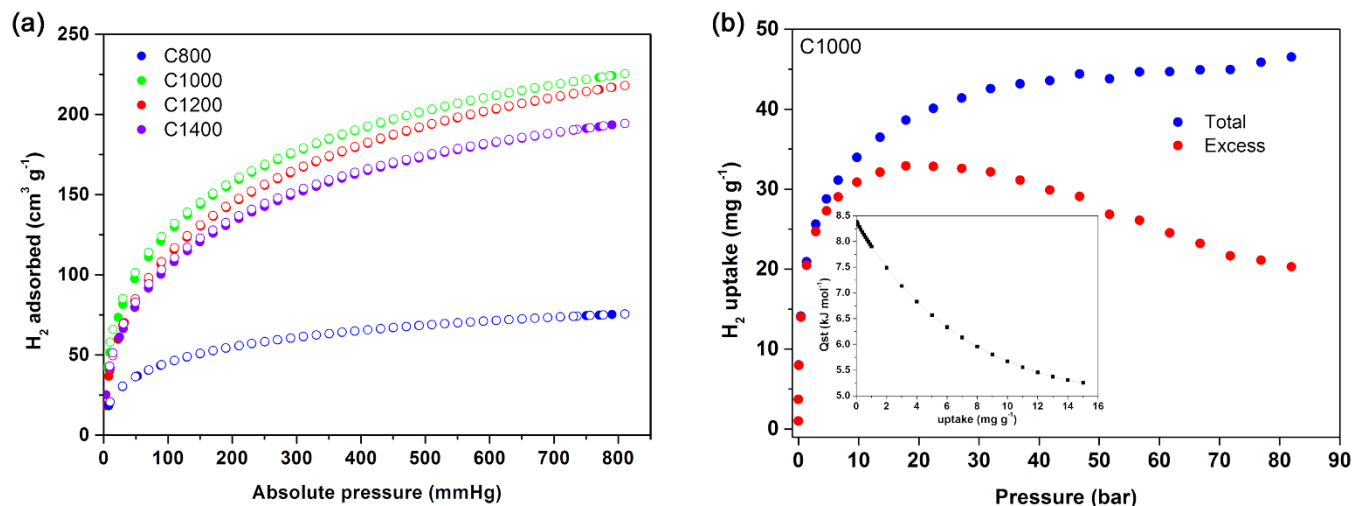
direct-method carbonization to transform non-permanent highly porous MOF  $[Zn_3(BTC)_2 \cdot (H_2O)_3]_n$  into stable nanoporous carbons with high surface areas. These carbon materials exhibited a large gas storage capacity and exceptionally high adsorption selectivity for  $CO_2/CH_4$ . We carefully investigated the structure of the porous carbons, the effect of the carbonization temperature on its gas adsorption properties.

## Results

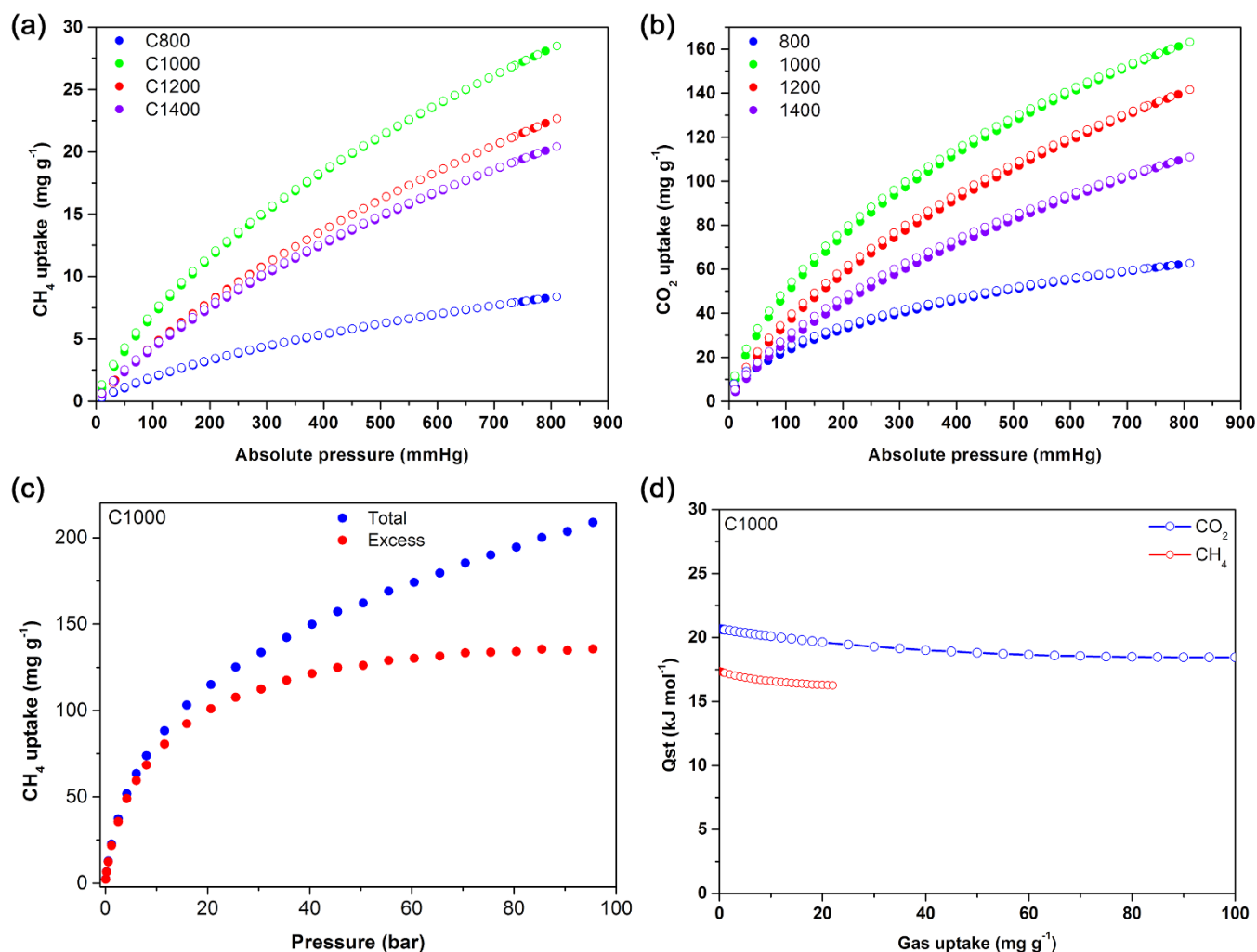
The presence of nanopores in the obtained samples was confirmed by nitrogen adsorption-desorption measurements (Figure 1a). Nitrogen isotherms were also carried out to evaluate the specific surface areas and pore-size distribution of the C800, C1000, C1200 and C1400 samples. The general shape of the  $N_2$  sorption isotherms for four samples indicates the existence of different pore sizes varying from micropores to mesopores. At low relative pressure area ( $P/P_0 < 0.1$ ), the curves showed a drastic uptake suggesting the presence of micropores. Hysteresis between the adsorption and desorption curves for all the samples reveal the presence of mesopores. Meanwhile, slight uptakes at high relative pressure near to 1.0 point indicating that existence some macropores, which probably forming between particles. All the samples exhibited very similar pore size distribution with a peak centering at ca. 3 nm (Figure 1b). Here it should be pointed out that the surface area of the original crystals cannot be

obtained because the framework of original crystals may collapse during the activated process, whereas high surface area is obtained when the crystals deal with high temperature carbonization. This method-direct carbonization provided a meaningful approach for solving the problem of effective use of unstable porous crystal materials.

The high surface areas of the obtained carbon materials prompted us to study their gas-uptake capacity, especially that for hydrogen, carbon dioxide and methane. As is shown in Figure 2a, the hydrogen adsorption isotherms of all the obtained carbons measured at 1 bar and liquid nitrogen temperature (77 K) by the volumetric method. All the isotherms do not display any hysteresis, indicating that the uptake of hydrogen by the nanoporous carbon materials is reversible. The hydrogen uptake capacity of C1000 reached  $20.1 \text{ mg g}^{-1}$ , which is comparable with HKUST-1 (the amount absorbed  $25.4 \text{ mg g}^{-1}$ ). From the pore size distribution analysis, the micropore pore volume can be regarded as facilitating the hydrogen uptake. The nearly close micropore distribution of three samples C1000, C1200 and C1400 can also explain their close adsorption quantity of hydrogen uptakes. The isosteric heat of adsorption for  $H_2$  was obtained by applying the virial-type expression of the Clausius-Clapeyron equation to the isotherms measured at 77 and 87 K. The isosteric heat of adsorption at low coverage is around  $8.4 \text{ kJ mol}^{-1}$  for C1000, decreasing slightly to  $5.3 \text{ kJ mol}^{-1}$  at higher coverage (Figure 2b). This value of the heat



**Figure 2** | (a)  $H_2$  isotherms for all carbon samples at 77 K and 1 bar; (b) high-pressure total (blue) and excess (red)  $H_2$  adsorption isotherms for C1000 at 77 K, and the insert plot showing isosteric heats of adsorption ( $Q_{st}$ ) as a function of  $H_2$  uptake for C1000.



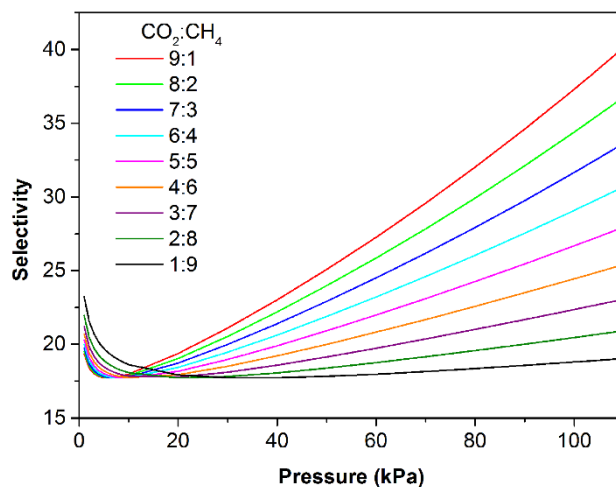
**Figure 3** | (a) CH<sub>4</sub> isotherms for all carbon samples at 298 K and 1 bar; (b) CO<sub>2</sub> isotherms for all carbon samples at 298 K; (c) high-pressure CH<sub>4</sub> adsorption measurements on C1000 at 298 K; (d) Isothermic heats of adsorption (Qst) as a function of CH<sub>4</sub> and CO<sub>2</sub> uptake for C1000.

of adsorption at low coverage is higher than that of HKUST-1 ( $\sim 7$  kJ mol<sup>-1</sup>), silica gel (7.3 kJ mol<sup>-1</sup>) and other microporous carbons after various chemical activations (7–7.5 kJ mol<sup>-1</sup>)<sup>37,38</sup>. The high enthalpy could be attributed to the small size of the pore.

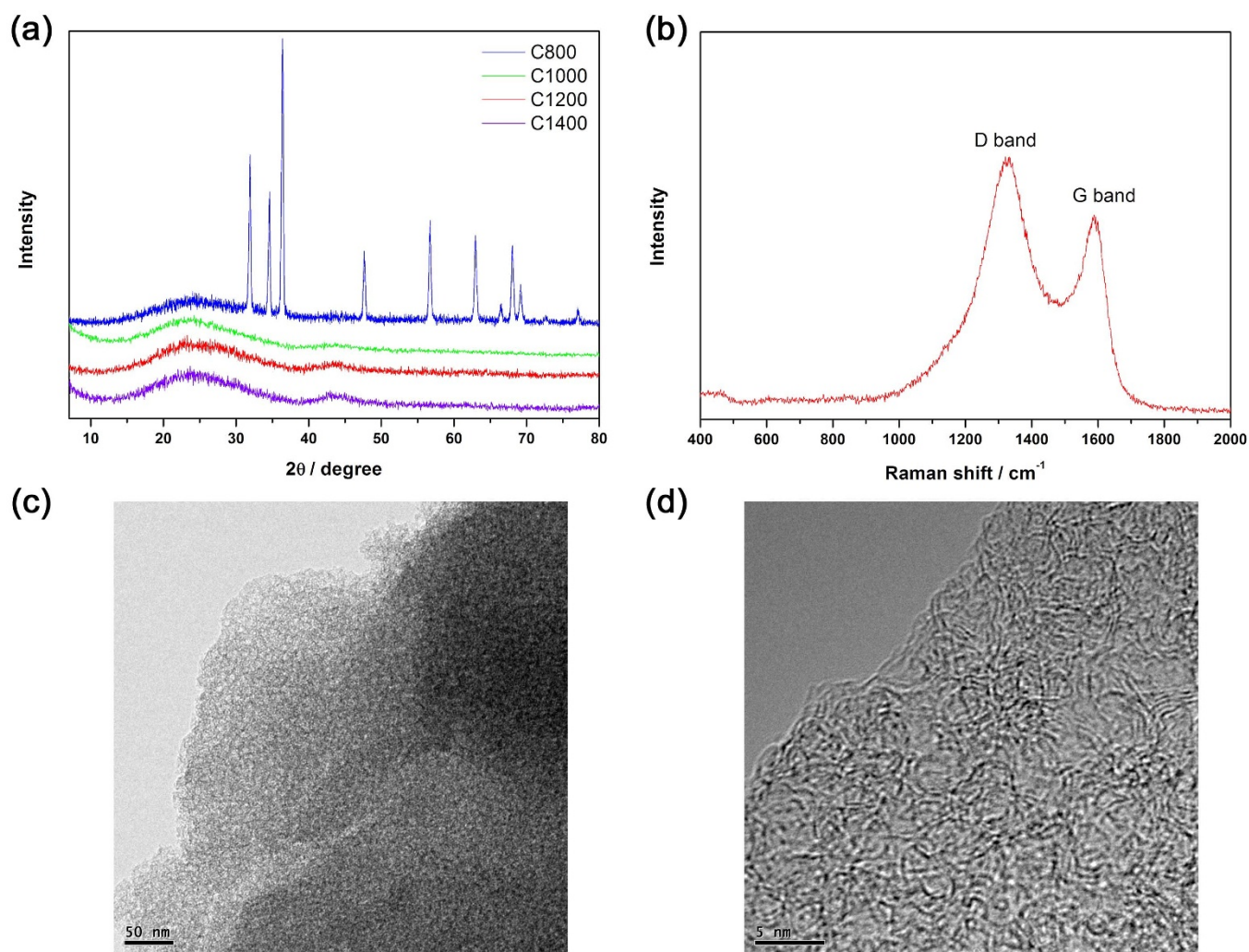
H<sub>2</sub> or CH<sub>4</sub> is a good candidate as an on-board fuel, however it lacks a reliable way of storage. In order to further evaluate the gas storage capacity of C1000, high-pressure adsorption capacities of H<sub>2</sub> and CH<sub>4</sub> of C1000 were measured at 77 K and 298 K, respectively (Figure 2b and 3c). As is shown in Figure 2b, the excess H<sub>2</sub> uptake at 77 K and 17.9 bar can reach 32.9 mg g<sup>-1</sup> and the total uptake is high to 45 mg g<sup>-1</sup> which can compare to that of many porous carbon materials<sup>1,39,40</sup>. The saturation excess CH<sub>4</sub> uptake of C1000 at 298 K and 95 bar is up to 135.6 mg g<sup>-1</sup>, 11.9 wt.% (HKUST-1 15.7 wt.% at 75 bar and 303 K)<sup>41</sup>. Meanwhile, at 95 bar, the total CH<sub>4</sub> uptake can reach as high as 208 mg g<sup>-1</sup> (17.2 wt%). Though the CH<sub>4</sub> uptake is still below the target of 400 mg g<sup>-1</sup> in an ANG fuel storage system for passenger vehicle usage, it is one of the best methane storage materials based on porous materials so far<sup>40,42</sup>.

In addition, the CO<sub>2</sub> and CH<sub>4</sub> were also measured at 298 K, respectively. As shown in Figure 3a and 3b, the maximum adsorbed amount of CO<sub>2</sub> and CH<sub>4</sub> of C1000 up to 163 mg g<sup>-1</sup> and 28 mg g<sup>-1</sup> at 298 K and 1 bar, respectively, and the enormous difference of uptakes shows that the C1000 should have CO<sub>2</sub>/CH<sub>4</sub> separation performance. The significantly high CO<sub>2</sub>/CH<sub>4</sub> separation selectivity demonstrates the promise of C1000 for practical CO<sub>2</sub>/CH<sub>4</sub> separation at room temperature. The CO<sub>2</sub>/CH<sub>4</sub> adsorption selectivity for

binary mixtures can be calculated by the IAST which has been successfully applied to predict binary gas mixture separation for the porous carbon, zeolites, MOFs, and porous polymers. As can be seen from Figure 4, the adsorption selectivities of C1000 for CO<sub>2</sub>/CH<sub>4</sub> as



**Figure 4** | IAST predicted selectivity for CO<sub>2</sub>/CH<sub>4</sub> with different mole ratios in C1000.



**Figure 5** | (a) PXRD pattern of samples; (b) Raman spectra of C1200; (c) and (d) TEM images of sample C1200.

different ratios were estimated from the experimental single-component isotherms which were fitted to a single-site Langmuir-Freundlich model. Overall C1000 showed increasing  $\text{CO}_2/\text{CH}_4$  selectivities with increasing pressure. For example, C1000 exhibited exceptionally high adsorption selectivity for  $\text{CO}_2/\text{CH}_4$  in an equimolar mixture at 298 K and 1 bar ( $S_{\text{ads}} = 27$ ) which is much higher than that of some porous materials at the similar condition<sup>43–45</sup>, such as PPN-1 ( $S_{\text{ads}} = 4.5$ )<sup>46</sup>, UTSA-25 ( $S_{\text{ads}} = 12.5$ )<sup>47</sup>,  $\text{Zn}_3(\text{OH})(\text{p-CDC})_{2.5}$  ( $S_{\text{ads}} = 5 \sim 17$ )<sup>48</sup>, OMC ( $S_{\text{ads}} = 3.4$ )<sup>49</sup>. We attributed much higher quadrupole moment of  $\text{CO}_2$  to the high adsorption selectivity for  $\text{CO}_2/\text{CH}_4$ . The interactions between  $\text{CO}_2$  molecule and carbon are stronger than  $\text{CH}_4$ <sup>18</sup>. Moreover, we also investigated the heat of adsorption of  $\text{CH}_4$  and  $\text{CO}_2$  in the temperature range between 298 K and 273 K. The isosteric heat of adsorption of  $\text{CO}_2$  at low coverage is around  $20.7 \text{ kJ mol}^{-1}$  for C1000, decreasing slightly to  $18.8 \text{ kJ mol}^{-1}$  at higher coverage. For the heat of adsorption of  $\text{CH}_4$  at low coverage is around  $17.4 \text{ kJ mol}^{-1}$  for C1000, decreasing slightly to  $16.3 \text{ kJ mol}^{-1}$  at higher coverage (Figure 3d). In terms of heat of adsorption,  $\text{CO}_2$  is higher than  $\text{CH}_4$ . This result can also account for the high adsorption selectivity for  $\text{CO}_2/\text{CH}_4$ . Both values of  $\text{CO}_2$  and  $\text{CH}_4$  are comparable with several commercially activated carbons ( $16\text{--}25 \text{ kJ mol}^{-1}$  for  $\text{CO}_2$  and  $16\text{--}20 \text{ kJ mol}^{-1}$  for  $\text{CH}_4$  at zero loading, respectively)<sup>50,51</sup>.

## Discussion

The obtained nanoporous carbon materials exhibited high gas storage abilities and adsorption selectivity prompted us to study

its pore structures. Powder X-ray diffraction patterns (PXRD) of C800, C1000, C1200 and C1400 were presented in Figure 5a. All the sharp peaks were observed in sample C800 that could be assigned to the ZnO species. To obtain pure carbon materials, it is necessary washing with strong acids in the usual method. On the other hand, this undoubtedly needs an additional step of washing process. In previous reports, when the temperature higher than  $800^\circ\text{C}$ , ZnO was reduced to metallic Zn species, and the carbon matrix materials obtained as long as the temperature higher the boiling point of metallic Zn ( $908^\circ\text{C}$ )<sup>22,52</sup>. Based on this strategy, the much higher carbonization temperature was used, which up to  $1000^\circ\text{C}$ ,  $1200^\circ\text{C}$ , and  $1400^\circ\text{C}$ . The results are the same as expected, for the samples of C1000, C1200 and C1400, the peaks of ZnO species from PXRD cannot be found instead by two broad peaks at around  $24^\circ$  and  $44^\circ$  that were assigned to the carbon (002) and (101) diffractions, respectively. Also, the Energy-dispersive X-ray spectrometer (EDS) and Fourier transform infrared spectroscopy (FT-IR) measurements were performed to further confirm the removal of Zn from carbon matrix. The EDS results indicate that the percentage of Zn present in the carbon matrix is almost negligible when the temperature up to  $1000^\circ\text{C}$  (that is, less than  $<1\%$ ; Figure S1, Table S1). From the FTIR spectra analysis (Figure S2), a weak peak located at  $1120 \text{ cm}^{-1}$  can be attributed to the C-O vibration. Zn-O vibration was disappeared in C1000, C1200 and C1400, however, which is obvious in C800 nearby  $440 \text{ cm}^{-1}$ . In addition, from the (002) peaks in the PXRD profiles, the degree of graphitization of the C1000, C1200 and C1400 samples could be low<sup>53</sup>.


**Table 1 | BET surface areas and pore volumes for all the carbon samples**

Samples	$S_{\text{BET}}^a$ ( $\text{m}^2 \text{g}^{-1}$ )	$V_t^b$ ( $\text{cm}^3 \text{g}^{-1}$ )	$V_{\text{micro}}^c$ ( $\text{cm}^3 \text{g}^{-1}$ )	$V_{\text{micro}}/V_t$ (%)
C800	464	0.25	0.11	44
C1000	1492	0.96	0.26	27
C1200	1671	1.01	0.29	29
C1400	1254	0.73	0.26	36

<sup>a</sup>The specific surface area ( $S_{\text{BET}}$ ) was calculated by the Brunauer-Emmet-Teller (BET) method.

<sup>b</sup> $V_t$  represented the total pore volume.

<sup>c</sup> $V_{\text{micro}}$  represented the volume of micropore.

In order to further investigate the details of structure on carbon materials, Raman spectra and transmission electron microscopy (TEM) were performed. Raman spectra for the C1200 sample are shown in Figure 5b. The spectra displayed D and G bands at 1333 and 1588  $\text{cm}^{-1}$ , respectively. Generally speaking, the appearance of the D peak corresponds to the presence of a disordered carbon structure. The relative ratios of the G bands to the D bands ( $I_G/I_D$ ) reveal the crystallization degree of graphitic carbon. The appearance of the obvious D bands indicated that graphene sheets were not well developed and the carbon structure contained both graphitic and disordered carbon atoms<sup>28–31</sup>. In addition, from the high resolution images observations (Figure 5c and 5d), randomly assembled the nanometer-sized sheets were observed in the obtained carbon materials, and the disordered graphitic layers suggest a relatively low degree of graphitization, revealing a low concentration of parallel single layers in the obtained carbon material, which in agreement with the PXRD and Raman spectra results mentioned above<sup>29</sup>.

The BET surface area and pore size distributions of all the samples are shown in the Table 1. From the table analysis, the pore structures of obtaining carbons vary depending on the treatment conditions. The pore-size distribution calculated from DFT was widely distributed from 1 to 4 nm. The BET surface area and total pore volume of C800 were found to be 464  $\text{m}^2 \text{g}^{-1}$  and 0.25  $\text{cm}^3 \text{g}^{-1}$ , respectively, which are much lower than other three samples. This may cause by ZnO species remained in the obtained carbon. However, the highest BET surface area of 1671  $\text{m}^2 \text{g}^{-1}$  and corresponding pore volume 1.01  $\text{cm}^3 \text{g}^{-1}$  is obtained for the sample of C1200, suggesting that the carbonization temperature plays an important role in the resultant carbon. Recently, Kim<sup>32</sup> and Kurungot<sup>35</sup> have found that the porosity of the carbon materials depends linearly on the Zn/C ratio of MOF precursors and even the nonporous MOF could also generate highly nonporous carbons. The removal of Zn from carbons is critical for acquiring high BET surface area. During the carbonization process ( $\geq 900^\circ\text{C}$ ), ZnO was reduced to Zn and vaporized away along with the  $\text{N}_2$  flow, accompany by considerable C and O mass-loss which evolution of CO and  $\text{CO}_2$ , leaving a more defective or hollow carbon network. This process acts as a simple self-activation for the carbon<sup>54</sup>. This observation may account for the high improvement of the BET surface area from C800 to C1200. It is noticeable that the BET surface area of C1200 is even higher than its isostructural crystal (1507  $\text{m}^2 \text{g}^{-1}$  for HKUST-1) reported before<sup>37</sup>. Meanwhile, the data in the table also reveal the complication of the temperature effect on the carbon structures. The BET surface area increased with the temperature rose. But when the temperature reached 1400 $^\circ\text{C}$ , it is reduced. This may be due to the higher temperature destroyed the structure of the pores.

In conclusion, we have successfully employed a method—direct carbonization of non-permanent highly porous MOF  $[\text{Zn}_3(\text{BTC})_2 \cdot (\text{H}_2\text{O})_3]_n$  without any additional carbon precursors to prepare porous carbon materials, which exhibits high specific surface areas, mainly with mesopores, significant gas uptake capabilities in both low-pressure and high-pressure environments as well as exceptionally high adsorption selectivity for  $\text{CO}_2/\text{CH}_4$ . The carbonization tem-

perature plays an important role in specific surface area, pore size distribution and gas uptake. The carbon materials obtained at 1200 $^\circ\text{C}$  have the highest specific surface areas ( $S_{\text{BET}} = 1671 \text{ m}^2 \text{g}^{-1}$ ). The C1000 has the best gas uptake capacities and exhibited exceptionally high adsorption selectivity for  $\text{CO}_2/\text{CH}_4$  in an equimolar mixture at 298 K and 1 bar ( $S_{\text{ads}} = 27$ ). Combined with gas uptake ability and physicochemical stability, these carbon materials are very promising for the clean energy storage and gas separation. This carbonization method can be easily extended to the preparation of nanoporous carbon materials by using the other non-permanent highly porous MOFs.

## Methods

**Sample preparation.** *Chemicals.* All chemicals were obtained from commercial vendors and used without further purification unless otherwise specified.

Preparation of MOF  $[\text{Zn}_3(\text{BTC})_2 \cdot (\text{H}_2\text{O})_3]_n$ .  $[\text{Zn}_3(\text{BTC})_2 \cdot (\text{H}_2\text{O})_3]_n$  crystals were prepared by our modified method according to a previous report<sup>36</sup>. A mixture of  $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (0.2975 g, 1 mmol), 1, 3, 5-benzenetricarboxylic acid (0.2100 g, 1 mmol), 4, 4'-bipyridine (0.0156 g, 0.1 mmol), and N, N-Dimethylformamide (DMF, 12 mL) was stirred at room temperature for 2 h. The solution was filled in a 25 mL vial. The vial was capped tightly, placed in an oven and heated to 80 $^\circ\text{C}$  for 48 h to yield large colorless blocky crystals. After cooling, the crystals were filtered, washed with DMF three times and immersed in dried DMF for further experiments.

*Preparation of nanoporous carbon.* The prepared  $[\text{Zn}_3(\text{BTC})_2 \cdot (\text{H}_2\text{O})_3]_n$  crystals were put into a ceramic boat. Then the prepared MOF was transferred to a tube furnace and heated under a nitrogen gas flow from room-temperature to 800 $^\circ\text{C}$ , 1000 $^\circ\text{C}$ , 1200 $^\circ\text{C}$ , 1400 $^\circ\text{C}$  with a heating rate of 5 $^\circ\text{C min}^{-1}$  to pyrolyze the organic species. After the temperature reached the goal settings, it was maintained for 5 h. After that, the material was then cooled to room temperature with a cooling rate of 5 $^\circ\text{C min}^{-1}$ . Finally, the MOFs calcined at 800 $^\circ\text{C}$ , 1000 $^\circ\text{C}$ , 1200 $^\circ\text{C}$  and 1400 $^\circ\text{C}$  for 5 h afford the nanoporous carbon materials designated as C800, C1000, C1200, and C1400, respectively.

**Measurements.** The nitrogen adsorption-desorption measurements were carried out at liquid nitrogen temperature (77 K) by using an automatic volumetric adsorption equipment (Micromeritics, ASAP2020). PXRD patterns were recorded on a MiniFlex II spectrometer using  $\text{Cu K}\alpha$  radiation. TEM images were obtained using a JEOL JEM-2010 microscope. Raman data were obtained on a LabRAM Aramis (Laser Confocal Micro-Raman Spectroscopy) spectrometer using a 532 nm wavelength. FT-IR spectra were collected on a VERTEX 70 spectrometer (using KBr pellets). EDS was performed using a JSM 6700 microscope. The high temperature pyrolysis reaction was performed on a tube furnace (KTL 1600, Nanjing NanDa Instrument Plant). Low pressure (<800 torr) gas sorption isotherms was performed using a Micromeritics ASAP 2020 surface area and pore size analyzer. Pore size distribution data were obtained from the  $\text{N}_2$  sorption isotherms based on the DFT model on the Micromeritics ASAP 2020 software package (assuming slit pore geometry). An ultra-high purity (UHP, 99.9999% purity) grade of  $\text{N}_2$ ,  $\text{H}_2$ ,  $\text{CH}_4$ , and  $\text{CO}_2$  gases was used throughout the adsorption experiments. Prior to the measurements, all the samples were degassed at 120 $^\circ\text{C}$  for 10 h to remove the adsorbed impurities. High pressure excess adsorption of  $\text{H}_2$  and  $\text{CH}_4$  were performed using a Hydrogen Storage Analyser (HTP1-V, Hiden) at 77 K (liquid nitrogen bath) or 298 K (room temperature). Prior to the measurements, the sample was degassed at 120 $^\circ\text{C}$  for 10 h to remove the adsorbed impurities. The hydrogen isosteric heat of sorption was calculated as a function of the hydrogen uptake by comparing the adsorption isotherms at 77 K and 87 K. The data were modeled with a virial-type expression composed of parameters  $a_i$  and  $b_i$  (Equation 1), and the heat of adsorption ( $Q_{\text{st}}$ ) was then calculated from the fitting parameters using Equation 2, where  $p$  is the pressure,  $N$  is the amount adsorbed,  $T$  is the temperature,  $R$  is the universal gas constant, and  $m$  and  $n$  determine the number of terms required to adequately describe the isotherm. In order to compare the efficacy of C1000 for  $\text{CO}_2/\text{CH}_4$  separation, we used the IAST of Myers and Prausnitz<sup>55</sup> along with the pure component isotherm fits to determine the molar loadings in the mixture for specified partial pressures in the bulk gas phase. The measured experimental data on pure component isotherms for  $\text{CO}_2$  and  $\text{CH}_4$ , in terms of excess loadings, were first converted to absolute loading using the Peng-Robinson equation of state for estimation of the fluid densities. The pore volume of C1000 used for this purpose was 0.96  $\text{cm}^3 \text{g}^{-1}$ . The absolute component loadings at 298 K were fitted with either a single-site Langmuir-Freundlich model (Equation 3), where  $a$  is saturation capacity and  $b$  and  $c$  are constant.

$$\ln p = \ln N + \frac{1}{T} \sum_{i=0}^m a_i N^i + \sum_{i=0}^n b_i N^i \quad (1)$$



$$Q_{st} = -R \sum_{i=0}^m a_i N^i \quad (2)$$

$$N = a \times \frac{bp^c}{1 + bp^c} \quad (3)$$

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## Acknowledgments

We gratefully thank the financial support of the NSF of China (No. 21271172), the “One Hundred Talent Project” from Chinese Academy of Sciences, and the NSF of Fujian Province (No. 2012J01058).



## Author contributions

D.Q.Y. and W.J.W. designed the study and reviewed the manuscript. W.J.W. performed the experiments and prepared the manuscript.

## Additional information

Supplementary information accompanies this paper at <http://www.nature.com/scientificreports>

**Competing financial interests:** The authors declare no competing financial interests.

**How to cite this article:** Wang, W.J. & Yuan, D.Q. Mesoporous carbon originated from non-permanent porous MOFs for gas storage and CO<sub>2</sub>/CH<sub>4</sub> separation. *Sci. Rep.* **4**, 5711; DOI:10.1038/srep05711 (2014).



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